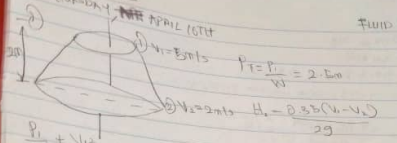


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MEX HARDENIC

THURSDAY, 17 APRIL 2014

FLUID MECHANICS

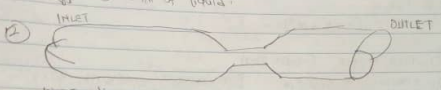


$$\frac{P_1}{\rho} + \frac{v_1^2}{2} + Z_1 = \frac{P_2}{\rho} + \frac{v_2^2}{2} + Z_2 + H$$

$$\frac{P_2}{\rho} - \frac{P_1}{\rho} = \frac{v_1^2 - v_2^2}{2} + 2 - 0.25(5 - 2)^2$$

$$\frac{P_2}{\rho} = 2.5 + 1.09 + 2 \cdot 0.161$$

$$\frac{P_2}{\rho} = 5.49 \text{ m of liquid.}$$



INLET = di. 20 cm =  $20 \times 10^{-2} \text{ m}$

$$A = \frac{\pi d^2}{4} = \frac{\pi \times (20 \times 10^{-2})^2}{4}$$

+ THROAT DIAMETER

$$A_1 = 0.0314 \text{ m}^2$$

$$P_1 = 17.662 \text{ N/cm}^2 = 17.662 \times 10^4 \text{ N/m}^2$$

$$Cd = 0.98$$

$$A_2 = 7.25 \times 10^{-3} \text{ m}^2$$

To get h,

$$\frac{P_1}{\rho} - \frac{P_2}{\rho} = h$$

$$P_1 = 17.662 \times 10^4 \text{ N/m}^2$$

$$W = 9.81 \times 10^3 \text{ N/m}^3$$

But we have that at throat vacuum pressure

$$= 20 \text{ cm of Hg}$$

$$= 0.2 \text{ m Hg}$$

$$= 0.3 \times 13.6 = 4.08$$

$$P_2 = -4.08 \text{ cmHg vacuum pressure}$$

$$\text{then } \frac{P_1}{\rho} = \frac{17.662 \times 10^4}{9.81 \times 10^3} = 18$$

$$\frac{P_1}{\rho} - \frac{P_2}{\rho} = 18 - (-4.08) = 22.08$$

$$Q = C_d A_2 A_1 \sqrt{\frac{2gH}{C_d^2 A_1^2 - A_2^2}}$$

$$= 0.98 \times 0.0314 \times 7.25 \times 10^{-3} \times \sqrt{\frac{2 \times 9.81 \times 22.08}{(0.0314)^2 - (7.25 \times 10^{-3})^2}}$$

$$= 2.4156 \times 10^{-4} \times 624.39$$

$$= 0.1652$$

$$Q_{\text{actual}} = 0.1652 \text{ m}^3/\text{s}$$

3) Orifice meter; Given that  
 $d_o = 15 \text{ mm} = 15 \times 10^{-2} \text{ m}$  Pipe diameter,  $d_p = 30 \text{ mm} = 30 \times 10^{-2} \text{ m}$   
 $A_o = \frac{\pi \times (15 \times 10^{-2})^2}{4}$   
 $A_p = \frac{\pi \times (30 \times 10^{-2})^2}{4}$   
 $= 0.01767 \text{ m}^2$   
 SpG of oil = 0.96 = 0.0706  $\text{m}^3$   
 Coefficient of discharge = 0.64  
 Reading of differential = 100 mmHg

Differential head  $h_1 = \left( \frac{101}{50} - 1 \right)$

$$50 h_1 = 13.6$$

$$50 \times 10^{-2} \left[ \frac{13.6}{0.9} - 1 \right]$$

$$h = 60 \times 10^{-2} \text{ m} = 0.6 \text{ m}$$

$$= 7.032 \text{ m}$$

$$Q = C_d A_1 A_2 \sqrt{2gh}$$

$$\sqrt{A_1^2 - A_2^2}$$

$$= \frac{0.84 \times 0.01767 \times 0.01767 \times \sqrt{2 \times 9.81 \times 0.6}}{\sqrt{(0.01767^2) - (0.01767^2)}}$$

$$= 3.77 \times 10^{-3} \times 11.765$$

$$\sqrt{4.62 \times 10^{-2}}$$

$$= 0.1314 \text{ m}^3/\text{s}$$

$$(4) \quad \gamma = 17000 \text{ N/m}^3 = 0.17 \text{ t/m}^3, \quad S_{H_2O} = 1.026$$

$$\Delta H = \gamma \left( \frac{S_1 + S_2}{S_1 S_2} - 1 \right)$$

$$\Delta H = 0.17 \left( \frac{13.6}{1.026} - 1 \right)$$

$$\Delta R = 2.03 \text{ m}$$

$$V = \int 2\pi r h$$

$$V = \int 2\pi r \cdot 2.03$$

$$V = 6.323 \text{ m}^3$$

$$(5) \quad Q = 0.05 \text{ dm}^3/\text{min} = 833 \times 10^{-6} \text{ m}^3/\text{sec}$$

$$\text{Speed of Rotation} = 1700 \text{ rev/min} = 28.33 \text{ rev/s}$$

$$\text{Nominal Displacement} = 10 \text{ cm}^3/\text{rev} = 10^{-5} \text{ m}^3$$

$$\text{Torque } J_{\text{ref}} = 15 \text{ Nm}$$

$$\text{Pressure Change} = 15 \text{ bar} = 15 \times 10^5 \text{ N/m}^2$$

$$\text{Ideal flow rate} = \text{Nominal displacement} \times \text{speed of rotation}$$

$$= 10^{-5} \times 28.3$$

$$= 2.83 \times 10^{-4} \text{ m}^3/\text{s}$$

$$(A) \quad \text{Volumetric Efficiency} = \frac{\text{Actual flow rate} \times 100}{\text{Ideal flow rate}}$$

$$= \frac{833 \times 10^{-3}}{2.83 \times 10^{-4}} \times 100$$

$$= 29.45\%$$

$$(B) \quad \text{Fluid Power, } P_f = \Delta P \cdot Q$$

$$= 8.33 \times 10^{-3} \times 15 \times 10^5$$

$$= 124.95 \text{ watts}$$

$$(C) \quad \text{Shaft power} = T \times \omega$$

$$\omega = 2\pi \times \text{speed of rotation}$$

$$\omega = 2\pi \times 28.3$$

$$\omega = 177.81 \text{ rad/sec}$$

$$\therefore \text{Shaft power} = 15 \times 177.81$$

$$= 2667.2 \text{ watts}$$

$$(D) \quad \text{Overall Efficiency} = \frac{\text{Fluid Power} \times 100}{\text{Shaft power}}$$

$$= \frac{124.95}{2667.2} \times 100$$

$$= 4.68\%$$