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Case: 2D flow

- fluid mechanics

∴ length $L = 2.0m$

The velocity flow at source end: $V_1 = 5m/s$

The velocity flow at lower end: $V_2 = 2m/s$

Let the pressure head at the source end: $P_1 = 2.5m$ of liquid

$$\begin{aligned} \text{Let the loss of head: } h_L &= \frac{0.25(V_1 - V_2)^2}{2g} \\ &= \frac{0.25(5 - 2)^2}{2 \times 9.81} = 0.161m \end{aligned}$$

Let the pressure head at the lower end: $P_2 = ?$

Applying Bernoulli equation

$$\frac{P_1}{\rho g} + \frac{V_1^2}{2g} + z_1 = \frac{P_2}{\rho g} + \frac{V_2^2}{2g} + z_2 + h_L$$

Let $z_1 = \frac{P_1}{\rho g}$ and $z_2 = \frac{P_2}{\rho g}$ (determine pressure head)

$z_1 = 2.5$ and $z_2 = 0$ (determine pressure head)

Input the values

$$2.5 + \frac{5^2}{2 \times 9.81} + 2.5 = \frac{P_2}{\rho g} + \frac{2^2}{2 \times 9.81} + 0 + 0.161$$

$$\frac{P_2}{\rho g} = 2.5 + \frac{2.5}{19.62} + 2 - \left(\frac{4}{19.62} + 0.161 \right) = P_2$$

$$= 3.774 - 0.365 = P_2$$

$$P_2 = 3.409m \text{ of fluid}$$

2) Let inlet diameter: $D_1 = 20cm$

Let throat diameter: $D_2 = 10cm$

$$\text{Let inlet area} = A_1 = \frac{\pi D_1^2}{4} = \frac{\pi (20)^2}{4} = 314.16cm^2$$

$$\text{Let throat area} = A_2 = \frac{\pi D_2^2}{4} = \frac{\pi (10)^2}{4} = 78.54cm^2$$

Density of water $\rho = 1000 \text{ kg/m}^3$
pressure at inlet $= 17.6584 \text{ cm}^2 = 17.658 \times 10^7 \text{ N/m}^2$

$$\frac{P_1}{\rho g} = \frac{17.658 \times 10^7}{1000 \times 9.81} = 18 \text{ m}$$

$$\frac{P_2}{\rho g} = -30 \text{ cm of mercury, } \rho_{\text{Hg}} = 13.6$$

$$\frac{P_2}{\rho g} = -30 \times 10^{-2} \text{ of mercury} \times 13.6 \\ = -4.08 \text{ m}$$

$$\text{Differential head} = H = \frac{P_1}{\rho g} - \frac{P_2}{\rho g} \\ = 18 - (-4.08) \\ = 18 + 4.08 = 22.08 \text{ m} \times 100 \\ h = 2208 \text{ cm}$$

$$\text{Using } Q = \frac{C_d \sqrt{2gh} \cdot A_1 \cdot A_2}{\sqrt{A_1^2 - A_2^2}} \\ = \frac{0.95 \times \sqrt{2 \times 9.81 \times 2208} \times 0.11416 \times 78.54}{\sqrt{314.16^2 - 18.54^2}} \\ = \frac{0.95 \times 2081.37 \times 24674.1264}{304.18412} \\ = 160455 \text{ cm}^3/\text{s} \\ = \frac{160455 \text{ l}}{1000} = 160.455 \text{ l/sec}$$

