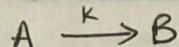


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CHE 532: Process Dynamics and Control II

For a first order rxn



$$-r_A = kC_A$$

$$\therefore r_A = -kC_A$$

Taking overall mass balance

$$\text{ACCUMULATION} = \text{IN} + \text{GENERATION} - \text{OUT}$$

$$\frac{dm}{dt} = \dot{m}_{in} + r_A V - \dot{m}_{out}$$

$$\text{We know } \dot{m} = FC_A$$

$$\text{and } m = C_A V$$

$$\frac{dm}{dt} = FC_{Ai} - FC_A + r_A V$$

$$\frac{dm}{dt} = FC_{Ai} - FC_A - kC_A V$$

$$\frac{d(C_A V)}{dt} = FC_{Ai} - FC_A - kC_A V$$

Constant volume

$$V \frac{dC_A}{dt} = FC_{Ai} - FC_A - kC_A V$$

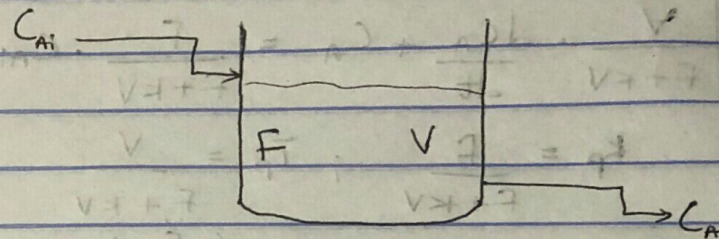
Divide through by F

$$\frac{V}{F} \frac{dC_A}{dt} = C_{Ai} - C_A - \frac{kC_A V}{F}$$

$$\frac{V}{F} \frac{dC_A}{dt} = C_{Ai} - \frac{kC_A V}{F} - C_A$$

$$\frac{V}{F} \frac{dC_A}{dt} = C_{Ai} + \left( \frac{-kC_A V - FC_A}{F} \right)$$

$$\frac{V}{F} \frac{dC_A}{dt} + \frac{FC_A + kC_A V}{F} = C_{Ai}$$



$$\frac{V}{F} \frac{dC_A}{dt} + C_A \left( \frac{F + KV}{F} \right) = C_{Ai}$$

Divide through by  $\left( \frac{F + KV}{F} \right)$

— standard form

$$\frac{V}{F + KV} \cdot \frac{dC_A}{dt} + C_A = \frac{F}{F + KV} \cdot C_{Ai}$$

$$K_p = \frac{F}{F + KV} ; T_p = \frac{V}{F + KV}$$

$$G_p(s) = \frac{K_p}{T_p s + 1} = \frac{\left( \frac{F}{F + KV} \right)}{\left( \frac{V}{F + KV} \right) s + 1}$$

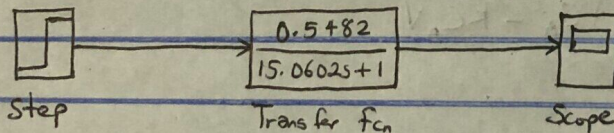
$$V = 2.5 \text{ m}^3; F = 0.091 \text{ m}^3/\text{min}; K = 0.03 \text{ min}^{-1}$$

$$K_p = \frac{0.091}{0.091 + (0.03 \times 2.5)} = \frac{0.091}{0.166} = 0.5482$$

$$T_p = \frac{2.5}{0.091 + (0.03 \times 2.5)} = \frac{2.5}{0.166} = 15.0602$$

$$G_p(s) = \frac{0.5482}{(15.0602)s + 1}$$

Open loop



Closed loop

