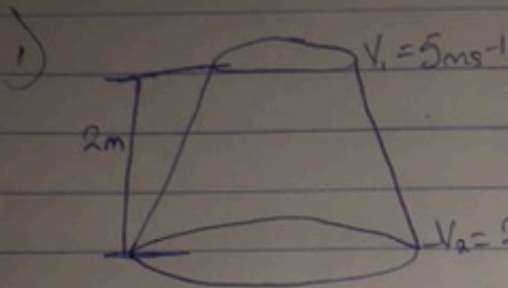


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18/ENG-08/045

Mechanical Engineering
ENG 2 (Fluid mechanics)



$$P_{T1} = \frac{P_1}{\omega} = 2.5 \text{ m}$$

$$H_w = \frac{0.35 (V_1 - V_2)^2}{2g}$$

using Bernoulli's equation, $\frac{P_2}{\omega} = ?$

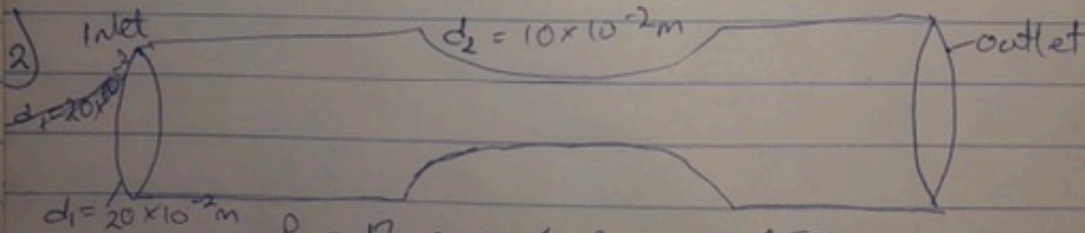
$$\therefore \frac{P_1}{\omega} + \frac{V_1^2}{2g} + Z_1 = \frac{P_2}{\omega} + \frac{V_2^2}{2g} + Z_2 + H_w$$

$$\therefore \frac{P_2}{\omega} = \frac{P_1}{\omega} + \left[\frac{V_1^2 - V_2^2}{2g} \right] + [Z_1 - Z_2] - H_w$$

$$\frac{P_2}{\omega} = 2.5 + \left[\frac{5^2 - 2^2}{2 \times 9.81} \right] + 2 - \frac{0.35 (5 - 2)^2}{2 \times 9.81}$$

$$\frac{P_2}{\omega} = \underline{\underline{5.409 \text{ m}}}$$

\therefore The pressure head at the lower end = 5.409 m



$$P_1 = 17.658 \text{ N/cm}^2 = 17.658 \times 10^4 \text{ N/m}^2, C_d = 0.98$$

$$P_2 = 300 \text{ mmHg} = 300 \times 10^{-2} \text{ mmHg}, Q = ?$$

$$A_1 = \frac{\pi \times (20 \times 10^{-2})^2}{4}, A_2 = \frac{\pi \times (10 \times 10^{-2})^2}{4}$$

$$A_1 = \underline{\underline{0.0314 \text{ m}^2}}$$

$$A_2 = 7.85 \times 10^{-3} \text{ m}^2$$

$$\frac{P_2}{\omega} = 0.2 \times 13.6 = \underline{\underline{2.72 \text{ mHg}}}$$

= 4.08 mHg (since vacuum pressure)

$$\frac{P_1}{\omega} = \frac{17.058 \times 10^4}{9.81 \times 10^5} = \underline{18 \text{ mHg}}$$

$$h = \frac{P_1}{\omega} - \frac{P_2}{\omega} = \frac{18 - (-4.08)}{\omega} = \underline{22.08}$$

$$Q = \frac{C_d A_1 A_2 \sqrt{2gh}}{\sqrt{A_1^2 - A_2^2}}$$

$$Q = \frac{0.98 \times 0.03 \times (7.85 \times 10^{-3}) \times \sqrt{2 \times 9.81 \times 22.08}}{\sqrt{(0.03^2 - (7.85 \times 10^{-3})^2)}}$$

