

Laminar Flow  
Mechanical Engineering  
18/EN/06/038

$V_1 = 5 \text{ ms}^{-1}$  PHg smaller end = 2.5m  $l = 2.0 \text{ m}$   
 $V_2 = 2 \text{ ms}^{-1}$   $hL = \frac{(0.35(V_1 - V_2))^2}{2g}$

Pressure end =  $h$

$L = Z_1 - Z_2$

$\frac{P_1}{\rho} + \frac{V_1^2}{2g} + Z_1 = \frac{P_2}{\rho} + \frac{V_2^2}{2g} + Z_2 + h$

$\frac{P_2}{\rho} = \frac{P_1}{\rho} + \frac{1}{2g} (V_1^2 + V_2^2) + (Z_1 - Z_2) - h$   
 $= \frac{2.5 + 5^2 - 2^2}{2 \times 9.81} + \frac{2 - (0.35(5-2))^2}{2 \times 9.81}$   
 $= 2.5 + 1.0712 - 0.16055$

$P_2 = 5.407 \text{ m of liquid}$

Pressure

2. Inlet diameter = 20cm, Inlet diameter = 100cm

$P_1 = 17658 \text{ N/cm}^2$   $Cl = 0.71$

$J = 30 \text{ cm of Mercury} = 0.3 \text{ m of mercury}$

$A_1 = \frac{\pi d^2}{4} = \frac{(20/100)^2 \times 3.142}{4} = 0.0214 \text{ m}^2$

$A_2 = \frac{\pi d^2}{4} = \frac{(10/100)^2 \times 3.142}{4} = 7.855 \times 10^{-3} \text{ m}^2$

$P_1 = \frac{17658}{1000} = 17.658 \times 10^3 \text{ Pa}$

$\rho = \frac{17658 \times 10^3}{9.81 \times 10^{-1}} = 1.8 \times 10^3$

$P_2 = 0.2 \times 13.6 = +4.08 \text{ m of H}_2\text{O}$

$h = \frac{P_1}{\rho} - \frac{P_2}{\rho} = \frac{1.8 \times 10^7}{1.8 \times 10^3} - (-4.08) = 4.08018 \text{ m}$

$Q = \frac{0.98 \times 0.0214 \times 7.855 \times 10^{-3}}{\sqrt{(0.0214)^2 - (7.855 \times 10^{-3})^2}} \times \sqrt{2 \times 9.81 \times 4.08018}$

$Q = 0.0209 \text{ m}^3/\text{s}$

3.  $D_1 = 15 \text{ cm}$   $D_2 = 30 \text{ cm}$   $S.G. = 0.7$

$Q = 1$  ~~5~~ 0.5m of mercury  $Cu = 0.64$

$A_1 = \frac{\pi d^2}{4} = \frac{(15/100)^2 \times 3.14}{4} = 0.0177 \text{ m}^2$

$A_2 = \frac{\pi d^2}{4} = \frac{(30/100)^2 \times 3.14}{4} = 0.0707 \text{ m}^2$

$h = \frac{13.6}{0.7} (1) \quad h_1 = y \left( \frac{5h}{30} - 1 \right)$

$h = 0.5 \left( \frac{13.6}{0.7} - 2 \right) \quad 5h = 13.6 \quad y = 50 \times 10^{-2}$   
 $= 7.055 \text{ m} \quad 6.56 \text{ m} \quad h = 50 \times 10^{-2} \left( \frac{13.6}{0.7} - 1 \right)$   
 $= 7.055 \text{ m}$

$Q = \frac{Cd A_1 A_2 \sqrt{2g h}}{\sqrt{A_1^2 + A_2^2}}$

$Q = 0.64 \times 0.0177 \times (0.0707) \times \sqrt{2 \times 9.81 \times 7.055}$   
 $\frac{0.0177 \times 0.0707}{0.0177}$

$Q = 7.26 \times 0.137 \text{ m}^3/\text{s}$

4.  $A = 13 \text{ m}$

$y = 170 \text{ mm of Mercury} = 0.17 \text{ m Hg} \quad \rho = J$

S.G. of mercury = 13.6

S.G. of sea water = 1.026

$\Delta h = y \left( \frac{13.6}{1.026} - 1 \right)$

$\Delta h = 0.17 \left( \frac{13.6}{1.026} - 1 \right)$

$h = 2.083 \text{ m}$

$V = \sqrt{2g \Delta h}$

$V = \sqrt{2 \times 9.81 \times 2.083}$

$V = 6.39 \text{ m/s}$

$$\begin{aligned}
 5 \quad Q &= 0.05 \text{ dm}^3/\text{min} = 8.33 \times 10^{-5} \text{ m}^3/\text{s} \\
 \text{Speed of Rotation} &= 1700 \text{ Rev/min} = 28.3 \text{ Rev/sec} \\
 \text{Normal Displacement} &= 10 \text{ cm}^3/\text{rev} = 10^{-5} \text{ m}^3/\text{rev} \\
 \text{Torque Input} &= 15 \text{ Nm} \\
 \text{Pressure Change} &= 15 \text{ bar} = 15 \times 10^5 \text{ N/m}^2 \\
 \text{Ideal flow rate} &= 10^{-5} \times 28.3 \\
 &= 2.83 \times 10^{-4} \text{ m}^3/\text{sec}
 \end{aligned}$$

$$\begin{aligned}
 \text{a) Volumetric Efficiency} &= \frac{\text{Actual flow rate (m}^3/\text{s)}}{\text{Ideal flow rate}} \\
 &= \frac{8.33 \times 10^{-5}}{2.83 \times 10^{-4}} \times 100 \\
 &= 29.45\%
 \end{aligned}$$

$$\begin{aligned}
 \text{b Fluid Power } P_f &= Q \times \Delta P \\
 &= 8.33 \times 10^{-5} \times 15 \times 10^5 \\
 &= 124.95 \text{ watts}
 \end{aligned}$$

$$\begin{aligned}
 \text{c Shaft Power} &= \tau \times \omega \\
 \omega &= 2\pi \times \text{speed of rotation} \\
 \omega &= 2\pi \times 28.3 \\
 \omega &= 177.81 \text{ rad/sec} \\
 \therefore \text{Shaft power} &= 15 \times 177.81 \\
 &= 2667.2 \text{ watts}
 \end{aligned}$$

$$\begin{aligned}
 \text{d Overall efficiency} &= \frac{\text{Fluid Power (W)}}{\text{Shaft power}} \\
 &= \frac{124.95}{2667.2} \times 100 \\
 &= 4.68\%
 \end{aligned}$$