

JOHN EDWIN AKPAN  
18/ENGG 06/033  
MECHANICAL ENGR.  
ENGG 214

(1) Given data:

$$\text{Flow rate (Q)} = 10 \text{ dm}^3/\text{min}$$

$$\text{pressure change } (\Delta P) = 12 \text{ bar}$$

$$\text{Speed (N)} = 1500 \text{ rpm}$$

$$\text{Normal Displacement} = 10 \text{ cm}^3/\text{rev}$$

$$\text{Torque input (T)} = 12.5 \text{ N-m}$$

Solution.

$$\begin{aligned} \text{Flow rate} &= \text{Normal Displac} \times \text{Speed} = 10 \text{ cm}^3/\text{rev} \\ &\times 1500 \text{ rpm} \\ &= 15000 \text{ cm}^3/\text{min} = 15 \text{ dm}^3/\text{min} \end{aligned}$$

$$(i) \text{ Volumetric efficiency} = \frac{\text{Actual Flow}}{\text{Ideal flow}} = \frac{10}{15} = 0.6667$$

(ii)

$$Q = \frac{10 \times 10^{-03}}{60} \text{ m}^3/\text{sec} = 16.7 \times 10^{-05} \text{ m}^3/\text{sec}$$

$$\Delta P = 12 \times 10^5 \text{ N/m}^2$$

$$\begin{aligned} \text{Fluid power} &= \Delta P \times Q = 16.7 \times 10^{-05} \text{ m}^3/\text{sec} \\ &\times 12 \times 10^5 \text{ N/m}^2 = 200 \text{ Watts} \end{aligned}$$

$$\begin{aligned} \text{Shaft Power} &= \frac{2\pi NT}{60} = \frac{2\pi \times 1500 \times 12.5}{60} \\ &= 1963.5 \text{ Watts} \end{aligned}$$

$$\begin{aligned} \text{Overall efficiency} &= \text{F.P} / \text{S.P} = \frac{200}{1963.5} \\ &= 0.102 \text{ or } 10.2\% // \end{aligned}$$

(7) Question 7

$$\rho_{gg} = 19.62 \text{ N/m}^3$$

$$C_d = 0.96$$

$$d_1 = 0.3 \text{ m}$$

$$d_2 = 0.2 \text{ m}$$

Calculate  $Q$

$$V_1 = Q / 0.0707$$

$$V_2 = Q / 0.0314$$

for the manometer.

$$P_1 \neq P_2$$

$$P_1 + \rho_{gg} z_1 = P_2 + \rho_{gg} (z_2 - R_f) + \rho_{wg} R_f \quad \text{--- (1)}$$

$$P_1 - P_2 \Rightarrow 19.62 (z_2 - z_1) + 587.423 \quad \text{--- (1)}$$

For the manometer.

$$\frac{P_1}{\rho_{gg}} + \frac{V_1^2}{2g} + z_1 = \frac{P_2}{\rho_{gg}} + \frac{V_2^2}{2g} + z_2$$

$$P_1 - P_2 = 19.62 (z_2 - z_1) + 0.803 V_2^2 \quad \text{--- (2)}$$

Combining 1 & 2 we get

$$0.803 V_2^2 = 587.423$$

$$V_{2 \text{ ideal}} = 27.047 \text{ m/s}$$

$$Q_{\text{ideal}} = 27.047 \times \pi \times \left(\frac{0.2}{2}\right)^2 = 0.85 \text{ m}^3/\text{s}$$

$$Q = C_d Q_{\text{ideal}} = 0.96 \times 0.85 = 0.816 \text{ m}^3/\text{s} //$$

Continuation of Number 9

$$40.77 + 0.0288 + 10 = \frac{P_2}{1000 \times 9.81} + 6.115$$

$$\Rightarrow 50.7988 = \frac{P_2}{9810} + 6.115$$

$$\frac{P_2}{9810} = 50.7988 - 6.115 = 44.6838$$

$$P_2 = 44.6838 \times 9810$$

$$P_2 = 438348.078 \text{ N/m}^2 //$$

Question 9.

Solution

Given

At Section 1

$$D_1 = 300 \text{ mm} = 0.3 \text{ m}$$

$$A_1 = \frac{\pi}{4} (0.3)^2 = 0.070695 \text{ m}^2$$

$$P_1 = 400 \text{ kN/m}^2 = 400000 \text{ N/m}^2$$

$$Z_1 = 10 \text{ m}$$

At Section 2

$$D_2 = 0.15 \text{ m}$$

$$A_2 = \frac{\pi}{4} (0.15)^2 = 0.0177 \text{ m}^2$$

$$Z_2 = 6 \text{ m}$$

$$P_2 = ?$$

$$\text{Rate of flow or Discharge } Q = 40 \text{ lit/sec} = \frac{40}{1000}$$

$$= 0.040 \text{ m}^3/\text{sec}$$

$$\text{Now } Q = A_1 V_1 = A_2 V_2$$

$$\therefore V_1 = \frac{Q}{A_1} = \frac{0.040}{0.070695} = 0.566 \text{ m/s}$$

$$V_2 = \frac{Q}{A_2} = \frac{0.040}{0.0177} = 2.2599 \text{ m/s}$$

Applying Bernoulli's equation at section 1 and 2, we get

$$\frac{P_1}{\rho g} + \frac{V_1^2}{2g} + Z_1 = \frac{P_2}{\rho g} + \frac{V_2^2}{2g} + Z_2$$

$$\frac{400000}{1000 \times 9.81} + \frac{0.566^2}{2 \times 9.81} + 10 = \frac{P_2}{1000 \times 9.81} + \frac{2.2599^2}{2 \times 9.81} + 6$$

