

AREMY JOSILLOBA ETIMANUEL

18/ENG03/015

CIVIL ENGINEERING

Fluid Mechanics ENGR-214

1) Given Sp of gravity 0.7,  $D_1 = 150\text{mm} = 0.15\text{m}$

$$D_2 = 75\text{mm} = 0.075\text{m}$$

$$Z_2 - Z_1 = 150\text{mm} = 0.15\text{m}, \quad Q = 40 \text{ lit/sec}$$

$$= 0.04 \text{ m}^3/\text{s}$$

$$C_d = 0.76$$

Pressure difference:

$$A_1 = \frac{\pi D_1^2}{4} = \frac{\pi \times 0.15^2}{4} = 0.01767 \text{ m}^2$$

$$A_2 = \frac{\pi D_2^2}{4} = \frac{\pi \times 0.075^2}{4} = 0.00442 \text{ m}^2$$

$$Q = C_d \times \frac{A_1 A_2 \times \sqrt{2gh}}{\sqrt{A_1^2 - A_2^2}}$$

$$0.04 = \frac{0.76 \times 0.01767 \times 0.00442 \times \sqrt{2 \times 9.81 \times h}}{\sqrt{0.01767^2 - 0.00442^2}}$$

$$0.04 = 0.76 \times 0.004565 \times 4.429 \sqrt{h}$$

$$h = \left( \frac{0.04}{0.76 \times 0.004565 \times 4.429} \right)^2 = 4.247 \text{ m}$$

A  
18  
c)

$$(4.247 + 0.15) \rho g = \rho_1 P_2$$

$$P_1 - P_2 = (0.8 \times 1000 \times 9.81) (4.247 + 0.15)$$

$$P_1 - P_2 = 34.51 \text{ kN/m}^2$$

1)

2 Diameter of Inlet  $D_1 = 300 \text{ mm} = 0.3 \text{ m}$

Ph

$$\text{Area of Inlet } A_1 = \frac{\bar{u} D_1^2}{4} = \frac{11 \times 0.3^2}{4} = 0.07 \text{ m}^2$$

P.

w

Diameter of throat  $D_2 = 150 \text{ mm} = 0.15 \text{ m}$

$$\text{Area of inlet } A_2 = \frac{\bar{u} D_2^2}{4} = \frac{11 \times 0.15^2}{4} = 0.01767 \text{ m}^2$$

Specific gravity of heavy liquid (mercury) in U tube manometer  $S_{hc} = 13.6$

Specific gravity of liquid (oil)  $S_p = 0.9$

Reading of differential manometer,  $y = 250 \text{ mm} = 0.25 \text{ m}$

The differential "h" is given by

2) Inlet

$$h = \left( \frac{P_1}{\rho} + Z_1 \right) - \left( \frac{P_2}{\rho} + Z_2 \right)$$

$$= y \left[ \frac{S_{hc}}{S_p} - 1 \right] = 0.25 \left( \frac{13.6}{0.9} - 1 \right) = 3.55 \text{ m of oil}$$

Discharge of oil  $Q$

Using the relation

$$Q = C_d \times A_1 A_2 \times \sqrt{2gh}$$

$$Q = \frac{0.98 \times 0.07 \times 0.01767 \times \sqrt{2 \times 9.81 \times 3.53}}{\sqrt{0.07^2 - 0.01767^2}}$$

$$Q = 0.1489 \text{ m}^3/\text{s}$$

$$h = \left( 0.0 + \frac{0.96 \times 0.004505 \times 4.429}{2} \right)^2 = 4.247 \text{ m}$$

$$h = \left( \frac{P_1}{\rho} + z_1 \right) - \left( \frac{P_2}{\rho} + z_2 \right)$$

$$h = \left( \frac{P_1}{\rho} - \frac{P_2}{\rho} \right) + (z_1 - z_2)$$

$$4.247 = \left( \frac{P_1 - P_2}{\rho g} \right) - 0.15$$

$$4.247 + 0.15 = P_1 - P_2 / \rho g$$



Diameter of throat  $D_2 = 150 \text{ mm} = 0.15 \text{ m}$

$$\text{Area of inlet } A_2 = \frac{\bar{u} D_2^2}{4} = \frac{\bar{u} \times 0.15^2}{4} = 0.01767 \text{ m}^2$$

Specific gravity of heavy liquid (mercury) in U tube manometer  $S_{hc} = 13.6$

Specific gravity of liquid (oil)  $S_p = 0.9$

Reading of differential manometer,  $y = 250 \text{ mm} = 0.25 \text{ m}$

2)

The differential "h" is given by

$$h = \left( \frac{P_1}{w} + Z_1 \right) - \left( \frac{P_2}{w} + Z_2 \right)$$

$$= y \left[ \frac{S_{hc}}{S_p} - 1 \right] = 0.25 \left( \frac{13.6}{0.9} - 1 \right) = 3.55 \text{ m of oil}$$

Discharge of oil  $Q$

Using the relation

$$Q = \frac{C_d \times A_1 A_2 \times \sqrt{2gh}}{\sqrt{A_1^2 - A_2^2}}$$

$$Q = \frac{0.98 \times 0.07 \times 0.01767 \times \sqrt{2 \times 9.81 \times 3.55}}{\sqrt{0.07^2 - 0.01767^2}}$$

$$Q = 0.1489 \text{ m}^3/\text{s}$$

b) Pressure different between entrance and throat section  $P_1 - P_2$

$$\text{then } h = \left( \frac{P_1}{w} + Z_1 \right) - \left( \frac{P_2}{w} + Z_2 \right) = 3.53$$

$$h = \left( \frac{P_1}{w} - \frac{P_2}{w} \right) - (Z_2 - Z_1) = 3.53$$

$$Z_2 - Z_1 = 300 \text{ mm} = 0.3 \text{ m}$$