

LAW - ADUE EMMANUEL

19/ENG105/069

MECHATRONICS <200LVL>

QUESTION ONE (1)

$$\begin{aligned}\text{Actual flow rate} &= 10 \text{ dm}^3/\text{min} \quad \text{--- } Q \\ &= 0.01 \text{ m}^3/\text{min} = 1.67 \times 10^{-4} \text{ m}^3/\text{sec}\end{aligned}$$

$$\begin{aligned}\text{Speed} &= 1500 \text{ rev}/\text{min} \\ &= \frac{1500 \text{ rev}/\text{sec}}{60} = 25 \text{ rps}\end{aligned}$$

$$\begin{aligned}\text{Pressure} &= 12 \text{ bar} \quad \text{--- } P \\ &= 12 \times 10^5 \text{ N}/\text{m}^2\end{aligned}$$

$$\begin{aligned}\text{Normal displacement} &= 10 \text{ cm}^3/\text{rev} = \frac{10}{1000} \text{ m}^3/\text{rev} \\ &= 1 \times 10^{-5} \text{ m}^3/\text{rev}\end{aligned}$$

$$\begin{aligned}\text{Ideal flow rate} &= \text{normal displacement} \times \text{speed} \\ &= 1 \times 10^{-5} \times 25 \\ &= 2.5 \times 10^{-4} \text{ m}^3/\text{sec}\end{aligned}$$

$$\begin{aligned}\text{** Volumetric Efficiency} &= \frac{\text{Actual flow rate}}{\text{Ideal flow rate}} \times 100\% \\ &= \frac{1.67 \times 10^{-4}}{2.50 \times 10^{-4}} \times 100 \\ &= 66.8\%\end{aligned}$$

$$\begin{aligned}\text{** } P_f, \text{ Fluid power} &= Q \times P \\ &= 1.67 \times 10^{-4} \times 12 \times 10^5 \\ &= 200.4 \text{ Nm}/\text{sec}\end{aligned}$$

$$** \text{ Shaft power} = T \cdot \omega$$

$$= 12.5 \times \left(2 \times \frac{22}{7} \times \text{speed} \right)$$

$$= 12.5 \times 2 \times \frac{22}{7} \times 25$$

$$= 1964.25 \text{ Watts} //$$

** Overall Efficiency ;

$$= \frac{\text{fluid power}}{\text{shaft power}} \times 100$$

$$= \frac{200.4}{1964.25} \times 100 = 10.20 \% //$$

QUESTION TWO (2)

$$\begin{aligned}\text{Pressure change} &= 10 \text{ bar} \\ &= 10 \times 10^5 \text{ Nm}^{-2}\end{aligned}$$

$$\begin{aligned}\text{Actual flow rate } \dot{Q} &= 35 \text{ dm}^3/\text{min} \\ &= 5.83 \times 10^{-4} \text{ m}^3/\text{sec}\end{aligned}$$

$$\begin{aligned}\text{Fluid power} &= \dot{Q} \times P \\ &= 5.83 \times 10^{-4} \times 10 \times 10^5 \\ &= 5830 \text{ Watts}\end{aligned}$$

$$\begin{aligned}\text{Shaft power} &= \frac{\text{Fluid power} \times 100}{\text{Overall Efficiency}} \\ &= \frac{5830 \times 100}{87} = 6.701 \times 10^3 \text{ Watts} \quad \text{//}\end{aligned}$$

QUESTION THREE (3)

$$\begin{aligned}\text{Nominal displacement} &= 50 \text{ cm}^3/\text{rev} \\ &= \frac{50}{1000} \text{ m}^3/\text{rev} = 5 \times 10^{-5} \text{ m}^3/\text{rev}\end{aligned}$$

$$\begin{aligned}\text{Actual flow rate} &= 35 \text{ dm}^3/\text{min} \\ &= \frac{35}{100 \times 60} \text{ m}^3/\text{sec} = 5.83 \times 10^{-4} \text{ m}^3/\text{sec}\end{aligned}$$

$$\begin{aligned}\text{Fluid power} &= \dot{Q} \times P \\ &= 5.83 \times 10^{-4} \times 10 \text{ bar} \\ &= 5.83 \times 10^{-4} \times 10 \times 10^5 = 5830 \text{ Watts}\end{aligned}$$

$$\begin{aligned}** \text{ Overall Efficiency} &= \frac{5830}{15000} \times 100 \% \\ &= 38.87 \%\end{aligned}$$

$$\begin{aligned}
 \text{Ideal flow rate} &= \text{mmal displacement} \times \text{speed} \\
 &= 850 \text{ rpm} \times 5 \times 10^{-5} \\
 &= 5 \times 10^{-5} \times \frac{850}{60} \\
 &= \del{4} 7.085 \times 10^{-4} //
 \end{aligned}$$

