

$$H = 7.055 \text{ m}$$

$$Q = C_d A_0 A_1 \sqrt{2gh} = 0.64 \times 0.0176 \times 0.002 \times \sqrt{2 \times 9.81 \times 7.055}$$

$$Q = 0.137 \text{ m}^3/\text{s}$$

$$4) y = 170 \text{ mmHg} = 170 \times 10^{-3} \text{ mHg}$$

$$\text{Sp of mercury} = 13.6 \text{ g}$$

$$\text{Sp of sea water} = 1.021$$

$$V = \frac{\rho_1 g h}{\rho_2}$$

$$V = 6.29 \text{ m/s}$$

$$H = 120 \times 10^{-3} \times \left( \frac{13.6 - 1}{1.021} \right)$$

$$H = 2.08 \text{ m}$$

$$5) \text{ actual flow rate } Q = 5 \text{ dm}^3/\text{min} = 8.33 \times 10^{-5} \text{ m}^3/\text{sec}$$

$$P = 5 \text{ bar} = 5 \times 10^5 \text{ N/m}^2$$

$$V = 1700 \text{ rev/min} = 28.33 \text{ r/sec}$$

$$T = 15 \text{ N/m} \quad \text{Normal displacement} = 100 \text{ cm}^3/\text{r}$$

$$= 1 \times 10^{-5} \text{ m}^3/\text{rev}$$

Volumetric efficiency

$$\frac{\text{Actual flow rate}}{\text{Ideal flow rate}} \times 100\%$$

Ideal flow rate

$$\text{Ideal flow rate} = \text{displacement} \times \text{speed}$$

$$Q = 1 \times 10^{-5} \times 28.33$$

$$= 2.833 \times 10^{-4} \text{ m}^3/\text{sec}$$

$$\frac{P_2}{w} = 0.5 \times 18.6 = 9.3 \text{ mtg}$$

$$\frac{P_2}{w} = 4.64 \text{ (since vacuum pressure)}$$

$$2/w = \frac{17.058 \times 10^3}{4.81 \times 10^3} = 3.54$$

$$h = \frac{P_2}{w} = \frac{P_2}{w} = 18.6 - 14.02 = 4.58$$

$$Q = C_d A_1 A_2 \sqrt{\frac{2gh}{A_1^2 - A_2^2}}$$

$$Q = 0.78 \times 0.03 \times (7.85 \times 10^{-3}) \times \sqrt{2 \times 9.81 \times 4.58}$$

$$Q = 0.03 \times 7.85 \times 10^{-3} \times \sqrt{89.4}$$

$$Q = 0.166 \text{ m}^3/\text{s}$$

$$C_d = 0.64$$

$$Q = 7$$

$$S_m = 13.6$$

$$S_0 = 0.9$$

$$d_1 = 30 \times 10^{-2} \text{ m}$$

$$y = 50 \times 10^{-2} \text{ mtg}$$

$$S_y \text{ of } 0.77 = 0.9$$

$$H = y \left[ \frac{S_m}{S_0} - 1 \right]$$

$$3 \quad d_1 = 15 \times 10^{-3} \text{ m}$$

$$A_1 = \frac{\pi \times (15 \times 10^{-3})^2}{4}$$

$$= 0.01767 \text{ m}^2$$

$$A_1 = \frac{\pi \times (30 \times 10^{-2})^2}{4}$$

$$= 0.0707 \text{ m}^2$$

$$H = 50 \times 10^{-2} \left[ \frac{13.6 - 1}{0.9} \right]$$

$$\text{Volumetric efficiency} = \frac{8.33 \times 10^{-4}}{2.833 \times 10^{-4}} \times 100$$

$$= 29.4\%$$

Fluid power (or xHP)

$$= 8.33 \times 10^{-5} \times 15 \times 10^5 = 124.95 \text{ W}$$

Shaft power = TXW

$$W = 2 \times \bar{v} \times V = 2 \times 2 \times 8 \times 8 \times 10^3 = 178 \text{ rad/s}$$

> TXW

$$= 15 \times 178 = 2670 \text{ W}$$

Overall efficiency

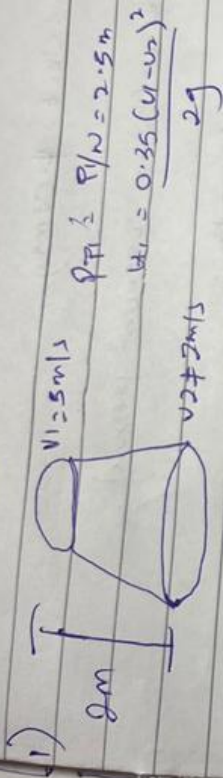
Fluid power  $\times 100\%$

Shaft power

$$= \frac{124.95}{2670} \times 100$$

$$= 4.68\%$$

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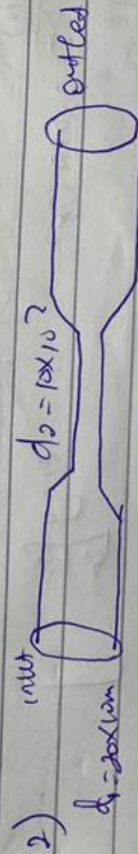
Using Bernoulli's equation  $P_1/N + \rho \left[ \frac{v_1^2}{2g} + z_1 \right] = P_2/N + \rho \left[ \frac{v_2^2}{2g} + z_2 \right] + \rho z$

$$P_2/N = P_1/N + \left[ \frac{\rho v_1^2}{2g} + \rho z_1 \right] - \left[ \frac{\rho v_2^2}{2g} + \rho z_2 \right] - \rho z$$

$$P_2/N = 2.5 + \left[ \frac{5^2}{2 \times 9.81} + 2 \right] - \left[ \frac{2^2}{2 \times 9.81} + 2 \right] - 0.167$$

$$P_2/N = 5.409 \text{ m}$$

$\therefore$  The pressure head at the lower end =  $5.409 \text{ m}$



$$P_1 = 17.658 \text{ m} / \text{m}^2 = 17.658 \times 10^4 \text{ N/m}^2 \quad C_d = 0.75$$

$$P_2 = 30 \text{ cm Hg} = 30 \times 10^{-2} \text{ m Hg} \quad \gamma = ?$$

$$\bar{P} = \frac{P_1 - P_2}{\gamma} = \frac{17.658 \times 10^4 - 30 \times 10^4}{10 \times 10^4} = 7.85 \times 10^{-3} \text{ m}^2$$

$$= 0.03 \text{ m}^2$$