

DABOT INDUSTRIAL CHEMICALS UNIT

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CHEMICAL ENGINEERING

ENIGALIA K FLUID MECHANICS

1) Given SP of gravity 0.8, $D_1 = 150 \text{ mm} = 0.15 \text{ m}$,
 $D_2 = 75 \text{ mm} = 0.075 \text{ m}$, $Z_2 - Z_1 = 150 \text{ mm} = 0.15 \text{ m}$
 $Q = 40 \text{ liter/sec} = 0.04 \text{ m}^3/\text{s}$, $C_d = 0.96$.

Pressure difference ($P_1 - P_2$)

$$P_1 - P_2 = \frac{4Q}{A_1} = \frac{4Q}{\frac{\pi}{4} \times 0.15^2} = 0.01467 \text{ m}^2$$

$$A_2 = \frac{4Q}{V} = \frac{4Q \times 0.96}{V} = 0.00442 \text{ m}^2$$

$$Q = \frac{C_d \times A_1 \times A_2 \times \sqrt{2\Delta P}}{\sqrt{A_1^2 + A_2^2}}$$

$$0.04 = \frac{0.96 \times 0.075 \times 0.01467 \times \sqrt{2 \times 9.81 \times \Delta P}}{\sqrt{0.01767^2 + 0.00442^2} \times \sqrt{2 \times 9.81 \times \Delta P}}$$

$$0.04 = 0.96 \times 0.076 \times 0.004565 \times 4.429 \sqrt{\Delta P}$$

$$\Delta P = \left(\frac{0.04}{0.96 \times 0.004565 \times 4.429} \right)^2 = 4.247 \text{ m}$$

$$h = \left(\frac{P_1}{\rho g} + Z_1 \right) - \left(\frac{P_2}{\rho g} + Z_2 \right)$$

$$h = \left(\frac{P_1}{\rho g} - \frac{P_2}{\rho g} \right) + (Z_1 - Z_2)$$

$$4.247 - \left(\frac{P_1 - P_2}{\rho g} \right) = 0.15$$

$$4.247 + 0.15 = \frac{P_1 - P_2}{\rho g}$$

$$(4.247 + 0.15) \rho g = P_1 - P_2$$

$$P_1 - P_2 = (0.8 \times 1000 \times 9.81) (4.247 + 0.15)$$

$$P_1 - P_2 = 34.51 \text{ kN/m}^2$$

2.) Diameter of Inlet $D_1 = 300 \text{ mm} = 0.3 \text{ m}$

$$\text{Area of Inlet } A_1 = \frac{\pi \times D_1^2}{4} = \frac{\pi \times 0.3^2}{4} = 0.0707 \text{ m}^2$$

Diameter of throat $D_2 = 150 \text{ mm} = 0.15 \text{ m}$

$$\text{Area of Inlet } A_2 = \frac{\pi \times D_2^2}{4} = \frac{\pi \times 0.15^2}{4} = 0.0177 \text{ m}^2$$

Specific gravity of heavy liquid (mercury) in U tube manometer, $S_m = 13.6$

Specific gravity of liquid (oil) flowing through pipe $S_p = 0.9$

Reading of differential manometer,

$$y = 250 \text{ mm} = 0.25 \text{ m}$$

The differential 'h' is given by

$$h = \left(\frac{P_1}{\rho} + z_1 \right) - \left(\frac{P_2}{\rho} + z_2 \right)$$

$$= y \left[\frac{S_m}{S_p} - 1 \right] = 0.25 \left[\frac{13.6}{0.9} - 1 \right] = 3.53 \text{ m}$$

c.) Discharge of oil Q

using the relation,

$$Q = \frac{C_d \times A_1 A_2 \times \sqrt{2gh}}{\sqrt{A_1^2 - A_2^2}}$$

$$Q = 0.98 \times 0.0707 \times 0.01767 \times \sqrt{2 \times 9.81 \times 3.53}$$
$$\sqrt{0.07^2 - 0.01767^2}$$

$$Q = 0.1489 \text{ m}^3/\text{s}$$

iv) Pressure difference between entrance and throat section $P_1 - P_2$

We know that

$$h = \left(\frac{P_1}{\rho} + z_1 \right) - \left(\frac{P_2}{\rho} + z_2 \right) = 3.53$$

$$h = \left(\frac{P_1}{\rho} - \frac{P_2}{\rho} \right) - (z_1 - z_2) = 3.53$$

$$Z_2 - Z_1 = 300 \text{ mm} = 0.3 \text{ m}$$

$$\left(\frac{P_1 - P_2}{w} \right) \cdot 0.3 = 3.53$$

$$\frac{P_1 - P_2}{w} = 3.53 \div 0.3$$

$$\frac{P_1 - P_2}{w} = 3.83$$

$$P_1 - P_2 = 3.83 w$$

$$P_1 - P_2 = 3.82 \times 9.81 \times 0.7$$
$$= 33.8 \text{ kN/m}^2$$