

## Question (1)

(1) length tube

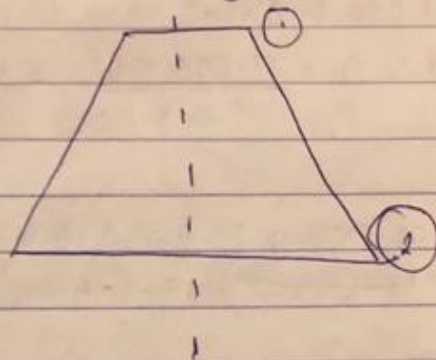
$$l = 2.0 \text{ m}$$

$$v_1 = 5 \text{ m/s}$$

$$P_1 (P_g = 2.5 \text{ m of liquid})$$

$$v_2 = 2 \text{ m/s}$$

$$\text{loss head} = h_L = \frac{0.85 (v_1 - v_2)^2}{2g}$$



$$= \frac{0.85 (5 - 2)^2}{2g} = \frac{0.85 \times 9}{2 \times 9.81} = 0.16$$

$$\text{pressure head } \frac{P_2}{P_g} = ?$$

Applying Bernoulli's equation at section (1) and (2), we get

$$\frac{P_1}{P_g} + \frac{v_1^2}{2g} + z_1 = \frac{P_2}{P_g} + \frac{v_2^2}{2g} + z_2 + h_L$$

Let the datum line passes through section (2). Then  $z_2 = 0$ ,  $z_1 = 2.0$ 

$$\frac{2.5 + 5^2}{2 \times 9.81} + 2.0 = \frac{P_2 + 2^2}{P_g \cdot 2 \times 9.81} + 0 + 0.16$$

$$2.5 + 1.27 + 2.0 = \frac{P_2}{P_g} + 0.203 + 0.16$$

$$\frac{P_2}{P_g} = (2.5 + 1.27 + 2.0) - (0.203 + 0.16)$$

$$= 5.77 - 0.363 = 5.407 \text{ m of fluid.}$$

## Question 2

Solution

Dia at inlet

$$d_1 = 20 \text{ cm}$$

$$a_1 = \frac{\pi}{4} \times (20)^2 = 314.16 \text{ cm}^2$$

$$d_2 = 10 \text{ cm}$$

$$a_2 = \frac{\pi}{4} \times 10^2 = 78.54 \text{ cm}^2$$

$$P_1 = 17.658 \text{ N/cm}^2 = 17.658 \times 10^4 \text{ N/m}^2$$

$$= 1000 \frac{\text{kg}}{\text{m}^3} \text{ and } \therefore \frac{P_1}{\rho g} = \frac{17.658 \times 10^4}{9.81 \times 1000} = 18 \text{ m of water}$$

$$P_2 = -30 \text{ cm of mercury}$$

$$\frac{P_2}{\rho g} = -0.30 \text{ m of mercury} = -0.30 \times 13.6 = -4.08 \text{ m of water}$$

$$\therefore h = \frac{P_1}{\rho g} - \frac{P_2}{\rho g} = 18 - (-4.08)$$

$$= 18 + 4.08 = 22.08 \text{ m of water} = 220.8 \text{ cm}$$

of water

The discharge  $Q$  is given by equation (6.8)

$$Q = C_d a_1 a_2 \times \sqrt{2gh}$$

$$= 0.98 \times \frac{314.16 \times 78.54}{\sqrt{(314.16)^2 - (78.54)^2}} \times \sqrt{2 \times 9.81 \times 220.8}$$

$$= \frac{50328837.21}{304} \times 165555 \text{ cm}^3/\text{s} = 165.555 \text{ lit/s}$$

### Question 3

solo

$$A_0 = \frac{\pi}{4} (15)^2 = 176.714 \text{ cm}^2 \text{ (} A_0 \text{ area of orifice)}$$

$$A_p = \frac{\pi}{4} (30)^2 = 706.858 \text{ cm}^2 \text{ (} A_p \text{ area of the pipe)}$$

$$h = \left[ \frac{13.6 - 1}{0.9} \right] \times 50 \text{ cm of oil}$$

$$= 705.555 \text{ cm of oil}$$

$$Q = C_d \frac{A_0 A_p}{\sqrt{A_p^2 - A_0^2}} \sqrt{2gh}$$

$$Q = \left( 0.64 \times \frac{176.714 \times 706.858}{\sqrt{706.858^2 - 176.714^2}} \times \sqrt{2 \times 9.81 \times 7.0555 \times 100} \right) \text{ cm}^3/\text{s}$$

$$Q = 137414.25 \text{ cm}^3/\text{sec}$$

$$Q = 137.41425 \text{ lts/sec}$$

### Question 4

Diff of Mercury level  $x = 170 \text{ mm} = 0.17 \text{ m}$

sp. gr. of Mercury  $s_g = 13.6$

sp. gr. of sea water  $s_0 = 1.026$

$$h = x \left[ \frac{s_g - 1}{s_0} \right] = 0.17 \left[ \frac{13.6 - 1}{1.026} \right] = 2.0834 \text{ m}$$

$$V = \sqrt{2gh} = \sqrt{2 \times 9.81 \times 2.0834} = 6.393 \text{ m/s}$$

$$= \frac{6.393 \times 60 \times 60}{1000} \text{ km/hr} = 23.017 \text{ km/hr}$$