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Chemical Engineering

1. $V_1 = 5 \text{ ms}^{-1}$ $P_L = ?$
 $V_2 = 2 \text{ ms}^{-1}$
 $P_3 = 2.5 \text{ m of liquid}$

$$H_L = \frac{0.35(V_1 - V_2)^2}{2g}$$
$$= \frac{0.35(5-2)^2}{2 \times 9.81}$$
$$= 0.161 \text{ m}$$

Apply Bernoulli's Equation

$$\frac{P_1}{\rho g} + \frac{V_1^2}{2g} + Z_1 = \frac{P_2}{\rho g} + \frac{V_2^2}{2g} + Z_2 + H_L$$

$$P_3 = \frac{P_1}{\rho g} \quad P_L = \frac{P_2}{\rho g}$$

$$Z_1 = 2 \text{ and } Z_2 = 0$$

$$\Rightarrow 2.5 + \frac{5^2}{2 \times 9.81} + 2 = P_L + \frac{2^2}{2 \times 9.81} + 0 + 0.161$$

$$\Rightarrow 2.5 + \frac{25}{19.62} + 2 = P_L + \frac{4}{19.62} + 0.161$$

$$\Rightarrow 2.5 + \frac{25}{19.62} + 2 - \frac{4}{19.62} - 0.161 = P_L$$

$$\Rightarrow P_L = 5.41 \text{ m}$$

2. $D_1 = 20 \text{ cm}$

$$D_2 = 10 \text{ cm}$$

$$A_1 = \frac{\pi(20^2)}{4} = 314.16 \text{ cm}^2$$

$$A_2 = \frac{\pi(10^2)}{4} = 78.54 \text{ cm}^2$$

ρ

$$\rho = 1000 \text{ kg/m}^3$$

$$\text{Pressure at inlet} = 17.658 \text{ N/cm}^2 = 17.658 \times 10^4 \text{ N/m}^2$$

$$\therefore \frac{P_1}{\rho g} = \frac{17.658 \times 10^4}{1000 \times 9.81} = 18 \text{ m}$$

$$\frac{P_2}{\rho g} = -30 \text{ cm of mercury, s.g. Hg} = 13.6$$

$$\begin{aligned} \frac{P_2}{\rho g} &= -30 \times 10^{-2} \text{ m of mercury} \times 13.6 \\ &= -4.08 \text{ m} \end{aligned}$$

$$\text{Let Differential Head} = h = \frac{P_1}{\rho g} - \frac{P_2}{\rho g}$$

$$= 18 - (-4.08)$$

$$= 22.08 \text{ m} \times 100$$

$$= 2208 \text{ cm}$$

$$\text{Using } Q = \frac{C_d \sqrt{2gh} \cdot A_1 A_2}{\sqrt{A_1^2 - A_2^2}}$$

$$\Rightarrow \frac{0.98 \times \sqrt{2 \times 9.81 \times 2208} \times 314.16 \times 78.54}{\sqrt{(314.16)^2 - (78.54)^2}}$$

$$\Rightarrow \frac{0.98 \times 2081.37 \times 24674.1264}{304.184112}$$

$$\Rightarrow 165455.3 \text{ cm}^3/\text{s}$$

$$\Rightarrow \frac{165455.3}{1000} = 165.455 \text{ lit/sec}$$

3. $d_1 = 30 \text{ cm}$

$$A_1 = \frac{\pi d_1^2}{4} = 1706.86 \text{ cm}^2$$

$$d_2 = 15 \text{ cm}$$

$$A_2 = 176.72 \text{ cm}^2$$

$$\rho_o \text{ of oil, } S_o = 0.9$$

$$S_{Hg} = 13.6$$

$$X = 50 \text{ cm of mercury}$$

$$C_d = 0.64$$

$$h = X \left(\frac{S_{Hg}}{S_o} - 1 \right)$$

$$= 50 \left(\frac{13.6}{0.9} - 1 \right) \Rightarrow 705.56 \text{ cm of oil}$$

Rate of flow

$$Q = \frac{C_d \sqrt{2gh} \cdot A_1 A_2}{\sqrt{A_1^2 - A_2^2}}$$

$$= \frac{0.64 \sqrt{2 \times 9.81 \times 705.56} \times 1706.86 \times 176.72}{\sqrt{(1706.86^2) - (176.72^2)}}$$

$$= 137443.29 \text{ cm}^3/\text{sec}$$

$$\Rightarrow \frac{137443.29}{1000} = 137.44 \text{ litres/sec}$$

4. $X = 170 \text{ mm} = 0.17 \text{ m}$

$$S_{Hg} = 13.6$$

$$S_o = 1.026$$

$$V = ?$$

$$v = \sqrt{2gh} \quad h = ?$$

$$h = x \left(\frac{S_1}{S_2} - 1 \right) = 0.17 \left(\frac{13.6}{1.026} - 1 \right)$$
$$= 2.0834 \text{ m}$$

$$\therefore v = \sqrt{2 \times 9.81 \times 2.0834} \Rightarrow 6.393 \text{ m/s}$$

$$\frac{6.393 \times 60^2}{1000} = 23.01 \text{ km/hr}$$

5. $Q = 0.05 \text{ m}^3/\text{min} = 50 \text{ dm}^3/\text{min}$

$$P_0 = 15 \text{ bar} = 15 \times 10^5 \text{ N/m}^2$$

$$\text{Speed} = 1700 \text{ rev/min}$$

$$T = 15 \text{ Nm}$$

$$ND = 10 \text{ cm}^3/\text{rev}$$

i) Volumetric efficiency = $\frac{\text{Actual flow rate}}{\text{Ideal flow rate}}$

$$\text{Ideal flow rate} = \text{Nominal flow rate} \times \text{speed}$$

$$= 10 \text{ cm}^3/\text{rev} \times 1700 \text{ rev/min}$$

$$= 17000 \text{ cm}^3/\text{min}$$

$$\Rightarrow \frac{17000}{1000000} = 0.017 \text{ m}^3/\text{min}$$

$$\text{Actual flow rate} = 0.05 \text{ m}^3/\text{min}$$

$$\therefore \text{Volumetric Efficiency} = \frac{0.05}{0.017} = 2.94 = 294\%$$

$$\begin{aligned} \text{ii) Fluid power} &= P \times Q \\ &= 15 \times 10^5 \times \frac{0.05}{60} \\ &= 12495 \text{ watts} \end{aligned}$$

$$\begin{aligned} \text{iii) Shaft Power} &= \frac{2\pi NT}{60} \\ &= \frac{2 \times \pi \times 1700 \times 15}{60} \\ &= 2670.35 \text{ watts} \end{aligned}$$

$$\text{iv) Overall Efficiency} = \frac{\text{Fluid Power}}{\text{Shaft Power}}$$

$$\Rightarrow \frac{1249.5}{2670.35} = 0.468$$

$$\Rightarrow 0.468 \times 100 = 46.8\%$$