* * Volumetric Efficiency : $\frac{\text{Act flow rate}}{\text{Ideal flow rate}} \times 100\%$

$$\begin{aligned}
 &= \frac{5.83 \times 10^{-4}}{7.085 \times 10^{-4}} \times 100\% \\
 &= 82.29\% //
 \end{aligned}$$

QUESTION FOUR

$$\begin{aligned}
 Z &= 24000 \text{ cm} \\
 Z &= 240 \text{ m} \quad \swarrow
 \end{aligned}$$

$$\begin{aligned}
 \text{Volumetric flow rate} &= 13 \text{ l/sec} \\
 &= \frac{13 \text{ m}^3/\text{sec}}{1000} = 13 \times 10^{-3} \text{ m}^3/\text{sec}
 \end{aligned}$$

$$\text{Jet velocity} = 66 \text{ m/s}$$

$$\text{Water density} = 1000 \text{ kg/m}^3$$

* * Since $p=0$ and $Z=0$; < Jet power >

$$P = (0 \times Q) + \frac{\rho Q \cdot v^2}{2} + \rho g Q (0)$$

$$\Rightarrow P = \frac{\rho Q \cdot v^2}{2}$$

$$= \frac{1000 \times 13 \times 10^{-3} \times 66^2}{2}$$

$$P = 28314 \text{ Watts} \quad \text{--- Power of jet}$$

* * Power supplied from reservoir :

Since $p=0$ and $v=0$;

$$P = (0 \times Q) + \frac{\rho Q (0)^2}{2} + \rho g Q Z$$

$$\Rightarrow P = \rho g Q Z$$

$$= 1000 \times 9.81 \times 13 \times 10^{-3} \times 240$$

$$= 30607.2 \text{ Watts}$$

* * Power lost in transmission = Power of reservoir - Jet power ;

$$= 30607.2 - 28314$$

$$= 2293.2 \text{ Watts}$$

* * Headloss in pipeline, h : power lost in transmission

$$\frac{\rho g Q}{2}$$

$$= \frac{2293.2}{2}$$

$$= \frac{1000 \times 9.81 \times 13 \times 10^{-3}}{2}$$

$$= 17.982 \text{ m}$$

* * Efficiency = $\frac{\text{Jet power}}{\text{Reservoir power}} \times 100\%$

$$= \frac{28314}{30607.2} \times 100\%$$

$$= 92.5\%$$

QUESTION FIVE

$$S_g \text{ of oil} = 0.89$$

$$Z = 30, \text{ m} = 30 \text{ m}$$

$$Q = 200 \text{ l/sec} = 0.22 \text{ m}^3/\text{sec}$$

$$V = 7 \text{ m/sec}$$

Introducing $z=0$, and $p=0$;

$$** P = \frac{\rho Q V^2}{2} \quad \text{--- Jet power}$$

$$\text{Recall, } S_g = 0.89$$

$$S_g = \frac{x}{1000} \quad ; \quad x = 890$$

$$\rho = x = 890$$

$$P = \frac{890 \times 0.22 \times 7^2}{2}$$

$$P = 4797.1 \text{ Watts}$$

** Power supplied from reservoir:

$$P = \rho g Q Z$$

$$= 890 \times 9.81 \times 0.22 \times 300$$

$$= 576239.4 \text{ Watts}$$

$$\underline{=} 576.24 \text{ Watts}$$

** Power loss:

$$= (576.24 - 4.7971) \text{ kW}$$

$$= 571.44 \text{ kilowatts}$$

$$= (576239.4 - 4797.1) \text{ kilowatts}$$

$$= 571.4423 \text{ kilowatts}$$

$$= 571442.3 \text{ Watts} \quad \text{//}$$

* * Head used to overcome losses:

$$= \frac{571442.3}{890 \times 9.81 \times 0.22}$$

$$= 297.51 \text{ m} \quad \text{//}$$

QUESTION SIX

$$P = \rho g Q z$$

$$z = 20 \text{ m} = h$$

$$P = 1 \text{ MW}, \quad g = 9.81$$

$$Q = VA$$

$$d = 10 \text{ cm} = 10 \times 10^{-2} \text{ m}$$

$$A = \frac{\pi d^2}{4} = 7.85 \times 10^{-3} \text{ m}^2$$

The initial velocity is needed while $v = 0$;

