

(1)

$$\text{Head loss, } h = \frac{0.35 (v_1 - v_2)^2}{2g}$$

$$\text{where } v_1 = 5 \text{ m/s, } v_2 = 2 \text{ m/s, } g = 9.8 \text{ m/s}^2$$

$$\therefore h = \frac{0.35 (5 - 2)^2}{2 \times 9.8}$$

$$h = 0.161 \text{ m}$$

But difference in pressure head in section 1 and 2 is

$$h = \frac{P_1 - P_2}{\omega}$$

Where

$$\omega = \rho \text{ of water} \times g$$

$P_1 =$  Pressure head

at section (1) = 2.5 m

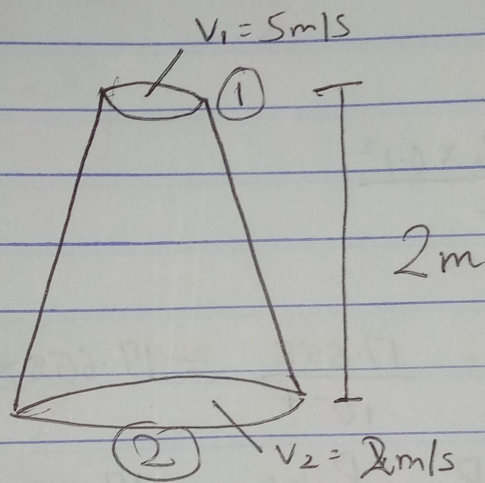
$P_2 =$  Pressure head at section (2) = ?

$$h = 0.161 \text{ m}$$

$$\therefore 0.161 = \frac{2.5 - P_2}{1000 \times 9.8}$$

$$- P_2 = \frac{1000 \times 9.8 \times 0.161 - 2.5}{1000 \times 9.8}$$

$$P_2 = -1.5753 \text{ m}$$



(2)

$$Q_{\text{actual}} = C_d \cdot A_1 A_2 \sqrt{2gh}$$

$$A_1^2 = A_2^2$$

$$d_1 = 20 \text{ cm} = \frac{20}{100} = 0.2 \text{ m}$$

$$A_1 = \frac{\pi d_1^2}{4} = \frac{3.142 \times 0.2^2}{4}$$

$$A_1 = 0.03142 \text{ m}^2$$

$$d_2 = 10 \text{ cm} = 0.1 \text{ m}$$

$$A_2 = \frac{\pi d_2^2}{4} = \frac{3.142 \times 0.1^2}{4}$$

$$A_2 = 0.00786 \text{ m}^2$$

$$P_{\text{inlet}} 17.658 \text{ N/cm}^2 = \frac{17.658}{10^{-4}} = 17.658 \times 10^4$$

~~$$P_1 = P_{\text{inlet}} = \frac{17.658 \times 10^4}{10^3 \times 9.81}$$~~

$$\frac{P_1}{\omega} = \frac{P_{\text{inlet}}}{\rho g} = \frac{17.658 \times 10^4}{10^3 \times 9.81}$$

$$\frac{P_1}{\omega} = 18$$

Specific gravity of mercury = 13.6

$$P_2 = P_{\text{vacuum pressure}}$$

~~$$P_2 = -4.08 \text{ m}$$~~

$$\text{Vacuum pressure } 30 \text{ cm Hg} = -0.3 \times 13.6$$

$$\frac{P_2}{\omega} = -4.08 \text{ m}$$

$$\text{Recall, } h = \frac{P_1 - P_2}{\omega} = \frac{P_1}{\omega} - \frac{P_2}{\omega}$$

~~$$h = 18 - (-4.08)$$~~

$$h = 18 + 4.08$$

$$h = 22.08$$

$$\therefore Q_{\text{actual}} = 0.98 \times 0.03142 \times 0.00786 \sqrt{2 \times 9.81 \times 22.08}$$

$$\sqrt{(0.03142)^2 - (0.00786)^2}$$

$$= 5.037 \times 10^{-3}$$

$$0.0304$$

$$Q_{\text{actual}} = 0.166 \text{ m}^3/\text{sec}$$

(5)

$$(i) \text{ Volumetric efficiency} = \frac{\text{Actual flow rate}}{\text{Theoretical flow rate}} \times 100$$

$$\begin{aligned} \text{Actual flow rate} &= Q = 5 \text{ dm}^3/\text{min} \\ 5 \text{ dm}^3/\text{min} &= 8.33 \times 10^{-5} \text{ m}^3/\text{s} \\ &= 8.33 \times 10^{-5} \text{ m}^3/\text{s} \end{aligned}$$

