MATRIC NO: 19/ENG01/017

## DEPARTMENT: CHEMICAL ENGINEERING

## FLUID MECHANICS ASSIGNMENT

1. A pump delivers $10 \mathrm{dm}^{3} / \mathrm{min}$ with a pressure rise of $\mathbf{1 2} \mathbf{b a r}$. The speed of rotation is 1500 revolution / min and the nominal displacement is $10 \mathrm{~cm}^{3} / \mathrm{rev}$. The Torque input is 12.5 N . Calculate:
i. The volumetric efficiency.
ii. Fluid Power.
iii. The shaft power.
iv. The overall efficiency.

## SOLUTION

Idea flow rate $=$ Nominal Displacement $\times$ Speed $=10 \times 1500=15000 \mathrm{~cm}^{3} / \mathrm{min}=15 \mathrm{dm}^{3}$ /min.

Volumetric efficiency $=$ Actual Flow/Ideal Flow $=10 / 15=0.67$ or $67 \%$.
$\mathrm{Q}=\left(10 \times 10^{-3}\right) / 60 \mathrm{~m}^{3} / \mathrm{s}=16.7 \times 10^{-5} \mathrm{~m}^{3} / \mathrm{s}$
$\Delta \mathrm{p}=12 \times 10^{5} \mathrm{~N} / \mathrm{m}^{2}$
Fluid Power $=\mathrm{Q} \Delta \mathrm{p}=16.7 \times 10^{-5} \times 12 \times 10^{5}=200.04$ Watts
Shaft Power $=2 \pi \mathrm{NT} / 60=2 \pi \times 1500 \times 12.5 / 60=1963.5 \mathrm{Nm}$
Overall Efficiency $=$ F.P. $/$ S.P. $=200.4 / 1963.5=0.0102$ or $1.02 \%$
2. A pump Delivers $35 \mathbf{~ d m}^{3} / \mathbf{m i n}$ with a pressure change of $\mathbf{1 0 0}$ bar. If the overall efficiency is $87 \%$. Calculate the shaft power.

## SOLUTION

$\mathrm{Q}=\left(35 \times 10^{-3}\right) / 60 \mathrm{~m}^{3} / \mathrm{s}=58.33 \times 10^{-5} \mathrm{~m}^{3} / \mathrm{s}$
$\Delta \mathrm{P}=100 \times 10^{5} \mathrm{~N} / \mathrm{m}^{2}$
Fluid Power $=\mathrm{Q} \times \Delta \mathrm{P}=58.33 \times 10^{-5} \times 100 \times 10^{5}=5833$ Watts
Overall Efficiency = Fluid Power / Shaft Power
Shaft Power = Fluid Power / Overall Efficiency

$$
=5833 / 0.87=6704.6 \mathrm{Nm}
$$

3. A pump has a nominal displacement of $50 \mathrm{~cm}^{3} / \mathrm{rev}$ and a pressure rise of $\mathbf{1 0 0}$ bar. If the shaft power is 15 Kilowatts. Calculate the overall Efficiency and Volumetric Efficiency. Taking Actual Flow rate $=\mathbf{3 5} \mathbf{~ d m}^{3} / \mathbf{m i n}$ and speed of rotation $=\mathbf{8 5 0} \mathbf{r}$ p m.

## SOLUTION

Idea flow rate $=$ Nominal Displacement $\times$ Speed $=50 \times 850=42500 \mathrm{~cm}^{3} / \mathrm{min}=42.5 \mathrm{dm}^{3}$ /min.

Volumetric efficiency $=$ Actual Flow/Ideal Flow $=35 / 42.5=0.82$ or $82 \%$. $\mathrm{Q}=\left(35 \times 10^{-3}\right) / 60 \mathrm{~m}^{3} / \mathrm{s}=58.33 \times 10^{-5} \mathrm{~m}^{3} / \mathrm{s}$
$\Delta \mathrm{p}=100 \times 10^{5} \mathrm{~N} / \mathrm{m}^{2}$
Fluid Power $=\mathrm{Q} \Delta \mathrm{p}=58.33 \times 10^{-5} \times 100 \times 10^{5}=5833$ Watts
Shaft Power $=15 \mathrm{~kW}=15000 \mathrm{Nm}$
Overall Efficiency $=$ F.P. $/$ S.P. $=5833 / 15000=0.389$ or $38.9 \%$
4. Water is drawn from a reservoir in which the water level is $2,4000 \mathrm{~cm}$ above the datum at the rate of 13 liters/sec. The Outlet of the pipe is at datum level and is fitted a nozzle to produce a high speed jet in order to drive a turbine of pelton wheel type. If the velocity of jet is $\mathbf{6 6} \mathbf{~ m} / \mathrm{sec}$. Calculate
i. Power of Jet
ii. Power Supplied from reservoir
iii. Head used to overcome Losses.
iv. Efficiency of the pipeline and nozzle in transmitting operation.