Question 8.

$$d_1 = 0.152 \text{ m} \Rightarrow A_1 = \frac{\pi}{4} (0.152)^2 = 0.01814 \text{ m}^2$$

$$d_2 = 0.076 \text{ m} \Rightarrow A_2 = \frac{\pi}{4} (0.076)^2 = 0.00454 \text{ m}^2$$

$$\rho = 0.8 \times 1000 = 800 \text{ kg/m}^3$$

$$C_d = 0.97$$

→ Applying Bernoulli's

$$\frac{P_1}{\rho g} + \frac{V_1^2}{2g} + Z_1 = \frac{P_2}{\rho g} + \frac{V_2^2}{2g} + Z_2$$

$$a) P_1 = P_2$$

$$\frac{V_1^2}{2g} + Z_1 = \frac{V_2^2}{2g} + Z_2$$

By Continuity

$$Q = V_1 A_1 = V_2 A_2$$

$$V_2 = V_1 \frac{A_1}{A_2} = V_1 (9)$$

$$\frac{V_1^2}{2g} + 0.314 = \frac{1.6 (V_1^2)}{2g}$$

$$V_1 = \sqrt{\frac{0.314 \times 2 \times 9.81}{1.5}} = 1.0934 \text{ m/s}$$

$$Q = C_d A_1 V_1 = 0.97 \times (0.01814) \times (1.0934)$$

$$Q = 0.0192 \text{ m}^3/\text{s}$$

$$(b) P_1 - P_2 = 15170$$

$$\rightarrow \frac{P_1 - P_2}{\rho g} = \frac{V_2^2 - V_1^2}{2g} - 0.914$$

$$\frac{15170}{800 \times 9.81} = \frac{Q^2 (220.43^2 - 55.11^2)}{2 \times 9.81} - 0.914$$

$$Q = 0.035 \text{ m}^3/\text{s} //$$

Question 6

$$\text{Power} = \frac{\text{work done}}{\text{time}}$$

$$\text{work done} = \frac{mgh}{\text{time}}$$

$v$  = Velocity of Stream.

$\rho$  = Density of water ( $1000 \text{ kg/m}^3$ )

$$\dot{m} = \rho \times v$$

$$v = \sqrt{2gh} = \sqrt{2 \times 9.81 \times 20}$$

$$= 19.7989 \text{ m/s}$$

$$P = \rho \pi r^2 v \frac{gh}{t}$$

$$\text{Power} = 1000 \times \left( \frac{10 \times 10^{-2}}{2} \right)^2 \times 19.7989 \times 9.8 \times 20$$

$$= 1000 \times \pi \times 2.5 \times 10^{-3} \times 19.7959 \times 9.8 \times 20$$

$$\Rightarrow 30478.03 \text{ W}$$

$$\text{Power} = 30478.03 \text{ W} //$$

JOHN EDWIN AKPAM.  
18/ENGA 061033  
MECHANICAL ENGA.  
ENGA 06214.

Question 5

$$\rho = 890 \text{ kg/m}^3$$

$$H = 300 \text{ m}$$

$$Q = 220 \text{ L/s} = 0.22 \text{ m}^3/\text{s}$$

$$V = 7 \text{ m/s}$$

(1) Power of jet  $P = \frac{1}{2} \times \rho Q V^2 = \frac{1}{2} \times 890 \times 0.22 \times 7^2$   
 $P = 4797.1 \text{ Watt} = 4.797 \text{ kW.}$

(2) Power supplied from reservoir  $\bar{P} = \rho Q H$   
 $= 890 \times 9.81 \times 0.22 \times 300$   
 $\bar{P} = 576239.4 \text{ W}$   
 $\bar{P} = 576.239 \text{ kW}$

(3) Power supplied from reservoir =  $\rho Q H$   
 $= 890 \times 0.22 \times 300 = 58740 \text{ kg m/sec}$

Power issuing jet =  $\frac{1}{2} \rho V^2 Q = \frac{1}{2} \times \frac{890}{9.81} \times 7^2 \times 0.22$   
 $= 489 \text{ kg m/s.}$

Power lost in transmission =  $\rho Q h = 58740 - 489$   
 $= 58251 \text{ kg m/s.}$

or  $h = \frac{58251}{890 \times 0.22} = 297.50 \text{ m}$

(4)  $\eta = \frac{\text{power of jet}}{\text{power supplied}} = \frac{489}{58740} = 0.0083 = 0.8324\%$

Question 4

Solution.

