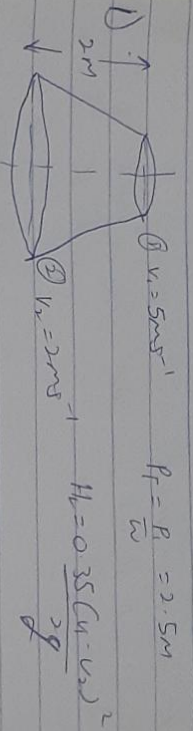


Kibardu Benedict I

184FN17086036

Mechanical engineering

Fluid mechanics assignment.



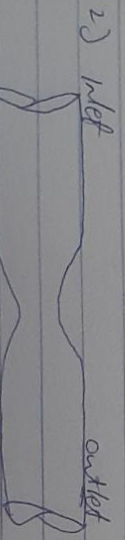
$$\frac{P_1}{\rho} + \frac{v_1^2}{2g} + z_1 = \frac{P_2}{\rho} + \frac{v_2^2}{2g} + z_2 + H_L$$

$$\frac{P_2}{\rho} = \frac{P_1}{\rho} - \frac{v_1^2 - v_2^2}{2g} + (z_1 - z_2) - 0.35 \frac{(v_1 - v_2)^2}{2g}$$

$$\frac{P_2}{\rho} = 2.5 + \frac{5^2 - 2^2}{2 \times 9.81} + 2 - 0.35 \frac{(5 - 2)^2}{2 \times 9.81}$$

$$\frac{P_2}{\rho} = 2.5 + 1.07 + 2 - 0.161$$

$$\frac{P_2}{\rho} = 5.409 \text{ m of liquid.}$$



Inlet,  $d = 20 \text{ cm} = 20 \times 10^{-2} \text{ m}$

$$A = \frac{\pi d^2}{4} = \frac{\pi \times (20 \times 10^{-2})^2}{4}$$

$A_1 = 0.314 \text{ m}^2$  throat diameter,  $d_2 = 10 \text{ cm} = 10 \times 10^{-2} \text{ m}$

$$P_1 = 17.668 \text{ N/cm}^2 \quad A = \frac{\pi d^2}{4} = \frac{\pi \times (10 \times 10^{-2})^2}{4}$$

$$Q = 0.98 \quad A_2 = 7.85 \times 10^{-3} \text{ m}^2$$

$$5. Q = 0.05 \text{ liter}^{-1} = 8.33 \times 10^{-5} \text{ m}^3 \text{ sec}^{-1}$$

$$\text{Speed of rotation} = 1750 \text{ rev/min} = 28.3 \text{ rev/sec}$$

$$\text{Nominal displacement} = 100 \text{ cm}^3/\text{rev} = 10^{-5} \text{ m}^3/\text{rev}$$

$$\text{Torque input} = 15 \text{ Nm}$$

$$\text{Pressure drop} = 15 \text{ bar} = 15 \times 10^5 \text{ N/m}^2$$

$$\text{Ideal flow rate} = \text{Nominal displacement} \times \text{speed of rotation} \\ = 10^{-5} \times 28.3 = 2.83 \times 10^{-4} \text{ m}^3/\text{sec}$$

$$a) \text{ Volumetric efficiency} = \frac{\text{Actual flow rate}}{\text{Ideal flow rate}} \times 100$$

$$= \frac{8.33 \times 10^{-5}}{2.83 \times 10^{-4}} \times 100$$

$$= 29.45\%$$

$$b) \text{ Fluid power, } P_f = Q \times \Delta P = 8.33 \times 10^{-5} \times 15 \times 10^5$$

$$= 124.95 \text{ watts}$$

$$c) \text{ Shaft power, } = T \times \omega$$

$$\omega = 2\pi \times \text{speed of rotation} = 2 \times \pi \times 28.3$$

$$\omega = 177.81 \text{ rad/sec}$$

$$\therefore \text{Shaft power} = 15 \times 177.81 = 2667.2 \text{ watts}$$

$$d) \text{ Overall efficiency} = \frac{\text{Fluid power}}{\text{Shaft power}} \times 100$$

$$= \frac{124.95}{2667.2} \times 100$$

$$= 4.68\%$$

$$\text{Differential head } h = \left( \frac{5h_1}{55} - 1 \right)$$

$$5h \geq 13.6$$

$$h \geq 50 \times 10^{-2}$$

$$h = 50 \times 10^{-2} \left( \frac{13.6}{0.9} - 1 \right)$$

$$h = 50 \times 10^{-2} \times 14.11$$

$$= 7.055 \text{ m}$$

$$Q = C_d A_1 A_2 \sqrt{2gH}$$

$$= 0.64 \times 0.017 \times 0.67 \times 0.29$$

$$= \sqrt{0.07069^2} - (0.017 \times 0.67^2)$$

$$= 0.1334 \text{ m}^3 \text{ s}^{-1}$$

4.  $y = 170 \text{ mmHg} = 0.17 \text{ mHg}$ ,  $5.0 \text{ gHg} = 13.6 \times 5.0 \text{ g} = 1.026$

$$\Delta h = y \left( \frac{5 \rho_{\text{Hg}}}{\rho_{\text{fluid}}} - 1 \right)$$

$$\Delta h = 0.17 \left( \frac{13.6}{1.026} - 1 \right)$$

$$\Delta h = 2.28 \text{ m}$$

$$v = \sqrt{2g\Delta h}$$

$$v = \sqrt{2 \times 9.81 \times 2.28}$$

$$v = 6.388 \text{ m s}^{-1}$$

To get  $k$ ;

$$\frac{P_1}{\rho} - \frac{P_2}{\rho} = k$$

$$P = 17.668 \times 10^4 \text{ Nm}^{-2}$$

$$W = 9.81 \times 10^3 \text{ Nm}^{-3}$$

But we have that throat vacuum pressure = 30 cm of Hg

$$\approx 0.3 \text{ mHg}$$

$$\approx 0.3 \times 136 = 4.08$$

$$\frac{P_2}{\rho} = -4.08 \text{ (Since vacuum pressure)}$$

$$\text{Then } \frac{P_1}{\rho} = \frac{17.668 \times 10^4}{981 \times 10^3} = 18$$

$$\therefore \frac{P_1}{\rho} - \frac{P_2}{\rho} = 18 - (-4.08) = 22.08$$

$$Q = C_d A_1 A_2 \sqrt{\frac{2gk}{(A_1^2 - A_2^2)}}$$

$$0.98 \times 0.0314 \times 7.85 \times 10^{-3} \times \sqrt{\frac{2 \times 9.81 \times 22.08}{(0.0314^2 - (7.85 \times 10^{-3})^2)}}$$

$$\approx 0.4156 \times 10^{-4} \times 864.59$$

$$\approx 0.1653$$

$$Q_{\text{actual}} = 0.1653 \text{ m}^3 \text{ s}^{-1}$$

3) Orifice meter; given that

$$h_0 = 15 \text{ cm} = 0.15 \text{ m} \text{ piezometer; } A_p = 30 \text{ cm} \times 30 \text{ cm} = 900 \text{ cm}^2 = 0.09 \text{ m}^2$$

$$A_0 = 1 \text{ cm} \times 1 \text{ cm} = 1 \text{ cm}^2 = 10^{-4} \text{ m}^2 \quad A_p = \pi \times (30 \times 10^{-3})^2$$

$$\approx 0.01767 \text{ m}^2$$

$$\approx 0.007069 \text{ m}^2$$

$$S.I. Co. of discharge = 0.64$$

Coefficient of discharge = 0.64

Reading of differential = 50 cm Hg