

1) $V_1 = 5 \text{ m/s}$ $V_2 = 2 \text{ m/s}$
 smaller end = 2.5m $l = 2.0$
 $h_1 = \frac{0.35(V_1 - V_2)^2}{2g}$

$$L = b_1 - b_2 = 2 \text{ m}$$

$$\frac{P_1}{\rho} + \frac{V_1^2}{2g} + z_1 = \frac{P_2}{\rho} + \frac{V_2^2}{2g} + z_2$$

$$\frac{P_2}{\rho} = \frac{P_1}{\rho} + \frac{1}{2g} (V_1^2 + V_2^2) + (z_1 - z_2)h$$

$$= 2.05 + \frac{(5^2 - 2^2)}{2 \times 9.81} + 2 = \frac{(0.35(5-2)^2)}{2 \times 9.81}$$

$$= 2.05 + 1.07 + 2 = 0.16055$$

$$P_2 = 5.409 \text{ bar}$$

Pressure at lower end
 $= 5.409 \text{ bar}$

2) Inlet diameter = ~~200m~~ 20 cm

Throat diameter = 10 cm

$$C_d = 0.98$$

Initial $P_1 = 17.658 \text{ N/cm}^2$

$$A_1 = \frac{\pi d^2}{4} = \frac{1}{4} \times \left(\frac{20}{100}\right)^2 \times \pi$$

$$= 0.0314 \text{ m}^2$$

$$A_2 = \frac{\pi d^2}{4} = \frac{1}{4} \times \left(\frac{10}{100}\right)^2 \times \pi$$

$$= 7.85 \times 10^{-3} \text{ m}^2$$

If $y = 30 \text{ cm}$ (0.3m of mercury)

$$P_1 = 17.658$$

$$= \frac{17.658}{1000} = 1.7658 \times 10^{-3} \text{ N/m}^2$$

$$\frac{P_1}{\rho} = \frac{1.7658 \times 10^{-3}}{9.81} = 1.8 \times 10^{-4} \text{ m}$$

$$\frac{P_2}{\rho} = 0.3 \times 13.6 = 4.08$$

$$h = \frac{P_1}{\rho} - \frac{P_2}{\rho} = 1.8 \times 10^{-4} - (-4.08)$$

$$= 4.08018 \text{ m}$$

$$Q = C_d \times \frac{A_1 A_2}{\sqrt{A_1 A_2}} \times \sqrt{2gh}$$

$$Q = 0.98 \times \frac{0.0314 \times 7.85 \times 10^{-3}}{\sqrt{0.0314 \times 7.85 \times 10^{-3}}} \times \sqrt{2 \times 9.81 \times 4.08}$$

$$= 0.070 \text{ m}^3/\text{s}$$

3) $D_1 = 15 \text{ cm}$ $D_2 = 30 \text{ cm}$

50 cm = 0.5m of mercury

$$S.G = 0.9 \quad C_d = 0.64$$

$$A_1 = \frac{\pi d^2}{4} = \frac{1}{4} \times \left(\frac{15}{100}\right)^2 \times \pi$$

$$= 0.0176 \text{ m}^2$$

$$A_2 = \frac{\pi d^2}{4} = \frac{1}{4} \times \left(\frac{30}{100}\right)^2 \times \pi$$

$$= 0.0706 \text{ m}^2$$

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$$h = \sqrt{\left(\frac{13.6}{0.4} - 1\right)} = 6.54 \left(\frac{13.6}{0.4} - 1\right) = 7.055$$

$$Q = C_d \times A_1 A_2 \times \sqrt{2gh} \times \frac{\sqrt{A_1^2 - A_2^2}}{\sqrt{A_1^2 - A_2^2}}$$

$$= 0.64 \times \frac{(0.0176 \times 0.0706)}{\sqrt{(0.0176)^2 - (0.0706)^2}} \times \sqrt{2 \times 9.81 \times 7.055}$$

$$= 2.83 \times 10^{-3} \text{ m}$$

4) Orifice diameter = 15 cm

Pipe diameter =

1700 mm of mercury = 0.17

S.G. of mercury = 13.6

S.G. of sea water = 1.026

$$h = \sqrt{\left(\frac{\text{S.G. of mercury} - 1}{\text{S.G. of sea water}} - 1\right)}$$

$$h = 0.17 \left(\frac{13.6}{1.026} - 1\right)$$

$$= 2.083$$

$$V = \sqrt{2gh} = \sqrt{2 \times 9.81 \times 2.083}$$

$$= 6.39 \text{ m/s}$$

$$5) Q = 0.65 \text{ dm}^3/\text{min}$$

$$= 8.33 \times 10^{-5} \text{ m}^3/\text{s}$$

$$\text{Speed of rotation} = 1700 \text{ rev/min}$$

$$= 28.3 \text{ rev/s}$$

$$\text{Nominal displacement} = 10 \frac{\text{cm}^3}{\text{rev}}$$

$$= 10^{-5} \frac{\text{m}^3}{\text{rev}}$$

$$\text{Torque Input} = 15 \text{ Nm}$$

$$\text{Pressure change} = 15 \text{ bar} = 15 \times 10^5 \text{ N/m}^2$$

Ideal Flowrate = Nominal displacement \times speed rotation

$$= 10^{-5} \times 28.3$$

$$= 2.83 \times 10^{-4} \text{ m}^3/\text{s}$$