$$\begin{aligned} \text{(i) Power of jet} &= \frac{1}{2} \rho V^2 Q \\ &= \frac{1}{2} \times \frac{1000}{9.81} \times 66^2 \times 0.13 \\ &= 28862 \text{ kgm/sec} \\ &= 28862 \times 9.81 \\ &= 283140 \text{ W} = 283.14 \text{ kW} \end{aligned}$$

(ii) At the reservoir, pressure is atmospheric and velocity of free surface is zero,  $\phi = 0$ ,  $V = 0$

$$\begin{aligned} \text{Power supplied from reservoir} &= \rho Q g z \\ &= \gamma Q z \end{aligned}$$

$$\begin{aligned} &= 1000 \times 0.13 \times 240 \\ &= 31200 \text{ kgm/sec} \\ &= 31200 \times 9.81 = 306072 \text{ W} \\ &= 306.072 \text{ kW} \end{aligned}$$

(iii) if  $H_1$  = Total head at the reservoir  
 $H_2$  = Total head at the jet  
 $h$  = head loss in transmission

a. power supplied from reservoir =  $\gamma Q H_1 = 31200 \text{ kgm/sec}$

b. power of issuing jet =  $\gamma Q H_2 = 28862 \text{ kgm/sec}$

a - b = c, power lost in transmission =  $\gamma Q h = 2338 \text{ kgm/sec}$

$$\begin{aligned} \text{Head loss in pipe} &= h = (\text{power lost}) / \gamma Q \\ &= h = 2338 / (1000 \times 0.13) \\ &h = 17.98 \text{ m} \end{aligned}$$

$$40000 = 416.67Q + 0.0625Q^2$$

$$\Rightarrow Q = 94.65 \text{ ft/day}$$



Question 3 Continues

Overall efficiency of the pump is given as

$$\eta_o = \frac{S_g Q_H}{P_{\text{shaft}}}$$

$$S_g H = \Delta P = 100 \text{ bar} = 100 \times 10^5 \text{ N/m}^2$$

$$Q = Q_{\text{actual}} = 35 \text{ dm}^3/\text{min}$$

$$= \frac{35 \times 10^{-3}}{60} = 5.8333 \times 10^{-4} \text{ m}^3/\text{sec}$$

$$(P)_{\text{shaft}} = 15 \text{ Kwatts} = 15 \times 10^3 \text{ watts}$$

$$\eta_o = \frac{100 \times 10^5 \times 5.8333 \times 10^{-4} \times 100}{15 \times 10^3}$$

$$\eta_o = 38.88\%$$

Question 2

$Q_{\text{actual}} = \text{Volume flow rate from the pump.}$

$$= 35 \text{ dm}^3/\text{min}$$

$$= \frac{35 \times 10^{-3}}{60} \text{ m}^3/\text{sec} = 5.8333 \times 10^{-4} \text{ m}^3/\text{sec}$$

$$\text{pressure change} = \Delta P = 100 \text{ bar} = 100 \times 10^5 \text{ Pa}$$
$$= 100 \times 10^5 \text{ N/m}^2$$

Overall efficiency of pump is given as

$$\eta_o = \frac{S_g Q H}{P}$$

$P = \text{Shaft power}$

$$S_g H = \Delta P$$

$$\Rightarrow \boxed{P = \frac{Q \Delta P}{\eta_o}} \Rightarrow P = \frac{5.8333 \times 10^{-4} \times 100 \times 10^5}{0.87}$$

$$P = \text{shaft power} = 6704.98 \text{ watts}$$

$$P = 6.705 \text{ Kwatts.}$$

Question 3

Given: Nominal displacement of pump

$$= 50 \text{ cm}^3/\text{rev}$$

$$\text{Speed of rotation} = 850 \text{ rev/min}$$

(Q) theory = theoretical discharge

$$= \text{Nominal displacement} \times \text{Speed of rotation}$$

$$= 50 \times 850$$

$$= 42500 \text{ cm}^3/\text{min} = 42.5 \text{ dm}^3/\text{min}$$

$$\text{Volumetric efficiency} = \frac{Q_{\text{act}}}{Q_{\text{th}}} = \frac{35 \text{ dm}^3/\text{min}}{42.5 \text{ dm}^3/\text{min}} \times 100$$

$$= 82.353\%$$

JOHN EDWIN AKPAN.

181ENG 061033

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Question 10

Solution.

Given:

Diff. of mercury level

Sp. gr. of mercury

Sp. gr. of sea-water,

$$x = 170 \text{ mm} = 0.17 \text{ m}$$

$$S_g = 13.6$$

$$S_o = 1.026$$

$$h = x \left[ \frac{S_g}{S_o} - 1 \right] = 0.17 \left[ \frac{13.6}{1.026} - 1 \right] = 2.0834 \text{ m}$$

$$V = \sqrt{2gh} = \sqrt{2 \times 9.81 \times 2.0834} = 6.393 \text{ m/s}$$

$$= \frac{6.393 \times 60 \times 60}{1000} \text{ km/hr} = 23.01 \text{ km/hr} //$$