## SOLUTION

5. Oil of specific gravity 0.89 is drawn from a reservoir in which the oil is $\mathbf{3 0 , 0 0 0} \mathbf{~ c m}$ above the datum at the rate 220 Litres $/ \mathrm{sec}$. If the velocity of jet is $7 \mathrm{~m} \mid s e c$. Calculate
i. Power of Jet
ii. Power supplied from reservoir
iii. Head used to overcome Losses
iv. Efficiency of the pipeline and nozzle in transmitting operation.

## SOLUTION

6. A fountain sends a stream of water 20 m up into the air. If the base of the stream is 10 cm in diameter, what power is required to send the water to this height?

## SOLUTION

Known data:
$\mathrm{h}=20 \mathrm{~m}, \mathrm{~d}=10 \mathrm{~cm}=0.10 \mathrm{~m}$
$\rightarrow \mathrm{A}=(\pi / 4) \mathrm{d}^{2}=0.7854(0.10 \mathrm{~m})^{2}=7.854 \times 10^{-3} \mathrm{~m}^{2}$
$V_{f}=0$

Unknowns:
'W=?

The speed of the water at the upper end of the stream is zero. Then, the initial speed of the water is defined by the following expression:
$\mathrm{V}^{2}{ }_{\mathrm{f}}=\mathrm{V}_{\mathrm{i}}{ }^{2}-2 \mathrm{gh}$
$V_{i}=\sqrt{ } V^{2}{ }_{f}+2 g h$
$\mathrm{V}_{\mathrm{i}}=\sqrt{ } 0^{2}+2(9.8 \mathrm{~m} / \mathrm{s} 2) *(20 \mathrm{~m})=19.80 \mathrm{~m} / \mathrm{s}$

The flow rate is equal to the speed through the area.
$\mathrm{Q}=\mathrm{v}^{*} \mathrm{~A}=(19.80 \mathrm{~m} / \mathrm{s})^{*}(7.854 \times 10-3 \mathrm{~m} 2)=0.1555 \mathrm{~m} 3 / \mathrm{s}$
The hydraulic power required to drive the water to a height h is defined by the following expression:
$\cdot \mathrm{W}=\rho \mathrm{gQh}=\left(1000 \mathrm{~kg} / \mathrm{m}^{3}\right)^{*}\left(9.8 \mathrm{~m} / \mathrm{s}^{2}\right)^{*}\left(0.1555 \mathrm{~m}^{3} / \mathrm{s}\right)^{*}(20 \mathrm{~m})=30478 \mathrm{kgm}^{2} / \mathrm{s}^{3}=30 \times 10^{3} \mathrm{~W}$
The power required is:
$\cdot \mathrm{W}=30 \times 10^{3} \mathrm{~W}$.
7. A Venturimeter with an entrance diameter of 0.3 m and a throat diameter of $\mathbf{0 . 2 m}$ is used to measure the volume of gas flowing through a pipe. The discharge coefficient of the meter is $\mathbf{0 . 9 6}$. Assuming the specific weight of the gas to be constant at $19.62 \mathrm{~N} / \mathrm{m}^{3}$, calculate the volume flowing when the pressure difference between the entrance and the throat is measured as 0.06 m on a water U -tube manometer.

## SOLUTION

$\rho_{\mathrm{g}} \mathrm{g}=19.62 \mathrm{~N} / \mathrm{m}^{3}$
$\mathrm{C}_{\mathrm{d}}=0.96$
$\mathrm{d}_{1}=0.3 \mathrm{~m}$
$\mathrm{d}_{2}=0.2 \mathrm{~m}$
Calculate; Q ,

$$
\mathrm{u}_{1}=\mathrm{Q} / 0.0707, \quad \mathrm{u}_{2}=\mathrm{Q} / 0.0314
$$

For the manometer;

$$
\begin{aligned}
& \mathrm{P}_{1}+\rho_{\mathrm{g}} \mathrm{gZ}=\mathrm{P}_{2}+\rho_{\mathrm{g}} \mathrm{~g}^{*}\left(\mathrm{z}_{2}-\mathrm{R}_{\mathrm{p}}\right)+\rho_{\mathrm{w}} \mathrm{~g} R_{\mathrm{p}} \\
& \mathrm{P}_{1}-\mathrm{P}_{2}=19.62^{*}\left(\mathrm{z}_{2}-\mathrm{z}_{1}\right)+587.423
\end{aligned}
$$

