

$$V = \sqrt{2gh}$$

$$V = \sqrt{2 \times 9.81 \times 2.083}$$

$$V = 6.39 \text{ m/s}$$

5.)  $0.05 \text{ m}^3/\text{min}$

15 bar

1700 rpm

10 cm<sup>3</sup> per rev

15 Nm

$$A_1 = \frac{\pi d^2}{4} = \frac{\pi \times (15/100)^2}{4}$$

$$A_1 = 0.0176 \text{ m}^2$$

$$A_2 = \frac{\pi d^2}{4} = \frac{\pi \times (30/100)^2}{4}$$

$$A_2 = 0.0706 \text{ m}^2$$

$$h = y \left[ \frac{13.6}{0.9} - 1 \right]$$

$$h = 0.5 \left[ \frac{13.6}{0.9} - 1 \right]$$

$$= 7.05 \text{ m of oil}$$

$$Q = C_d \cdot A_1 \cdot A_2 \cdot \frac{\sqrt{2gh}}{\sqrt{A_1^2 - A_2^2}}$$

$$Q = 0.64 \times 0.0176 \times 0.0706 \times \frac{\sqrt{2 \times 9.81 \times 7.05}}{\sqrt{(0.0706)^2 - (0.0176)^2}}$$

$$Q = \frac{9.35 \times 10^{-3}}{4.0112}$$

$$Q = 2.33 \times 10^{-3} \text{ m}^3/\text{s}$$

4)  $A_{\text{pers}} = 15 \text{ m}$

170 mm of mercury (0.17 m)

S.G. of mercury = 13.6

S.G. of sea-water = 1.026

$V = ?$

$$h = y \left( \frac{S h_1}{S h_2} - 1 \right)$$

$$h = 0.17 \left( \frac{13.6}{1.026} - 1 \right)$$

$$h = 2.083 \text{ m}$$

$$y = 30 \text{ cm (0.3 m of mercury)}$$

$$\text{Pressure at inlet } P_1 = 17.658$$

$$= \frac{17658}{10000} = 1.7658 \times 10^{-3} \text{ N/m}$$

$$\frac{P_1}{w} = \frac{17658 \times 10^{-3}}{9.81} = 1.8 \times 10^{-4} \text{ m}$$

$$\frac{P_2}{w} = 0.3 \times 13.6 = -4.08 \text{ of } H_2O$$

$$h = \frac{P_1}{w} - \frac{P_2}{w} = 1.8 \times 10^{-4} (-4.08)$$

$$h = 4.08018 \text{ m}$$

$$Q = C_d \times \frac{A_1 A_2}{\sqrt{A_1^2 - A_2^2}} \times \sqrt{2gh}$$

$$Q = 0.98 \times \frac{0.0314 \times 7.853 \times 10^{-3}}{\sqrt{(0.0314)^2 - (7.853 \times 10^{-3})^2}} \times \sqrt{2 \times 9.81 \times 4.08018}$$

$$Q = \frac{0.000241}{0.0304} \times 8.947$$

$$Q = 0.0709 \text{ m}^3/\text{s}$$

3.)  $D_1 = 15 \text{ cm}$

$D_2 = 30 \text{ cm}$

50 cm of mercury (0.5 m)

$Q = ?$

$S.G. = 0.9$

$C_d = 0.64$

4.)  $A_2$

ECREBODR EFE CHASTIAN

18/ENG05/014

Mechatronics Engineering  
Basic Fluid Mechanics (ENG)

1.)  $V_1 = 5 \text{ m s}^{-1}$

$V_2 = 2 \text{ m s}^{-1}$

$P_1$  at smaller end = 2.5 m

$$h_f = \frac{0.35 (V_1^2 - V_2^2)^2}{2g}$$

$L = 2.0 \text{ m}$

$P_2$  at lower end

$L = z_1 - z_2 = 2 \text{ m}$

$$\frac{P_1}{\rho} + \frac{V_1^2}{2g} + z_1 = \frac{P_2}{\rho} + \frac{V_2^2}{2g} + z_2 + h_f$$

$$\frac{P_2}{\rho} = \frac{P_1}{\rho} + \frac{1}{2g} (V_1^2 - V_2^2) + (z_1 - z_2) - h_f$$

$$= 2.5 + \frac{5^2 - 2^2}{2 \times 9.81} + 2 - \frac{0.35(5-2)^2}{2 \times 9.81}$$

$$= 2.5 + 1.07 + 2 - 0.11055$$

$P_2 = 5.409 \text{ bar}$ ,

$\therefore$  Pressure at lower end is 5.409 bar.

2.) Inlet diameter = 200 mm

Throat diameter = 100 mm

Pressure at inlet = 17.058 N/m

Vacuum pressure at throat = 30 cm of mercury

$d = 0.98$

$$A_1 = \frac{\pi d^2}{4} = \frac{\left(\frac{20}{100}\right)^2 \times \pi}{4}$$

$A_1 = 0.0314 \text{ m}^2$

$$A_2 = \frac{\pi d^2}{4} = \frac{\left(\frac{10}{100}\right)^2 \times \pi}{4}$$

$A_2 = 7.853 \times 10^{-3} \text{ m}^2$