

Name - Tolunlogo Akemi
Matric no - 1716401078
Department - Mechanical Eng.

- Pressure gradient is constant
- The flow is uniform
- The flow is steady

- Diameter of the pipe (m)
- The density of the fluid passing through the pipe (kg/m^3)
- The viscosity of the fluid (Ns/m^2)
- The Velocity of the flow (m/s)

Aerofluid

It is lifting device
mainly used in gaseous
fluid

It is mainly used for lifting
airplanes and jet

Hydrofluid

It is lifting device
mainly used in liquid
fluid

It is mainly used for Ocean
drag and crane machines
move with a high air
velocity in water

16. Given $\rho = 0.7 \text{ g/cm}^3 = 0.7 \times 10^3 \text{ kg/m}^3 = 0.7 \times 10^3 \text{ N/m}^3$

$$V = 1 \text{ m/s}$$

$$h = 10 \text{ m} = 0.1 \text{ m}$$

$$dp = 6000 \text{ N/m}^2$$

$$h = 60 \text{ m}$$

Therefore the pressure difference gradient is

$$\frac{dp}{dh} = \frac{6000}{60} = 1 \times 10^3 \text{ N/m}^3$$

i. Velocity distribution = $v = v_{\text{avg}} \left[1 - \frac{r^2}{R^2} \right] \left(\frac{dp}{dz} \right) \left(\frac{4\mu}{\rho g} \right)$

$$V = 1007 + 55558g - 555558g$$

$$v = (5.67 \times 10^{-8}) \cdot (2.5 \times 10^3)^2 \cdot 7$$

∴ Discharge per unit width $= \frac{v \cdot b}{12 \mu} \left(\frac{dp}{dx} \right)$

$$T = 0.0001059257$$

$$= 0.0757 \text{ m}^2/\text{s}$$

∴ Shear stress at upper plate = $\tau = \mu \cdot \frac{dv}{dy}$

$$= \frac{\mu \cdot v}{b} = \frac{1}{2} \left(\frac{dp}{dx} \right) \left(\frac{b}{2} \right)$$

$$= \frac{1}{2} \cdot \frac{\mu \cdot v}{b} = \frac{1}{2} \left(\frac{dp}{dx} \right) \left(\frac{b}{2} \right)$$

$$\tau = 0.095 = 95 \text{ N/m}^2$$

② Given $\mu = 0.1 \text{ Pa}\cdot\text{s}$

$$P_1 = 120 \text{ kPa}$$

$$v = 0.15 \text{ m/s}$$

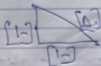
$$\frac{dv}{dy} = (P_1 - P_2) \cdot \frac{1}{2\mu}$$

∴ $\tau = \mu \cdot \frac{dv}{dy}$

$$\text{And } P_1 = P_1 + P_2 = \text{Piezometric}$$

$$= 262.38 \text{ kN/m}^2$$

$$\text{And } P_2 = P_2 + P_3 = \text{Piezometric}$$



$$A_{40} = \sqrt{1^2 + 1^2} = \sqrt{2} \text{ cm}$$

Therefore

$$\frac{dp}{dx} = \frac{(P_1 - P_2)}{A_2} = \frac{(262.38 - 80)}{\sqrt{2}} = 191.748 \text{ kN/m}^2$$

Velocity distribution $u = U_{\max} \left[1 - \left(\frac{y}{h} \right)^2 \right]$

$$U = 1500 + 11632 y - 71637 y^2$$

$$U = (7.16378 \times 10^4) y^2 + 11632 y + 1500$$

1) Shear distribution $\tau = \frac{\mu U}{h} \left(\frac{dy}{dx} \right) (2y - 2h)$

$$\tau = 213 + 64.74 - 12378 y$$

$$\tau = 507.74 - (1.237 \times 10^5) y$$

b) Maximum flow velocity

At maximum flow velocity $\frac{dy}{dx} = 0$

$$0 = (1.4328 \times 10^5) y + 565.62$$

$$y = 3.9476 \times 10^{-3} \text{ m}$$

$$U_{\max} = (7.16378 \times 10^4) (3.9476 \times 10^{-3})^2 + 565.62$$

$$= 3.9476 \times 10^{-3}$$

$$U_{\max} = 1.12 \text{ m/s}$$

② Shear stress upper plate is

$$\tau = 507.74$$

$$\text{Therefore } \tau = 507.74 - (1.237 \times 10^5) y$$

$$\tau = 779.26 \text{ N/m}^2$$