For the Venturimeter;

$$
\begin{array}{r}
\frac{P_{1}}{\rho_{g} g z}+\frac{u_{1}^{2}}{2 g}+z_{1}=\frac{p_{2}}{\rho_{g} g}+\frac{u_{2}^{2}}{2 g}+z_{2} \\
\mathrm{P}_{1}-\mathrm{P}_{2}=19.62^{*}\left(\mathrm{z}_{2}-\mathrm{z}_{1}\right)+0.803 \mathrm{u}_{2}^{2}
\end{array}
$$

Combining (1) and (2);

$$
\begin{aligned}
& 0.803 \mathrm{u}_{2}^{2}=587.423 \\
& \mathrm{u}_{\text {2ideal }}=27.047 \mathrm{~m} / \mathrm{s} \\
& \mathrm{Q}_{\text {ideal }}=27.047 \times \Pi^{*}\left(\frac{0.2}{2}\right)^{2}=0.85 \mathrm{~m}^{3} / \mathrm{s} \\
& \mathrm{Q}=\mathrm{C}_{\mathrm{d}} * \mathrm{Q}_{\text {ideal }}=0.96 \times 0.85=0.816 \mathrm{~m}^{3} / \mathrm{s}
\end{aligned}
$$

8. A Venturimeter of throat diameter 0.076 m is fitted in a 0.152 m diameter vertical pipe in which liquid of relative density 0.8 flows downwards. Pressure gauges are fitted to the inlet and to the throat sections. The throat being 0.914 m below the inlet. Taking the coefficient of the meter as 0.97 find the discharge a) when the pressure gauges read the same b) when the inlet gauge reads $15170 \mathrm{~N} / \mathrm{m}^{2}$ higher than the throat gauge.

## SOLUTION

$$
\begin{aligned}
& \mathrm{d}_{1}=0.152 \mathrm{~m}, \mathrm{~d}_{2}=0.076 \mathrm{~m}, \mathrm{~A}_{1}=0.01814 \mathrm{~m}, \mathrm{~A}_{2}=0.00454 \mathrm{~m}, \rho=800 \mathrm{~kg} / \mathrm{m}^{3} \\
& \mathrm{C}
\end{aligned}
$$

$$
d=0.97
$$

Apply Bernoulli;

$$
\frac{P_{1}}{\rho_{g} g Z}+\frac{u_{1}^{2}}{2 g}+z_{1}=\frac{p_{2}}{\rho_{g} g}+\frac{u_{2}^{2}}{2 g}+z_{2}
$$

a. $P_{1}=P_{2}$

$$
\frac{u_{1}^{2}}{2 g}+z_{1}=\frac{u_{2}^{2}}{2 g}+z_{2}
$$

By continuity;

$$
\begin{gathered}
\mathrm{Q}=\mathrm{u}_{1} \mathrm{~A}_{1}=\mathrm{u}_{2} \mathrm{~A}_{2} \\
\mathrm{u}_{2}=\mathrm{u}_{1} \frac{A_{1}}{A_{2}}=\mathrm{u}_{1} 4 \\
\frac{u_{1}^{2}}{2 g}+0.914=\frac{16 u_{1}^{2}}{2 g} \\
\mathrm{u}_{1}=\sqrt{ } \frac{0.914 \times 2 \times 9.81}{15}=1.0934 \mathrm{~m} / \mathrm{s} \\
\mathrm{Q}=\mathrm{C}_{\mathrm{d}} \mathrm{~A}_{1} \mathrm{u}_{1} \\
\mathrm{Q}=0.96 \times 0.01814 \times 1.0934=0.019 \mathrm{~m}^{3} / \mathrm{s}
\end{gathered}
$$

b.

$$
\begin{aligned}
& \quad \mathrm{P}_{1}-\mathrm{P}_{2}=15170 \\
& \frac{P_{1}-P_{2}}{\rho g}=\frac{u_{2}^{2}-u_{1}^{2}}{2 g}-0.914 \\
& \quad \frac{P_{1}-P_{2}}{\rho g}=\frac{Q^{2}\left(220.43^{2}-55.11^{2}\right)}{2 g}-0.914 \\
& 55.8577=\mathrm{Q}^{2} *\left(220.43^{2}-55.11^{2}\right) \\
& \mathrm{Q}=0.035 \mathrm{~m}^{3} / \mathrm{s} .
\end{aligned}
$$

9. The water is flowing through a tapering pipe having diameter 300 mm and 150 mm at section $1 \& 2$ respectively. The discharge through the pipe is 40lit/sec. the section 1 is 10 m above datum and section 2 is $\mathbf{6 m}$ above datum. Find the intensity of pressure at section 2 , if that at section 1 is $400 \mathrm{kN} / \mathrm{m}^{2}$.

