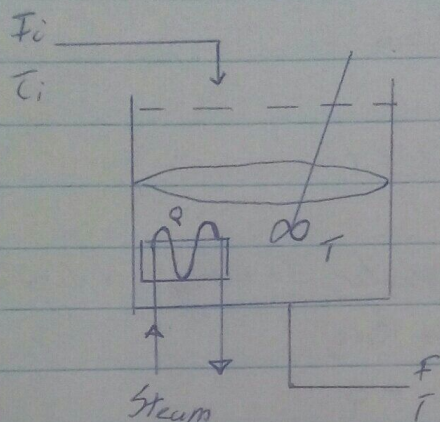


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14/ENGE01/015

CHE 531

Assignment 1



Assuming that $Q = m_i h_s$

liquid density, $\rho = 1000 \text{ kg/m}^3$

Liquid inlet flowrate, $F_i = 0.15 \text{ m}^3/\text{min}$

Latent heat of vaporization of steam at boiling point, h_s
 $= 2258 \text{ kJ/kg}$

Taking an Energy balance about the system,

$$\frac{dU}{dt} = F_i \rho \left(u + \frac{P_i}{\rho} \right) - F \rho \left(u + \frac{P}{\rho} \right) + Q + W_s$$

Since Enthalpy, $H = u + Pv$,

$$\frac{dH}{dt} = \frac{du}{dt} + \frac{Pv}{dt}$$

$$\therefore \frac{dH}{dt} - \frac{d(Pv)}{dt} = \frac{du}{dt}$$

$$\Rightarrow \frac{dH}{dt} - \frac{d(Pv)}{dt} = F_i \rho H_i - F \rho H + Q + W_s$$

$$\text{Since } \frac{d(PV)}{dt} = \frac{Pdv}{dt} + \frac{VdP}{dt}$$

Since Volume is constant (i.e. $\frac{dV}{dt} = 0$) and $\frac{dP}{dt}$ can be neglected

due to constant density $\therefore \frac{d(PV)}{dt} = 0$

$$\therefore \frac{dT}{dt} = FSH_i - FSH + Q + W_s$$

Neglecting work done by the impeller, assuming a single phase & constant heat capacity, C_p - we have,

$$V\rho C_p \frac{dT}{dt} = F\rho C_p (\bar{T}_i - \bar{T}) + Q$$

$$\frac{dT}{dt} = \frac{F}{V} (\bar{T}_i - \bar{T}) + \frac{Q}{F\rho C_p}$$

$$\frac{V}{F} \frac{dT}{dt} + \bar{T} = \bar{T}_i + \frac{Q}{F\rho C_p} \rightarrow \text{Theoretical dynamic Model.}$$

Recall $Q = M_s h_s$

$$\frac{2}{0.15} \frac{dT}{dt} + \bar{T} = \bar{T}_i + \frac{2258}{0.15 \times 1000 \times 4.187}$$

$$20 \frac{dT'}{dt} + \bar{T}' = \bar{T}'_i + 3.6 \text{ m/s}^2$$

Finding the transfer function,

$$20(sT'(s) - T'(0)) + T'(s) = \bar{T}'_i(s) + 3.6 \text{ m/s}^2(s)$$

$$20sT'(s) + T'(s) = \bar{T}'_i(s) + 3.6 \text{ m/s}^2(s)$$

$$T'(s)(20s + 1) = \bar{T}'_i(s) + 3.6 \text{ m/s}^2(s)$$

$$T'(s) = \frac{\bar{T}'_i(s)}{(20s + 1)} + \frac{3.6 \text{ m/s}^2(s)}{(20s + 1)}$$