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COMPUTER ENGINEERING

FLUID MECHANICS (ENG 214)

1. Pressure head at smaller end = 2.5 m

Length of tube = 2.0 m (TL)

Velocity of flow at lower end = 5 m s^{-1} (v_1)

Velocity of flow at higher end = 2 m s^{-1} (v_2)

$$\Rightarrow \text{loss of head} = \frac{0.35(v_1 - v_2)^2}{2g} h_L$$

$$\Rightarrow \text{loss of head} = \frac{0.35(5-2)^2}{2 \times 9.81} = 0.16 \text{ m}$$

\Rightarrow pressure head at higher end $\frac{P_2}{\rho}$

$$= \frac{P_1}{\rho} + \frac{v_1^2}{2g} + z_1 = \frac{P_2}{\rho} + \frac{v_2^2}{2g} + z_2 + h_L$$

$$z_2 = 0, \quad z_1 = 2.0 \text{ m} //$$

$$\Rightarrow 2.5 + \frac{5^2}{2 \times 9.81} + 2 = \frac{P_2}{\rho} + \frac{2^2}{2 \times 9.81} + 0.16$$

$$= 5.275 = \frac{P_2}{\rho} + 0.364 =$$

$$\frac{P_2}{\rho} = 5.275 - 0.364 = 5.41 \text{ m at liquid.}$$

Pressure head at higher end = 5.41 m //

2. Inlet diameter = 20 cm = 0.2 m

Throat diameter = 10 cm = 0.1 m

Pressure at inlet = $17.658 \text{ N/cm}^2 = 176.58 \text{ kN/m}^2$

30 cm of mercury

COD = 0.98

Solution:

Area of inlet = $A_1 = \frac{\pi}{4} \times 0.2^2 = 0.0314 \text{ m}^2$

Area of throat = $\frac{\pi}{4} \times 0.1^2 = 0.00785 \text{ m}^2$

$\Rightarrow P_1/w = 176.58/9.8 = 18.01 \text{ m}$

Vacuum pressure at the throat

$P_2/w = -300 \text{ mm} = -0.3 \times 13.6 = -4.08 \text{ of water}$

Differential head, $h = \frac{P_1}{w} - \frac{P_2}{w} = 18.01 - (-4.08) = 22.09 \text{ m}$

\Rightarrow Rate of flow, Q

Using the relation, $Q = C_d \times \frac{A_1 A_2}{\sqrt{A_1^2 - A_2^2}} \times \sqrt{2gh}$

$\therefore Q = \frac{0.98 \times 0.0314 \times 0.00785}{\sqrt{(0.0314)^2 - (0.00785)^2}} \times \sqrt{2 \times 9.81 \times 22.09}$

$Q = \frac{0.00241}{0.00304} \times 20.82$

$Q = 0.165 \text{ m}^3/\text{s}$

\therefore Discharge of water through Venturimeter = $0.165 \text{ m}^3/\text{s}$

3. Orifice diameter $A_0 = 15 \text{ cm} = 0.15 \text{ m}^2$
 Pipe diameter $= 30 \text{ cm} = 0.3 \text{ m}^2$
 Manometer reading $= 0.5 \text{ m}$ of mercury
 S.G. of oil $= 0.9$, $C_{od} = 0.64$

Solution:

$$\text{Area of Orifice} = \frac{\pi}{4} \times 0.15^2 = 0.0177 \text{ m}^2 = A_0$$

$$\text{Area of pipe} = \frac{\pi}{4} \times 0.30^2 = 0.0707 \text{ m}^2 = A_1$$

$$\text{Difference in head, } h = y \left[\frac{S_H L}{S_0} - 1 \right]$$

$$= 0.5 \left[\frac{13.6}{0.9} - 1 \right] = 7.06 \text{ m of oil}$$

\Rightarrow Discharge Q

Using the equation, $Q = C_d \times A_0 \times A_1 \times \sqrt{\frac{2gh}{A_1^2 - A_0^2}}$

$$Q = 0.64 \times 0.0177 \times 0.0707 \times \sqrt{\frac{2 \times 9.8 \times 7.06}{(0.0707)^2 - (0.0177)^2}}$$

$$= \frac{0.0942}{0.707} = 0.133 \text{ m}^3/\text{s}$$

Rate of discharge $= 0.133 \text{ m}^3/\text{s}$

4. Reading at manometer, $y = 170 \text{ mm} = 0.17 \text{ m}$

Sp of gravity of mercury, $S_{hg} = 13.6$

Sp gravity of sea water, $S_w = 1.026$

Sp gravity

Find head h using the relation

$$h = y \left[\frac{S_{hg}}{S_w} - 1 \right]$$

$$h = 0.17 \left[\frac{13.6}{1.026} - 1 \right] = 2.05$$

\therefore Speed of submarine

$$v = \sqrt{2gh} = \sqrt{2 \times 9.81 \times 2.05}$$

$$v = 6.38 \text{ m/s}$$

iii) Shaft power $= T \cdot \omega$

where $T = \text{torque}$

$\omega = \text{angular speed}$

$$T = 15 \text{ Nm}, \quad \omega = 2 \text{ rev for } 1 \text{ rev}$$

$$\omega = \frac{2 \text{ rev}}{60} \text{ for } 1 \text{ rev}$$

$$\omega = 2 \times \frac{32}{7} \times 28.3 = 177.89 \text{ rad/s}$$

$$\therefore \text{ shaft power} = 15 \times 177.89$$

$$= 2668.35 \text{ watts}$$

5. Actual flow rate $= 0.25 \text{ m}^3/\text{min}$

pressure charge $= 156 \text{ bar}$

Speed of rotation $= 1700 \text{ rev/min}$

Normal displacement $= 10 \text{ cm}^3/\text{rev}$

Torque $= 15 \text{ Nm}$

$$\text{Ideal flow rate} = 28.3 \times 10^{-4} \times 1700$$

$$= 2.83 \times 10^{-4} \text{ m}^3/\text{sec}$$

iv) Overall efficiency

$$= \frac{\text{Fluid power}}{\text{shaft power}} \times 100$$

$$= \frac{1245}{2668.35} \times 100$$

$$= 46.66\%$$

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i) Volumetric efficiency $= \frac{\text{Actual rate} \times 100}{\text{Ideal rate}}$

$$= \frac{0.25 \times 10^{-3}}{2.83 \times 10^{-4}} \times 100 = 29.6\%$$

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ii) Fluid power $= Q \cdot \Delta p$

$$= 0.25 \times 10^{-3} \times 15 \times 10^5$$

$$= 1245 \text{ watts}$$