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 DEPT: MECHATRONICS ENGINEERING  
 COURSE: ENG 214 (FLUID MECHANICS)  
 MATRIC: 18/ENG05/057

SOLUTION:

(1) Let,  $L = 2.0\text{m}$

$V_1 = 5\text{m/s}$

$V_2 = 2\text{m/s}$

Reserve head =  $2.5\text{m}$

$$h_L = \frac{0.35(V_1 - V_2)^2}{2g}$$

$$h_L = \frac{0.35(5-2)^2}{2 \times 9.81} = 0.161\text{m}$$

Bernoulli's equation for real fluids

$$\frac{P_1}{\rho} + z_1 + \frac{V_1^2}{2g} = \frac{P_2}{\rho} + z_2 + \frac{V_2^2}{2g} + h_L$$

$$2.5 + 2 + \frac{5^2}{2 \times 9.81} = \frac{P_2}{\rho} + 0 + \frac{2^2}{2 \times 9.81} + 0.161$$

$$\frac{P_2}{\rho} = 5.41 //$$

(2) Inlet diameter =  $20\text{cm} = 0.2\text{m}$

$$A_1 = \frac{\pi}{4} \times 0.2^2 = 0.0314\text{m}^2$$

throat diameter =  $10\text{cm} = 0.1\text{m}$

$$A_2 = \text{Area of throat} = \frac{\pi}{4} \times 0.1^2 = 0.00785\text{m}^2$$

$$P_1 = \text{pressure at inlet} = 176.58\text{N/cm}^2 = 176.58\text{kN/m}^2$$

$$\frac{P_1}{\rho} = \frac{176.58}{9.81} = 18\text{m}$$

$$\frac{h}{\rho} = -30\text{cm of mercury} = -0.3\text{m of mercury} = -0.3 \times 13.6 = -4.08\text{m of water}$$

Discharge of water,  $Q$

$$Q = C_d \times A_1 A_2 \times \frac{\sqrt{2gh}}{\sqrt{A_1^2 - A_2^2}}$$

$$Q = 0.98 \times 0.0314 \times 0.00785 \times \frac{\sqrt{2 \times 9.81 \times 22.08}}{\sqrt{(0.0314)^2 - (0.00785)^2}}$$

$$Q = 0.1654\text{m}^3/\text{s} //$$

(3) Orifice diameter =  $15\text{cm} = 0.15\text{m}$

$$A_0 = \text{Orifice area} = 0.0176\text{m}^2$$

Pipe diameter =  $30\text{cm} = 0.3\text{m}$

$$A_1 = \text{Pipe area} = 0.071\text{m}^2$$

$C_d = 0.64$

Sp. g =  $0.9$  (oil)

Reading of differential manometer =  $50\text{cm}$  of mercury

=  $0.5\text{m}$  of mercury

$$h = y \left( \frac{\rho_m}{\rho} - 1 \right)$$

$$h = 0.5 \left( \frac{13.6}{0.9} - 1 \right)$$

$$h = 7.06$$

$$\text{Discharge, } Q = \frac{C_d \times A_0 \times A_1 \times \sqrt{2gh}}{\sqrt{A_1^2 - A_0^2}}$$

$$= \frac{0.64 \times 0.0176 \times 0.071 \times \sqrt{2 \times 9.81 \times 7.06}}{\sqrt{(0.071)^2 - (0.0176)^2}}$$

$$= 0.1368\text{m}^3/\text{s} //$$

(4)  $V = \sqrt{2g\Delta h}$

Manometer reading =  $170\text{mm} = 0.17\text{m}$  of mercury

Sp. gravity of mercury =  $13.6$

Sp. gravity of sea water =  $1.026$

$$\Delta h = y \left( \frac{\rho_m}{\rho} - 1 \right)$$

$$\Delta h = 0.17 \left( \frac{13.6}{1.026} - 1 \right)$$

$$\Delta h = 2.0834$$

$$V = \sqrt{2 \times 9.81 \times 2.0834}$$

$$V = 6.39\text{m/s}$$

$$V = 23.004\text{km/hr}$$

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- (5) Rate of pump delivery =  $5 \text{ dm}^3/\text{min}$
- Pressure change =  $15 \text{ bar} = 15 \times 10^5 \text{ N/m}^2$
- Speed of rotation =  $1700 \text{ rev/min} = 28.33 \text{ rev/sec}$
- nominal displacement =  $10 \text{ cm}^3/\text{rev}$
- Torque input =  $15 \text{ Nm}$

(i) Volumetric efficiency =  $\frac{\text{Actual flow rate}}{\text{Ideal flow rate}} \times 100\%$

shaft power =  $15 \times 178.09 = 2671.35 \text{ watts}$

Actual flow rate =  $5 \text{ dm}^3/\text{min}$   
 $\frac{5 \text{ dm}^3 \times 1 \text{ m}^3}{1 \text{ min} \times 1000 \text{ dm}^3 \times 60 \text{ sec}}$

(iv) Overall efficiency?  
 $= \frac{\text{fluid power}}{\text{shaft power}} \times 100$

$5 \text{ dm}^3/\text{min} = 8.33 \times 10^{-5} \text{ m}^3/\text{sec}$   
 nominal displacement =  $\frac{10 \text{ cm}^3 \times 1 \text{ m}^3}{\text{rev} \times 1000 \text{ cm}^3} = 1 \times 10^{-5} \text{ m}^3/\text{rev}$

$= \frac{124.95}{178.09} \times 100 = 70\%$

Ideal flow rate =  $\frac{\text{nominal displacement}}{\text{speed}} \times \text{pressure}$   
 $= 1 \times 10^{-5} \times 28.33 = 2.833 \times 10^{-4}$

$= \frac{124.95}{2671.35} \times 100 = 4.67\%$

Volumetric efficiency =  $\frac{8.33 \times 10^{-5}}{2.833 \times 10^{-4}} \times 100 = 29.4\%$

(ii) Fluid power = Actual flow rate  $\times$  pressure  
 $= 8.33 \times 10^{-5} \times 15 \times 10^5 = 124.95 \text{ watts or Nm/sec}$

(iii) shaft power = Torque input  $\times$  angular speed

Torque input =  $15 \text{ Nm}$   
 Angular speed =  $2\pi N = \omega$  (rps)  
 $\omega = \frac{2\pi N}{60}$  (rpm)

$\omega = 2 \times \frac{22}{7} \times \frac{1700}{60} = 178.09 \text{ rad/sec}$