3. $d_1 = 30 \text{ cm}$

$$A_1 = \frac{\pi d_1^2}{4} = \frac{\pi (30)^2}{4} = 706.86 \text{ cm}^2$$

diameter of orifice $d_2 = 15 \text{ cm}$

$$A_2 = \frac{\pi d_2^2}{4} = \frac{\pi (15)^2}{4} = 176.72 \text{ cm}^2$$

specific gravity of oil $S_o = 0.9$

specific gravity mercury, $S_{\text{Hg}} = 13.6$

Differential manometer reading, $x = 60 \text{ cm of mercury}$

Coefficient of discharge, $C_d = 0.64$

Differential head, $h = x \left(\frac{\rho_2}{\rho_1} - 1 \right)$

$$h = 20 \left(\frac{10.6}{8.7} - 1 \right)$$

$$h = 705.86 \text{ mm of oil}$$

The rate of flow of oil = $Q = C_d \sqrt{2gh} \cdot A_1 \cdot A_2$
 $\frac{A_1}{A_2} = \frac{A_1^2 - A_2^2}{A_2^2}$

$$Q = 0.64 \frac{\sqrt{2 \times 9.81 \times 705.86} \times 706.86 \times 176.72}{\sqrt{106.86^2 - 176.72^2}}$$

$$Q = 137443.29 \text{ cm}^3/\text{s}$$

$$Q = \frac{137443.29}{1000} = 137.44 \text{ l/s}$$

4) The difference of mercury level, $x = 116 \text{ mm} = 116 \times 10^{-3} = 0.116 \text{ m}$

The specific gravity of mercury $S_g = 13.6$

The specific gravity of sea water, $S_s = 1.026$

Speed, $V = ?$

$$V = \sqrt{2gh} \quad , \quad h = ?$$

$$h = x \left[\frac{S_g}{S_s} - 1 \right] = 0.116 \left[\frac{13.6}{1.026} - 1 \right]$$

$$\therefore V = \frac{\sqrt{2 \times 9.81 \times 2.0834 \text{ m}}}{1} = 6.393 \text{ m/s}$$

$$\text{In km/hr} \quad V = \frac{6.393 \times 60^2}{1000} = 23.61 \text{ km/hr}$$

5) $Q = 0.05 \text{ m}^3/\text{min} = 50 \text{ dm}^3/\text{min}$

$$P_0 = 15 \text{ bar} = 15 \times 10^5 \text{ N/m}^2$$

speed = 170 rpm

$$T = 15 \text{ Nm}, \quad M_p = 10 \text{ cm}^3/\text{rev}$$

i) Volumetric efficiency = $\frac{\text{Actual flow rate}}{\text{Ideal flow rate}}$

$$\begin{aligned} \text{Ideal flow rate} &= \text{cross-sectional area} \times \text{speed} \\ &= 10 \text{ cm}^2/\text{sec} \times 1700 \text{ m}/\text{min} \\ &= 17000 \text{ cm}^3/\text{min} \end{aligned}$$

$$\text{Ideal flow rate} = \frac{17000}{1000000} = 0.017 \text{ m}^3/\text{min}$$

$$\text{Actual flow rate} = 0.05 \text{ m}^3/\text{min}$$

$$\text{Volumetric efficiency} = \frac{0.05}{0.017} = 294\%$$

$$\text{ii fluid power} = P \times Q$$

$$P = 15 \times 10^5 \text{ N/m}^2$$

$$Q = 0.05 \text{ m}^3/\text{min} = \frac{0.05}{60} = 8.33 \times 10^{-4} \text{ m}^3/\text{s}$$

$$\begin{aligned} \text{fluid power} &= 15 \times 10^5 \times 8.33 \times 10^{-4} \\ &= 15 \times 10^5 \times 8.33 \times 10^{-5} \\ &= 1249.5 \times 10^{-5} \end{aligned}$$

$$\text{fluid power} = 1249.5 \text{ Watts}$$

$$\text{iii shaft power} = \frac{24 \text{ kW}}{60} = \frac{24 \times 1700 \times 15}{60}$$

$$\text{Shaft power} = 2670.35 \text{ Watts}$$

$$\begin{aligned} \text{iv Overall efficiency} &= \frac{\text{fluid power}}{\text{shaft power}} = \frac{1249.5}{2670.35} \\ &= 0.468 \end{aligned}$$

$$\begin{aligned} \text{Overall efficiency} &= 0.468 \times 100 \\ &= 46.8\% \end{aligned}$$

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list inquiry