

ACQUIBI HABIB

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PETROLIUM ENGINEERING



$$\frac{P_1 + \rho_1 V_1^2}{\rho_1} + z_1 = \frac{P_2}{\rho_1} + \frac{V_2^2}{2g} + z_2 + h_L$$

$$\frac{P_2}{\rho_1} = \frac{P_1}{\rho_1} + \frac{\rho_1 V_1^2}{2g} + (z_1 - z_2) - \frac{0.55(V_1 - V_2)^2}{2g}$$

$$\frac{P_2}{\rho_1} = 2.5 + 1.07 + 2.0 - 0.161$$

$$\frac{P_2}{\rho_1} = 5.409 \text{ m}$$

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$$V_{inlet} = d = 20 \text{ cm}$$

$$A = \frac{\pi d^2}{4}$$

$$= 0.0314 \text{ m}^2$$

$$A = 17.662 \text{ N/m}^2$$

$$= 17.662 \times 10^3 \text{ N/m}^2$$

$$C_d = 0.98$$

Theor diameter $d = 10$

$$A = \frac{\pi d^2}{4}$$

$$= 7.85 \times 10^{-3} \text{ m}^2$$

To get h

$$\frac{P_1 - P_2}{\rho_1 g} = h$$

$$P_1 = 17.662 \times 10^3 \text{ N/m}^2$$

$$P_2 = 9.81 \times 10^3 \text{ N/m}^2$$

Local Vacuum Pressure

$$= 30 \text{ cm of Hg}$$

$$= 0.5 \text{ mHg}$$

$$\frac{P_2}{w} = -9.08 \text{ (same vacuum pressure)}$$

$$\text{Then } \frac{P_1}{w} = \frac{17.628 \times 10^4}{9.81 \times 10^3} = 18$$

$$\frac{P_1}{w} - \frac{P_2}{w} = 18 - (-9.08) = 27.08$$

$$Q = C_d a v_0 \sqrt{\frac{2g h}{(m^2 - a^2)}}$$

$$= 2.4156 \times 10^{-4} \times 684.59 \\ = 0.1659 \text{ m}^3/\text{s}$$

$$\Rightarrow d_0 = 15 \text{ cm}$$

$$A_0 = \frac{\pi \times (15 \times 10^{-2})^2}{4}$$

$$\text{Pipe diameter} = 30 \text{ cm}$$

$$A_P = \frac{\pi \times (30 \times 10^{-2})^2}{4}$$

$$\text{D.P. Co of } C_{d1} = 0.95$$

Coefficient of discharge = 0.74

Reading of differential = 50 cm Hg

Differential head $h = y \left[\frac{S_{oil}}{S_w} - 1 \right]$

$$516 = 15.6$$

$$y = 50 \times 10^{-2}$$

$$h = 50 \times 10^{-2} \left[\frac{15.6}{1} - 1 \right]$$

$$h = 4.05 \text{ cm}$$

$$Q = C_d A_0 A_1 \sqrt{\frac{2gH}{A_0^2 - A_1^2}}$$

$$= 0.61 \times 10^{-4} \times 0.161 \times \sqrt{2 \times 9.81 \times 7.065} / \sqrt{(0.0706)^2 - (0.0176)^2}$$

$$= 0.1574 \text{ m}^3/\text{s}$$

4 $y = 170 \text{ mmHg} = 0.17 \text{ mHg}$, $5 \cdot g \cdot Hg = 13.6$, $5 \cdot g \cdot 5W = 1.026$

$$\Delta h = y \left(\frac{5 \cdot g \cdot Hg}{5 \cdot g \cdot W} - 1 \right)$$

$$\Delta h = 2.08 \text{ m}$$

$$V = \sqrt{2g \Delta h}$$

$$V = \sqrt{2 \times 9.81 \times 2.08}$$

$$V = 6.388 \text{ m/s}$$

5 $Q = 8.93 \times 10^{-5} \text{ m}^3/\text{s} \cdot C$

Speed of rotation = 28.3 rev/sec

Normal displacement = $10^{-5} \text{ m}^3/\text{rev}$

Torque limit = 15 Nm

Pressure change = $15 \times 10^5 \text{ N/m}^2$

Ideal flow rate = Normal displacement \times speed of rotation = $2.89 \times 10^{-4} \text{ m}^3/\text{sec}$

a Volumetric efficiency = $\frac{\text{Actual flow rate}}{\text{Ideal flow rate}} \times 100$

$$= 29.75\%$$

b fluid flow rate, $A = Q \times \Delta P$

$$8.93 \times 10^{-5} \times 15 \times 10^5$$

$$= 124.95 \text{ Watts}$$

c Shaft Power $\rightarrow \tau \times \omega$

$$\omega = 2 \times \pi \times \text{speed of rotation}$$

$$\omega = 197.9 \text{ rad/sec}$$

$$\text{Shaft Power} = 15 \times 197.9$$

$$= 2967.2 \text{ Watts}$$

d Overall Efficiency = $\frac{\text{fluid Power}}{\text{Shaft Power}} \times 100$

$$= \frac{124.05}{2967.2} \times 100$$

$$= 4.18\%$$

$$= 4.68\%$$