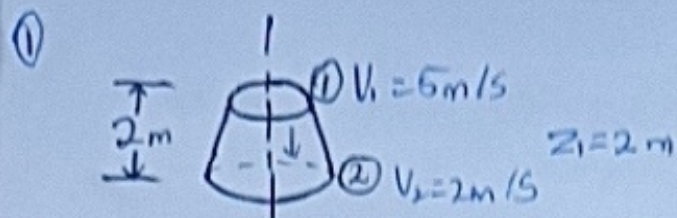


SHEKONI OLUDASEYI TAN

BIOMEDICAL ENGINEERING 15/ENCL02/087

ENCL214 ASSIGNMENT



$$\frac{P_1}{\rho} = 2.5 \text{ m}, \text{ Heat loss, } H_L = \frac{0.35(V_1 - V_2)^2}{2g}$$

$$H_L = \frac{0.35(5-2)^2}{2 \times 9.81} = 0.16 \text{ m}$$

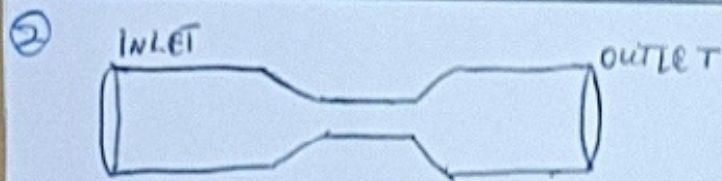
$$\frac{P_1}{\rho} + \frac{V_1^2}{2g} + Z_1 = \frac{P_2}{\rho} + \frac{V_2^2}{2g} + Z_2 + H_L$$

$$2.5 + 1.27 + 2 = \frac{P_2}{\rho} + 0.203 + 2 + 0.16$$

$$\frac{P_2}{\rho} = 2.5 + 1.27 + 2 - (0.203 + 0.16)$$

$$\frac{P_2}{\rho} = 5.77 - 0.363$$

$$= 5.407 \text{ m of liquid}$$



Inlet;

$$d_1 = 20 \text{ cm} = 0.2 \text{ m}$$

$$A_1 = \frac{\pi d_1^2}{4} = \frac{\pi \times 0.2^2}{4} = 0.0314 \text{ m}^2$$

$$P_1 = 17.658 \text{ N/cm}^2 = 176580 \text{ N/m}^2$$

throat diameter,

$$d_2 = 10 \text{ cm} = 0.1 \text{ m}$$

$$A_2 = \frac{\pi d_2^2}{4} = \frac{\pi \times 0.1^2}{4} = 7.85 \times 10^{-3} \text{ m}^2$$

$$h = \frac{P_1}{\rho} - \frac{P_2}{\rho}$$

$$P_1 = 176580 \text{ N/m}^2, \rho = 9810 \text{ kg/m}^3$$

$$\frac{P_2}{\rho} = 30 \text{ cm Hg} = 0.3 \text{ m Hg}$$

$$= 0.3 \times 13.6 = 4.08$$

$$\frac{P_2}{\rho} = -4.08$$

$$\frac{P_1}{\rho} = \frac{176580}{9810} = 18.01$$

$$\frac{P_1}{\rho} - \frac{P_2}{\rho} = 18.01 - (-4.08) = 22.09$$

$$Q = C_d A_1 A_2 \sqrt{\frac{2gh}{A_1^2 - A_2^2}}$$

$$Q = 0.98 \times 0.0314 \times 7.85 \times 10^{-3} \times \sqrt{\frac{2 \times 9.81 \times 22.09}{(0.0314^2 - (7.85 \times 10^{-3})^2)}}$$

$$Q = 0.1653 \text{ m}^3/\text{s}$$

③ $d_0 = 15 \text{ cm} = 0.15 \text{ m}$

$$A_0 = \frac{\pi \times 0.15^2}{4} = 0.01767 \text{ m}^2$$

$$d_p = 30 \text{ cm} = 0.3 \text{ m}$$

$$A_p = \frac{\pi \times 0.3^2}{4} = 0.07069 \text{ m}^2$$

$$\text{S.P.G. of oil} = 0.9$$

$$C_d = 0.64$$

$$\text{Reading of differential} = 60 \text{ cm Hg}$$

$$\text{Differential head } h = y \left[\frac{S_L h_L}{S_0} - 1 \right]$$

$$S_L h_L = 13.6$$

$$y = 50 \times 10^{-2}$$

$$h = 50 \times 10^{-2} \left[\frac{13.6}{0.9} - 1 \right]$$

$$h = 0.5 \times 14.11 = 7.055 \text{ m}$$

$$Q = \frac{C_d A_0 A_p \sqrt{2gh}}{\sqrt{A_p^2 - A_0^2}}$$

$$= \frac{0.64 \times 0.01767 \times 0.07069 \times \sqrt{2 \times 9.81 \times 7.055}}{\sqrt{(0.07069^2) - (0.01767^2)}}$$

$$= 0.1374 \text{ m}^3/\text{s}$$

$$\textcircled{4} \quad y = 170 \text{ mmHg} = 0.17 \text{ mHg}$$

$$S \cdot g \text{ Hg} = 13.6, S \cdot g \text{ sw} = 1.026$$

$$\Delta h = y \left(\frac{S \cdot g \text{ Hg}}{S \cdot g \text{ sw}} - 1 \right)$$

$$\Delta H = 0.17 \left(\frac{13.6}{1.026} - 1 \right)$$

$$\Delta H = 2.08 \text{ m}$$

$$V = \sqrt{2g\Delta h}$$

$$V = \sqrt{2 \times 9.81 \times 2.08}$$

$$V = 6.388 \text{ m/s}$$

$\textcircled{5}$

$$Q = 0.05 \text{ dm}^3/\text{min} = 8.33 \times 10^{-5} \text{ m}^3/\text{sec}$$

$$\text{Speed of rotation} = 1700 \text{ Rev/min} = 28.3 \text{ Rev/sec}$$

$$\text{Nominal Displacement} = 10 \text{ cm}^3/\text{rev} = 10^{-5} \text{ m}^3/\text{rev}$$

$$\text{Torque Input} = 15 \text{ Nm}$$

$$\text{Pressure Charge} = 15 \text{ bar} = 15 \times 10^5 \text{ N/m}^2$$

$$\text{Ideal Flowrate} = \text{Nominal displacement} \times \text{Speed of rotation}$$

$$= 10^{-5} \times 28.3 = 2.83 \times 10^{-4} \text{ m}^3/\text{sec}$$

\textcircled{a} Volumetric Efficiency

$$= \frac{\text{Actual flowrate}}{\text{Ideal flowrate}} \times 100$$

$$= \frac{8.33 \times 10^{-5}}{2.83 \times 10^{-4}} \times 100 = 29.45\%$$

\textcircled{b} Fluid Power,

$$P_f = Q \times \Delta P = 8.33 \times 10^{-5} \times 15 \times 10^5$$

$$= 124.95 \text{ watts}$$

\textcircled{c} Shaft Power

$$\Rightarrow T \times \omega$$

$$\omega = 2\pi \times \text{speed of rotation}$$

$$\omega = 2\pi \times 28.3 = 177.81 \text{ rad/sec}$$

$$\text{Shaft Power} = 15 \times 177.81$$

$$= 2667.2 \text{ watts}$$

\textcircled{d} Overall efficiency

$$\Rightarrow \frac{\text{Fluid Power}}{\text{Shaft Power}} \times 100$$

$$= \frac{124.95}{2667.2} \times 100 = 4.68\%$$