$$v^2 = u^2 - 2gh$$

$$u = \sqrt{v^2 + 2gh}$$

$$u = \sqrt{0^2 + 2 \times 9.81 \times 20}, \quad u = \sqrt{392.4}$$

$$u = 19.81 \text{ m s}^{-1}$$

$$Q = VA$$

$$= 19.81 \times 7.85 \times 10^{-3}$$

$$= 0.15558 \text{ m}^3/\text{s} = 0.156 \text{ m}^3/\text{s}$$

$$\therefore P = \rho g Q z$$

$$= 1 \text{ MW} \times 9.81 \times 0.156 \times 20$$

$$= 30.5 \text{ kilowatts}$$

QUESTION SEVEN

$$d_1 = 0.3 \text{ m}$$

$$A_1 = \frac{\pi d^2}{4} = 0.0707 \text{ m}^2$$

$$d_2 = 0.2 \text{ m}, \quad A_2 = 0.0314 \text{ m}^2$$

$$C_d = 0.96$$

$$\text{Sw of gas} = 19.62 \text{ N/m}^3$$

$$\therefore \rho g = 19.62$$

$$\rho = \frac{19.62}{9.81} = 2 \text{ kg/m}^3$$

$$\text{Recall, } Q = A_1 V_1 = A_2 V_2$$

From the above equation;

$$V_1 = \frac{Q}{0.0707}, \quad V_2 = \frac{Q}{0.0314}$$

MANOMETER :

$$P_1 + \rho g Z_1 = P_2 + \rho g (Z_2 - R_p) + \rho_w g R_p$$

$$P_1 - P_2 = 19.62 (Z_2 - Z_1) + 587.423 \quad \text{--- A}$$

VENTURIMETER :

$$\frac{P_1}{\rho g} + \frac{V_1^2}{2g} + Z_1 = \frac{P_2}{\rho g} + \frac{V_2^2}{2g} + Z_2$$

$$P_1 - P_2 = 19.62 (Z_2 - Z_1) + 0.803 V_2^2 \quad \text{--- B}$$

$$\langle Z_2 - Z_1 = 0.06 \text{ m} \rangle$$

Equating A and B :

$$19.62 (Z_2 - Z_1) + 587.423 = 19.62 (Z_2 - Z_1) + 0.803 V_2^2$$

$$0.803 V_2^2 = 587.423$$

$$V_2^2 = \frac{587.423}{0.803}$$

$$V_2^2 = 731.535$$

$$V_2 = \sqrt{731.535}$$

$$V_2 \underline{\underline{=}} 27.047 \text{ m s}^{-1}$$

$$Q_{\text{ideal}} = A_2 V_2$$

$$= 27.047 \times 0.0314$$

$$= 0.8492 \text{ m s}^{-1} \quad \underline{\underline{=}}$$

$$Q_{\text{real}} = C_d \times Q_{\text{ideal}}$$

$$= 0.96 \times 0.8492$$

$$= 0.815 \text{ m s}^{-1} \quad \underline{\underline{=}}$$

QUESTION 8

$$\text{Inlet diameter} = 0.152 \text{ m} \quad \text{--- } d_1$$

$$\text{Throat diameter} = 0.076 \text{ m} \quad \text{--- } d_2$$

$$z_1 - z_2 = 0.914 \text{ m}$$

a) Discharge when pressure gauges read the same :

$$\left(\frac{p_1}{\rho} + \frac{p_2}{\rho} \right) + \left(\frac{V_1^2}{2g} + \frac{V_2^2}{2g} \right) + (z_1 - z_2) = 0$$

$$\rightarrow 0 + \frac{V_1^2}{2g} - \frac{V_2^2}{2g} + 0.914 = 0 \quad \text{--- eqn (*)}$$

