

i) Pressure head at smaller end = 2.5m  $\frac{P_1}{\rho g}$   
Length of tube = 2.0m

Velocity of flow at lower end =  $5 \text{ms}^{-1}$   $V_1$

" " " " higher " =  $2 \text{ms}^{-1}$   $V_2$

$$\text{Loss of head} = \frac{0.35 (V_1 - V_2)^2}{2g} h_f$$

$$\text{Loss of head} = \frac{0.35 (5-2)^2}{2 \times 9.81} = 0.16 \text{m}$$

Pressure head at higher end,  $\frac{P_2}{\rho g}$

$$\frac{P_1}{\rho g} + \frac{V_1^2}{2g} + Z_1 = \frac{P_2}{\rho g} + \frac{V_2^2}{2g} + Z_2 + h_f$$

$$Z_2 = 0 \quad Z_1 = 2.0 \text{m}$$

$$2.5 + \frac{5^2}{2 \times 9.8} + 2 = \frac{P_2}{\rho g} + \frac{2^2}{2 \times 9.8} + 0.016$$

$$5.775 = \frac{P_2}{\rho g} + 0.364$$

$$\frac{P_2}{\rho g} = 5.775 - 0.364 = 5.411 \text{m of liquid}$$

Pressure head at higher end = 5.411m

Vacuum pressure at the throat

$$\frac{P_2}{\omega} = -300\text{mm} = -0.3 \times 13.6 = -4.08\text{m of water}$$

$$\text{Differential head, } h = \frac{P_1}{\omega} - \frac{P_2}{\omega} = 18.01 - (-4.08) = 22.09\text{m}$$

Rate of flow,  $Q$

$$\text{Using the relation } Q = \frac{C_d \times A_1 A_2}{\sqrt{A_1^2 - A_2^2}} \times \sqrt{2gh}$$

$$Q = \frac{0.98 \times 0.0314 \times 0.00785}{\sqrt{(0.0314)^2 - (0.00785)^2}} \times \sqrt{2 \times 9.81 \times 22.09}$$

$$= \frac{0.000241 \times 20.82}{0.0304}$$

$$Q = 0.165\text{m}^3/\text{s}$$

Discharge of water through Venturimeter =  $0.165\text{m}^3/\text{s}$

3) Orifice diameter  $A_o = 15\text{cm} = 0.15\text{m}^2$

Pipe diameter  $= 30\text{cm} = 0.3\text{m}^2$

Manometer reading  $= 0.5\text{m}$  of mercury

Sp. gr. of oil  $= 0.9$   $C_d = 0.64$

Solution

Area of pipe Orifice,  $\frac{\pi}{4} \times 0.15^2 = 0.0177\text{m}^2$

Area of pipe,  $\frac{\pi}{4} \times 0.30^2 = 0.707\text{m}^2 = A_1$

Differential head,  $h = y \left[ \frac{S_h}{S_o} - 1 \right]$

$= 0.5 \left[ \frac{13.6}{0.9} - 1 \right] = 7.06\text{m}$  of oil

Discharge  $Q$ :

Using the relation,  $Q = C_d \times A_o \cdot A_1 \frac{\sqrt{2gh}}{\sqrt{A_1^2 - A_o^2}}$

$Q = \frac{0.64 \times 0.707 \times 0.0177 \times \sqrt{2 \times 9.8 \times 7.06}}{\sqrt{(0.707)^2 - (0.0177)^2}}$

$= \frac{0.0942}{0.707} = 0.133\text{m}^3/\text{s}$

Rate of oil discharge  $= 0.133\text{m}^3/\text{s}$

4) Reading of manometry  $y = 170\text{mm} = 0.17\text{m}$  mercury

Sp. gravity of mercury,  $S_h = 13.6$

Sp. gravity of sea water,  $S_1 = 1.026$

To find the head, ( $h$ ) using the relation:

$h = y \left[ \frac{S_h}{S_1} - 1 \right]$

$h = 0.17 \left[ \frac{13.6}{1.026} - 1 \right] = 2.08$

$\therefore$  Speed of the submarine

$V = \sqrt{2gh} = \sqrt{2 \times 9.81 \times 2.08} = 6.38\text{m/s}$

$$5) \text{ Actual flow rate} = 0.05 \text{ m}^3 / 45 = 0.05 / 60 = 8.3 \times 10^{-4} \text{ m}^3/\text{s}$$

$$\text{pressure change} = 15 \times 10^5 \text{ N/m}^2$$

$$\text{Speed of rotation} = 1700 \text{ rev/min} = \frac{1700}{60} = 28.3 \text{ rev/s}$$

$$\text{Normal displacement} = 1 \times 10^{-5} \text{ m}^3/\text{rev}$$

$$\text{Torque input} = 15 \text{ Nm}$$

$$\text{Ideal flow rate} = \text{normal} \times \text{speed displacement}$$

$$= 28.3 \times 1 \times 10^{-5}$$

$$= 2.83 \times 10^{-4} \text{ m}^3/\text{sec}$$

$$i) \text{ Volumetric efficiency} = \frac{\text{Actual flow rate}}{\text{Ideal flow rate}} \times 100\%$$

$$= \frac{8.3 \times 10^{-4}}{2.83 \times 10^{-4}} \times 100$$

$$= 293.28\%$$

$$= 296\%$$

$$ii) \text{ fluid Power} = Q \cdot dp$$

$$= 8.3 \times 10^{-4} \times 15 \times 10^5$$

$$= 1245 \text{ Watts}$$

$$iii) \text{ Shaft Power} = T \cdot \omega$$

$$T = \text{torque input}$$

$$\omega = \text{angular speed}$$

$$T = 15 \text{ Nm}$$

$$\omega = 2\pi N \text{ for rps}$$

$$\omega = \frac{2\pi N}{60}$$

$$=$$

$$\omega = 2 \times \frac{22}{7} \times 28.3 = 177.89 \text{ rad/s}$$

$$\text{Shaft power} = 15 \times 177.89$$

$$= 2668.35 \text{ watts}$$

$$iv) \text{ Overall efficiency} = \frac{\text{fluid Power}}{\text{Shaft power}} \times 100\%$$

$$= \frac{1245}{2668.35} \times 100$$

$$= 46.66\%$$

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