## SOLUTION

At section 1;
$\mathrm{D}_{1}=300 \mathrm{~mm}=0.3 \mathrm{~m}$, Area $\mathrm{a}_{1}=\pi / 4 * 0.32=0.0707 \mathrm{~m}^{2}$, Pressure $\mathrm{p}_{1}=400 \mathrm{kN} / \mathrm{m}^{2}$, Height of upper end above the datum, $\mathrm{z}_{1}=10 \mathrm{~m}$

At section 2;
$\mathrm{D}_{2}=150 \mathrm{~mm}=0.15 \mathrm{~m}$, Area $\mathrm{A}_{2}=(\pi / 4) * 0.152=0.01767 \mathrm{~m}^{2}$,

Height of lower end above the datum, $z_{2}=6 \mathrm{~m}$
Rate of flow (that is discharge) $\mathrm{Q}=40 \mathrm{lit} / \mathrm{sec}=40 / 1000\left(1\right.$ litre $\left.=1 \mathrm{~m}^{3} / \mathrm{sec}\right)=0.04 \mathrm{~m}^{3} / \mathrm{sec}$ Intensity of pressure at section 2, $\mathrm{p}_{2}$

As the flow is continuous,

$$
\mathrm{Q}=\mathrm{A}_{1} \mathrm{~V}_{1}=\mathrm{A}_{2} \mathrm{~V}_{2} \text { (Continuity equation) }
$$

Therefore, $\mathrm{V}_{1}=\mathrm{Q} / \mathrm{A}_{1}=0.04 / 0.0707=0.566 \mathrm{~m} / \mathrm{sec}$ and $\mathrm{V}_{2}=\mathrm{Q} / \mathrm{A}_{2}=0.04 / 0.01767=2.264 \mathrm{~m} / \mathrm{sec}$ Apply Bernoulli's equation at sections $1 \& 2$, We get, $\mathrm{p}_{1} / \mathrm{w}+\mathrm{v}_{1}{ }^{2} / 2 \mathrm{~g}+\mathrm{Z}_{1}=\mathrm{p}_{2} / \mathrm{w}+\mathrm{v}_{2}{ }^{2} / 2 \mathrm{~g}+\mathrm{z}_{2}$
and $\mathrm{p}_{2} / \mathrm{w}=\mathrm{p}_{1} / \mathrm{w}+\left(\mathrm{v}_{1}{ }^{2}-\mathrm{v}_{2}{ }^{2} / 2 \mathrm{~g}\right)+\mathrm{z}_{1}-\mathrm{Z}_{2}=(400 / 9.81)+1 /(2 * 9.81) *(0.5662-2.2642)+(10-6)$
$=40.77-0.245+4\left(\right.$ as $\left.\mathrm{w}=\rho * \mathrm{~g}=1000 \times 9.81 \mathrm{~N} / \mathrm{m}^{3}\right)=44.525 \mathrm{~m}=9.81 \mathrm{kN} / \mathrm{m}^{3}$
$\mathrm{P}_{2}=44.525 * \mathrm{w}=44.525 * 9.81=436.8 \mathrm{kN} / \mathrm{m}^{2}$
10. A submarine moves horizontally in sea and has its axis 15 m below the surface of water. A pitot tube properly placed just in front of the submarine and along its axis is connected to the $\mathbf{2}$ limbs of $U$-tube containing mercury. The difference in mercury level is found to be 170 mm . Find the speed of the submarine knowing that the specific gravity of mercury is $\mathbf{1 3 . 6}$ and that of sea water is $\mathbf{1 . 0 2 6}$ with respect of fresh water.

## SOLUTION

$$
\begin{gathered}
\mathrm{V}=c \sqrt{2} g r\left(\frac{\text { spgr }_{m}}{s}-1\right) \\
\mathrm{X}=\frac{170}{1000}=0.17 \mathrm{~m} \\
\operatorname{spgr}_{m}=13.6 \\
\mathrm{Spgr}_{\mathrm{s}}=1.026 \\
\mathrm{C}=1 \\
\mathrm{~V}=1 * \sqrt{2} \times 9.81 \times 6.17 \times\left(\frac{13.6}{1.026}-1\right)
\end{gathered}
$$

$$
\mathrm{V}=6.4 \mathrm{~m} / \mathrm{s}
$$