→ From continuity equation : $A_1 V_1 = A_2 V_2$

$$V_1 = \frac{A_2 V_2}{A_1}$$

$$V_1 = \frac{\frac{\pi}{4} \times 0.076^2 \times V_2}{\frac{\pi}{4} \times 0.152^2}$$

$$V_1 = 0.25 V_2$$

Substitute " $V_1 = 0.25 V_2$ " into eqn (*) ;

$$\rightarrow \frac{(0.25 V_2)^2}{2g} - \frac{V_2^2}{2g} + 0.914 = 0$$

$$\rightarrow \left(\frac{0.0625 \times V_2^2}{2g} \right) - \frac{V_2^2}{2g} + 0.914 = 0$$

$$\rightarrow \left(\frac{0.0625}{2 \times 9.81} \times V_2^2 \right) - \left(\frac{V_2^2}{2 \times 9.81} \right) + 0.914 = 0$$

$$\rightarrow 0.00319 V_2^2 - \frac{V_2^2}{19.62} + 0.914 = 0$$

$$\rightarrow V_2^2 \left(0.00319 - \frac{1}{19.62} \right) + 0.914 = 0$$

$$\rightarrow V_2^2 (-0.0478) + 0.914 = 0$$

$$\rightarrow V_2^2 = \frac{-0.914}{-0.0478} = 19.12$$

$$V_2 = \sqrt{19.12} = 4.37 \text{ m s}^{-1}$$

~~Discharge, $Q = A_2 V_2$~~

$$\text{ ~~} Q = \frac{3.142 \times 0.076^2}{4} \times 6.92~~$$

$$\text{ ~~} Q = 0.031 \text{ m}^3 \text{ s}^{-1}~~$$

$$\rightarrow V_2^2 = \frac{-0.914}{-0.0478} = 19.12$$

$$V_2 = \sqrt{19.12} \\ = 4.37 \text{ m s}^{-1}$$

Discharge, $Q = A_2 V_2$

$$= \frac{3.142 \times 0.076^2}{4} \times 4.37$$

$$= 0.0198 \text{ m}^3 \text{ s}^{-1}$$

QUESTION 9

Diameter at S1, $d_1 = 300 \text{ mm} = 0.3 \text{ m}$

Diameter at S2, $d_2 = 150 \text{ mm} = 0.15 \text{ m}$

$Z_1 = 10$, $Z_2 = 6$

$P_1 = 40 \text{ kN/m}^2 = 40 \times 10^3 \text{ N/m}^2$

From continuity equation, $Q = A_1 V_1$

$[Q = 40 \text{ ltr/sec} = 0.04 \text{ m}^3/\text{sec}]$

$$0.04 = \frac{\pi \times d_1^2}{4} V_1 = \frac{3.142 \times 0.3^2}{4} V_1 = 0.071 V_1$$

$$0.04 = 0.071 V_1$$

$$V_1 = \frac{0.04}{0.071} = 0.56 \text{ m/s}$$

Recall, $A_1 V_1 = A_2 V_2$

$$0.071 \times 0.56 = \frac{3.142 \times 0.15^2}{4} V_2$$

$$0.04 = 0.0177 V_2 \quad ; \quad V_2 = \frac{0.04}{0.0177}$$

$$V_2 = 2.26 \text{ m/s}$$

From Bernoulli's equation;

$$\frac{P_1}{\rho} + \frac{V_1^2}{2g} + Z_1 = \frac{P_2}{\rho} + \frac{V_2^2}{2g} + Z_2$$

$$\frac{40 \times 10^3}{1000 \times 9.81} + \frac{0.56^2}{2 \times 9.81} + 10 = \frac{P_2}{1000 \times 9.81} + \frac{2.26^2}{2 \times 9.81} + 6$$

$$\frac{(40 \times 10^3) - P_2}{1000 \times 9.81} + \left(\frac{0.56^2 - 2.26^2}{2 \times 9.81} \right) + 4 = 0$$

$$\Rightarrow \frac{407.75 - P_2}{9810} + (-0.244) + 4 = 0$$

$$\rightarrow P_2 = 9810 (407.75 - 0.244 + 4)$$

$$\rightarrow P_2 = 4.04 \times 10^6 \text{ N/m}^2$$

QUESTION 10

Velocity of the submarine, $V = \sqrt{2gH}$

$$H = y \left(\frac{\text{SG of mercury} - \text{SG of water}}{\text{SG of water}} \right)$$

$$H = 0.17 \left(\frac{13.6 - 1.026}{1.026} \right)$$

$$= 0.17 \times 12.26$$

$$= 2.0842 \text{ m}$$

$$V = \sqrt{2 \times 9.81 \times 2.0842}$$

$$= 6.39 \text{ ms}^{-1}$$

\therefore the speed of the sub-marine = 6.39 ms^{-1} //