$$\begin{aligned} \text{Theoretical flow rate} &= \text{Displacement} / \text{rev} \times \text{driven speed} \\ \text{Driven speed} &= 1700 \text{ rev/min} = \frac{1700}{60} \text{ rev/sec} \\ &= 28.33 \text{ rev/sec} \end{aligned}$$

$$\text{Displacement / rev} = 10 \text{ cm}^3/\text{rev} = 1 \times 10^{-5} \text{ m}^3/\text{rev}$$

$$\begin{aligned} \therefore \text{Theoretical flow} &= 1 \times 10^{-5} \text{ m}^3/\text{rev} \times 28.33 \text{ rev/sec} \\ &= 2.833 \times 10^{-4} \text{ m}^3/\text{sec} \end{aligned}$$

$$\therefore \text{Volumetric efficiency} = \frac{8.33 \times 10^{-5}}{2.833 \times 10^{-4}} \times 100$$

$$= 29.4\%$$

(ii) Fluid power = Torque  $\times$  Speed

$$= 15 \times 28.33 = 0.529 \text{ Nm rev/sec}$$

$$\text{Shaft power} = \frac{\text{Fluid power}}{\text{Volumetric efficiency}}$$

$$= \frac{0.529}{29.4} = 0.018$$

$$\text{Overall efficiency} = \text{Volumetric eff} \times \text{Mechanical eff}$$

$$\text{Mechanical eff} = \frac{\text{Theoretical Torque} \times 100}{\text{Actual Torque}}$$

$$\text{Theoretical torque} = \text{Pressure} \times \text{displacement}$$

(5)

$$\text{Pressure} = 15 \text{ bar} = 1.5 \times 10^6 \text{ Nm}^{-2}$$

$$\text{displacement} = 1 \times 10^{-5} \text{ m}^3/\text{rev}$$

$$\begin{aligned} \text{Theoretical Torque} &= 1.5 \times 10^6 \times 1 \times 10^{-5} \\ &= 1.5 \times 10^1 \end{aligned}$$

$$= 15 \text{ Nm}$$

$$\therefore \text{Mechanical efficiency} = \frac{15}{15} \times 100$$

$$= 1 \times 100 = 100\%$$

$$\begin{aligned} \text{Overall efficiency} &= 29.4 \times 100 \\ &= 2.9 \times 10^{-3}\% \end{aligned}$$

(3)

$$d_0 = 15 \text{ cm} = 0.15 \text{ m}$$

$$A_0 = \frac{\pi d_0^2}{4} = \frac{3.142 \times 0.15^2}{4} = 0.0177 \text{ m}^2$$

$$d_1 = 30 \text{ cm} = 0.3 \text{ m}$$

$$A_1 = \frac{\pi d_1^2}{4} = \frac{3.142 \times 0.3^2}{4} = 0.0707 \text{ m}^2$$

$$y = 50 \text{ cm Hg} = 0.5 \text{ m Hg}$$

$$h = y \left( \frac{\text{S.g of mercury} - 1}{\text{Sg of oil}} \right)$$

$$h = 0.5 \left( \frac{13.6 - 1}{0.9} \right)$$

$$h = 7.06$$

$$Q = \frac{C_d \cdot A_0 \cdot A_1 \cdot \sqrt{2gh}}{\sqrt{A_1^2 - A_0^2}}$$

where  $C_d = 0.64$

$$Q = \frac{0.64 \times 0.0177 \times 0.0707 \sqrt{2 \times 9.81 \times 7.06}}{\sqrt{0.0707^2 - 0.0177^2}}$$

$$Q = \frac{0.0784}{0.068}$$

$$Q = 1.153 \text{ m}^3/\text{sec}$$

(4)

Reading of manometer  $y = 170 \text{ mm} = 0.17 \text{ m}$

$$S_{h_1} = \text{Sp}_g \text{ mercury} = 13.6$$

$$S_{h_2} = \text{Sp}_g \text{ sea water} = 1.026$$

$$h = y \left[ \frac{S_{h_1}}{S_{h_2}} - 1 \right]$$

$$h = 0.17 \left[ \frac{13.6}{1.026} - 1 \right]$$

$$h = 2.08 \text{ m}$$

$\therefore$  Speed of submarine  $V = \sqrt{2gh}$

$$V = \sqrt{2 \times 9.81 \times 2.08}$$

$$V = 12.07 \text{ m/s}$$