

CHUKWEMERIE MARVELLOUS

M/ENG05/009

MECHATRONICS ENGINEERING

MCT 322

QUESTION 1

1. $\mu = 0.9 \text{ Poise} = 0.09 \text{ N}\cdot\text{s}/\text{m}^2$

Relative density = 0.9 Density = 0.9×1000

Weight density = $0.9 \times 9810 = 8829 \text{ N}/\text{m}^3$

Diameter = $120 \text{ mm} = 0.12 \text{ m}$

$L = 12 \text{ m}$ $A = (\pi/4) (0.12)^2$

Weight of oil in 25secs = 785 N

$$Re = \frac{\rho V D}{\mu} \dots \dots (1)$$

$$V = \bar{u} \dots \dots (2)$$

$$\bar{u} = \frac{Q}{A} \dots \dots (3)$$

$$\frac{N}{s} = \frac{N}{\text{m}^3} \times \frac{\text{m}^3}{s} \dots \dots (4)$$

$$\frac{N}{s} = W \times Q$$

$$\frac{785}{25} = 8829 \times Q$$

$$Q = \frac{8829 \times 25}{785} \times \frac{1}{8829}$$

$$Q = 3.55 \times 10^{-3}$$

sub $Q = 3.55 \times 10^{-3}$ in (3)

$$\bar{u} = \frac{3.55 \times 10^{-3}}{(\bar{u}/4)(0.12)^2}$$

$$\bar{u} = 0.314 \text{ m/s}$$

Recall $v = \bar{u} = 0.314$

$$\therefore Re = \frac{(0.9 \times 1000) \times 0.314 \times 0.12}{0.09}$$

$$Re = 376.8$$

Pressure difference

$$(p_1 - p_2) = \frac{32\mu UL}{D^3}$$
$$= \frac{32 \times 0.09 \times 0.314 \times 12}{(0.12)^3}$$

$$p_1 - p_2 = \underline{753.6 \text{ N/m}^2}$$

$$h_f = \frac{p_1 - p_2}{\rho g} = \frac{753.6}{8829} = 0.085 \text{ m of oil}$$

QUESTION 2

Diameter of pipe, $D = 60 \text{ mm} = 0.06 \text{ m}$

Length of the pipe, $L = 850 \text{ m}$

Discharge, $Q = \text{8.5 lit/sec} = 0.0085$

kinematic viscosity of water, $\nu = 0.015 \text{ stokes} = 0.015 \times 10^{-4} \text{ m}^2/\text{s}$

$$\text{Mean velocity } V = \frac{Q}{A} = \frac{0.0085}{\frac{\pi}{4} \times (0.06)^2} = 3.0 \text{ m/s}$$

$$Re = \frac{VD}{\nu} = \frac{3.0 \times 0.06}{0.015 \times 10^{-4}} = 3600 \quad 120,000$$

$$f = \frac{0.0791}{Re^{1/4}} = \frac{0.0791}{120000^{1/4}} = 0.01021 \quad 4.2499 \times 10^{-3}$$

$$(i) \quad h_f = \frac{4fLV^2}{D \times 2g} = 4 \times \frac{0.01021 \times 850 \times 3^2}{0.06 \times 2 \times 9.81} = 4 \times \frac{4.2499 \times 10^{-3} \times 850 \times 3^2}{0.06 \times 2 \times 9.81}$$

$$h_f = 110.47 \text{ m}$$

$$(ii) \quad \tau_0 = \frac{fV^2\rho}{2} = 4 \times \frac{4.2499 \times 10^{-3} \times 3^2 \times 1000}{2}$$

$$\tau_0 = 19.12 \text{ N/m}^2$$

$$(iii) \quad Re = 120,000$$

(iv) Turbulent flow