$$Q = \underline{0.166 \text{ m}^3/\text{s}}$$

$$3) A_0 = 15 \times 10^{-2} \text{ m}$$

$$A_0 = \frac{\pi \times (15 \times 10^{-2})^2}{4} = 0.0177 \text{ m}^2$$

$$A_1 = \frac{\pi \times (30 \times 10^{-2})^2}{4} = 0.0707 \text{ m}^2$$

$$H = 50 \times 10^{-2} \left[\frac{13.6 - 1}{0.9} \right]$$

$$H = 7.055 \text{ m}$$

$$Q = \frac{0.64 \times 0.0177 \times 0.0707 \sqrt{2 \times 9.81 \times 7.055}}{\sqrt{0.0177^2 - 0.0707^2}}$$

$$Q = \underline{0.187 \text{ m}^3/\text{s}}$$

$$d_1 = 30 \times 10^{-2} \text{ m}$$

$$C_d = 0.64$$

$$y = 50 \times 10^{-2} \text{ mHg}$$

$$Q = ?$$

$$\text{S.G. of oil} = 0.9$$

$$S_{hi} = 13.6$$

$$S_o = 0.9$$

$$H = y \left(\frac{S_{hi} - 1}{S_o} \right)$$

$$\therefore Q = \frac{C_d A_0 A_1 \sqrt{2gh}}{\sqrt{A_1^2 - A_0^2}}$$

$$4) y = 170 \text{ mmHg} = 170 \times 10^{-3} \text{ mHg}$$

$$\text{S.g. of mercury} = 13.6 \text{ Hg}$$

$$\text{S.g. of Sea water} = 1.026$$

$$H = y \times \left(\frac{S_{hi} - 1}{S_o} \right)$$

$$H = 170 \times 10^{-3} \times \left(\frac{13.6 - 1}{1.026} \right)$$

$$H = 2.08$$

$$\therefore V = \sqrt{2gh}$$

$$V = \sqrt{2 \times 9.81 \times 2.08}$$

$$V = \underline{6.39 \text{ m/s}}$$

Name:

$$5) \text{ Actual flowrate } (Q) = 0.05 \text{ m}^3 = 5 \text{ dm}^3/\text{min} = 8.33 \times 10^{-5} \text{ m}^3/\text{sec}$$

$$P = 15 \text{ bar} = 15 \times 10^5 \text{ N/m}^2$$

$$V = 1700 \text{ rev/min} = 28.33 \text{ rev/sec}$$

$$T = 15 \text{ Nm}, \text{ Normal displacement } \bar{V} = 10 \text{ cm}^3/\text{rev} = 10 \times 10^{-6} \text{ m}^3/\text{rev}$$

1) Volumetric efficiency

$$\frac{\text{Actual flowrate}}{\text{Ideal flowrate}} \times 100\%$$

$$\text{Ideal flowrate} = \text{displacement} \times \text{Velocity}$$

$$Q = 10 \times 10^{-6} \times 28.33$$

$$= 2.833 \times 10^{-4} \text{ m}^3/\text{sec}$$

$$\therefore \text{Volumetric Efficiency} = \frac{8.33 \times 10^{-5}}{2.833 \times 10^{-4}} \times 100$$
$$= \underline{\underline{29.4\%}}$$

$$2) \text{ Fluid power} = (Q \times \Delta P)$$

$$= 8.33 \times 10^{-5} \times 15 \times 10^5 = 12495 \text{ watts}$$

$$3) \text{ Shaft power} = T \times \omega$$

$$\omega = 2 \times \pi \times V$$

$$\omega = 2 \times \pi \times 28.33 = 178 \text{ watts/sec}$$

$$\text{Shaft power} = T \times \omega$$

$$= 15 \times 178$$

$$= \underline{\underline{2670 \text{ watts}}}$$

$$4) \text{ Overall Efficiency} =$$

$$= \frac{\text{Fluid power}}{\text{Shaft power}} \times 100\%$$

$$= \frac{124.95}{2670} \times 100$$

$$= \underline{\underline{4.68\%}}$$