

LAW-ADUE EMMANUEL

19/ENGUS/069

MECHATRONICS < 200 Lvl >

ENG 214 ASSIGN

Q1 $V_1 = 5 \text{ ms}^{-1}$, $V_2 = 2 \text{ ms}^{-1}$

$P_{T1} = 2.5 \text{ m}$, $P_{T2} = ?$

$$P_{T1} - P_{T2} = \frac{0.35 (V_1 - V_2)^2}{2g}$$

$$2.5 - P_{T2} = \frac{0.35 \times 3^2}{2 \times 9.81} = 0.161$$

Since $P_{T1} - P_{T2} = 0.161$;

$$2.5 - P_{T2} = 0.161$$

$$P_{T2} = 2.5 + 0.161$$

$$P_{T2} = 2.67 \text{ m}$$

\therefore Pressure head at lower end = 2.67m ///

Q2 Inlet diameter, $d_1 = 20\text{cm} = 0.2\text{m}$

Throat diameter, $d_2 = 10\text{cm} = 0.1\text{m}$

$$P_1 = 17.658 \text{ N/cm}^2 \\ = 176,580 \text{ N/m}^2$$

$$P_2 = 30 \text{ cm Hg} = 0.3 \text{ m Hg}$$

$$C_d = 0.98$$

* * * * *

$$\text{Specific gravity of mercury} = 13.6$$

$$h = \frac{P_1}{\omega} - \frac{P_2}{\omega}$$

$$\Rightarrow \frac{P_1}{\omega} = \frac{176580}{1000 \times 9.81} = 18$$

$$\Rightarrow \text{Vacuum pressure} = 0.3 \times 13.6 \\ = 4.08$$

$$\therefore h = 18$$

$$= 18 - 4.08 = 13.92$$

$$\text{Area, } A_1 = \frac{\pi d_1^2}{4} = \frac{3.142 \times 0.2^2}{4} = 0.03142 \text{ m}^2$$

$$\text{Area, } A_2 = \frac{\pi d_2^2}{4} = \frac{3.142 \times 0.1^2}{4} = 0.007855 \text{ m}^2$$

Discharge of water, $Q_{act} = \frac{C_d A_1 A_2 \sqrt{2gh}}{\sqrt{A_1^2 - A_2^2}}$ 20

$$\therefore Q_{act} = \frac{0.98 \times 0.0314 \times 0.00786 \times \sqrt{2 \times 9.81 \times 13.92}}{\sqrt{0.0314^2 - 0.00786^2}}$$

$$Q_{act} = 0.131 \text{ //}$$

Q3 Orifice diameter, $d_2 = 15 \text{ cm} = 0.15 \text{ m}$

Pipe diameter, $d_1 = 30 \text{ cm} = 0.30 \text{ m}$

$$A_1 = \frac{\pi d_2^2}{4} = \frac{3.142 \times 0.15^2}{4} = 0.0177 \text{ m}^2$$

$$A_2 = \frac{\pi d_1^2}{4} = \frac{3.142 \times 0.30^2}{4} = 0.0707 \text{ m}^2$$

$$y = 50 \text{ cm Hg} = 0.5 \text{ m Hg}$$

$$C_d = 0.64$$

$$h = \frac{\text{SG of Hg} - \text{SG of oil}}{\text{SG of oil}} \times y$$

$$= \frac{13.6 - 0.9}{0.9} \times 0.5$$

$$= 7.06 \text{ m}$$

$$\text{Rate of flow, } Q_{act} = \frac{C_d A_2 A_1 \sqrt{2gh}}{\sqrt{A_1^2 - A_2^2}}$$

$$Q_{act} = \frac{0.64 \times 0.0177 \times 0.0707 \times \sqrt{2 \times 9.81 \times 7.06}}{\sqrt{0.0177^2 + 0.0707^2}}$$

$$Q_{act} = 0.138 \text{ m}^3/\text{s}$$

Q4 Velocity of the submarine, $V = \sqrt{2gH}$ 20

$$H = y \left(\frac{\text{SG of mercury} - \text{SG of water}}{\text{SG of water}} \right)$$

$$H = 0.17 \left(\frac{13.6 - 1.026}{1.026} \right)$$

$$= 0.17 \times 12.26$$

$$= 2.0842 \text{ m}$$

$$V = \sqrt{2 \times 9.81 \times 2.0842}$$

$$= 6.39 \text{ ms}^{-1}$$

\therefore the speed of the sub-marine = 6.39 ms^{-1} ///

$$9 - \frac{1}{10} + 0.914 = 0$$

Q5 Actual flow rate = $0.05 \text{ m}^3/\text{min}$;

$$Q = 0.05 \text{ m}^3 / 60 \text{ sec}$$

$$= 8.33 \times 10^{-4} \text{ m}^3/\text{sec}$$

$$\text{Speed} = 1700 \text{ rev/min}$$

$$= 1700 \text{ rev} / 60 \text{ sec}$$

$$= 28.33 \text{ rev/sec}$$

$$\text{Normal displacement} = 10 \text{ cm}^3/\text{rev}$$

$$= 1 \times 10^{-5} \text{ m}^3/\text{rev}$$

$$\text{Pressure} = 15 \text{ bar (P)}$$

$$= 15 \times 10^5 \text{ N/m}^2$$

$$\text{Ideal flow rate} = 28.33 \times 1 \times 10^{-5}$$

$$=$$

* Volumetric efficiency = $\frac{\text{Actual flow rate}}{\text{Ideal flow rate}} \times 100$

$$= \frac{8.33 \times 10^{-4}}{2.833 \times 10^{-4}}$$

$$= 2.940 \%$$

$$\begin{aligned}
 * \text{ Fluid power} &= Q \times P \\
 &= 8.33 \times 10^{-4} \times 15 \times 10^5 \\
 &= 1249.5 \text{ Nm/s or Watts}
 \end{aligned}$$

$$* \text{ Shaft power} = T \cdot \omega$$

$\langle \text{Torque input} \times \text{angular speed} \rangle$

$$T = 15 \text{ Nm}$$

$$\begin{aligned}
 \omega &= 2\pi \times \text{speed} \\
 &= 2 \times \frac{22}{7} \times 28.33 = 178.026
 \end{aligned}$$

$$= (15 \times 178.026) \text{ Watts}$$

$$= 2670.39 \text{ Watts}$$

$$\begin{aligned}
 * \text{ Overall Efficiency} &= \frac{\text{fluid power}}{\text{shaft power}} \times 100 \\
 &= \frac{1249.5}{2670.39} \times 100 \\
 &= 46.79 \%
 \end{aligned}$$