

NAME: Tunde - Adetula Simisola

MATRIC NUMBER: 18/ENG/081002

DEPARTMENT: BIOMEDICAL ENGINEERING

COURSE: FLUID MECHANICS (ENG 214)

DATE: MAY, 2020

i) Actual flow rate =  $10 \text{ dm}^3/\text{min} = 1.667 \text{ m}^3/\text{s} = 1.667 \times 10^{-4} \text{ m}^3/\text{s}$

Pressure change =  $12 \text{ bar} = 12 \times 10^5 \text{ N/m}^2$

Speed rotation =  $1500 \text{ rev/min} = 25.05 \text{ rev/sec}$

Nominal displacement =  $10 \text{ cm}^3/\text{rev} = 1 \times 10^{-5} \text{ m}^3/\text{rev}$

Torque input =  $12.5 \text{ Nm}$

ii) Volumetric Efficiency =  $\frac{\text{Actual flow rate}}{\text{Ideal flow rate}} \times 100\%$

Ideal flow rate = Nominal displacement  $\times$  speed rotation

=  $1 \times 10^{-5} \times 25.05$

=  $2.505 \times 10^{-4} \text{ m}^3/\text{s}$

Volumetric Efficiency =  $\frac{1.667 \times 10^{-4}}{2.505 \times 10^{-4}} \times 100$

=  $0.665 \times 100$

=  $66.5\%$

iii) Fluid power = Actual flow rate  $\times$  pressure change

=  $1.667 \times 10^{-4} \times 12 \times 10^5$

=  $200.04 \text{ Nm/sec}$

iv) Shaft power = Torque input  $\times$  Angular speed

Angular speed =  $2\pi \times$  speed of rotation

=  $2\pi \times 25.05$

=  $157.39 \text{ rev/sec}$

Shaft power =  $12.5 \times 157.39$

=  $1967.42 \text{ Nm/sec}$

$$\text{Overall Efficiency} = \frac{\text{Fluid power}}{\text{Shaft power}} \times 100\%$$

$$= \frac{200.04}{1967.42} \times 100$$

$$\approx 10.1676\%$$

$$\approx 10.2\%$$

2) Flow rate =  $35 \text{ dm}^3/\text{min} = 5.8345 \times 10^{-4} \text{ m}^3/\text{sec}$

Pressure change =  $100 \text{ bar} = 100 \times 10^5 \text{ N/m}^2$

Overall efficiency =  $87\%$

Shaft power = ?

$$\text{Fluid power} = 5.8345 \times 10^{-4} \times 100 \times 10^5$$

$$= 5834.5 \text{ W}$$

$$\text{Overall Efficiency} = \frac{\text{Fluid power}}{\text{Shaft power}} \times 100$$

$$87 = \frac{5834.5 \times 100}{\text{Shaft power}}$$

$$87 \times \text{Shaft power} = 5834.5 \times 100$$

$$\text{Shaft power} = \frac{5834.5 \times 100}{87}$$

$$= 6706.32 \text{ W}$$

$$= 6.70632 \text{ kW}$$

$\text{Nominal Displacement} = 50 \text{ cm}^3/\text{rev} = 5 \times 10^{-5} \text{ m}^3/\text{rev}$   
 $\text{Pressure change} = 100 \text{ bar} = 100 \times 10^5 \text{ N/m}^2$   
 $\text{Shaft power} = 15 \text{ kW} = 15,000 \text{ W}$   
 $\text{Actual flow rate} = 35 \text{ dm}^3/\text{min} = 5.8345 \times 10^{-4} \text{ m}^3/\text{sec}$   
 $\text{Speed of rotation} = 850 \text{ rpm} = 14.195 \text{ rev/sec}$

$\text{Overall Efficiency} = \frac{\text{Fluid power}}{\text{Shaft power}} \times 100$

$\text{Fluid power} = 5.8345 \times 10^{-4} \times 100 \times 10^5$   
 $= 5834.5 \text{ W}$

$\text{Overall Efficiency} = \frac{5834.5}{15000} \times 100$

$= 0.38897 \times 100$

$= 38.897\%$

$\approx 38.9\%$

$\text{Volumetric Efficiency} = \frac{\text{Actual flow rate}}{\text{Ideal flow rate}} \times 100$

$\text{Ideal flow rate} = \text{Nominal displacement} \times \text{speed of rotation}$

$= 5 \times 10^{-5} \times 14.195$

$= 7.0975 \times 10^{-4} \text{ m}^3/\text{sec}$

$\text{Volumetric Efficiency} = \frac{5.8345 \times 10^{-4}}{7.0975 \times 10^{-4}} \times 100$

$= 0.822 \times 100$

$= 82.2\%$

$\text{Water level (Z)} = 24,000 \text{ cm} = 240 \text{ m}$

$\text{Volumetric flow rate} = 13 \text{ liters/sec} = 13 \times 10^{-3} \text{ m}^3/\text{sec}$

$\text{Velocity of jet} = 66 \text{ m/sec}$

The jet issuing from the nozzle will be at atm pressure and at datum (e)

$P_2 = 0, z_2 = 0$

$\text{Density of water} = 1000 \text{ kg/m}^3$

$\text{Nominal Displacement} = 50 \text{ cm}^3/\text{rev} = 5 \times 10^{-5} \text{ m}^3/\text{rev}$   
 $\text{Pressure change} = 100 \text{ bar} = 100 \times 10^5 \text{ N/m}^2$   
 $\text{Shaft power} = 15 \text{ kW} = 15,000 \text{ W}$   
 $\text{Actual flow rate} = 35 \text{ dm}^3/\text{min} = 5.8345 \times 10^{-4} \text{ m}^3/\text{sec}$   
 $\text{Speed of rotation} = 850 \text{ rpm} = 14.195 \text{ rev/sec}$

$\text{Overall Efficiency} = \frac{\text{Fluid power}}{\text{Shaft power}} \times 100$   
 $\text{Fluid power} = 5.8345 \times 10^{-4} \times 100 \times 10^5 = 5834.5 \text{ W}$   
 $\text{Overall Efficiency} = \frac{5834.5}{15000} \times 100 = 38.897\% \approx 38.9\%$

$\text{Volumetric Efficiency} = \frac{\text{Actual flow rate}}{\text{Ideal flow rate}} \times 100$   
 $\text{Ideal flow rate} = \text{Nominal displacement} \times \text{speed of rotation}$   
 $= 5 \times 10^{-5} \times 14.195 = 7.0975 \times 10^{-4} \text{ m}^3/\text{sec}$   
 $\text{Volumetric Efficiency} = \frac{5.8345 \times 10^{-4}}{7.0975 \times 10^{-4}} \times 100 = 82.2\%$

$\text{Water level (z)} = 24,000 \text{ cm} = 240 \text{ m}$   
 $\text{Volumetric flow rate} = 13 \text{ liters/sec} = 13 \times 10^{-3} \text{ m}^3/\text{sec}$   
 $\text{Velocity of jet} = 66 \text{ m/sec}$   
 The jet issuing from the nozzle will be at atm pressure and at datum level,  
 $P_2 = 0, z_2 = 0$   
 $\text{Density of water} = 1000 \text{ kg/m}^3$

ii) Power at Jet

$$P = P_1 Q + \frac{\rho \cdot Q V^2}{2} + \rho g Q z$$

Introducing  $P=0$  and  $z=0$  in the equation above;

$$P = 0 \cdot Q + \frac{\rho \cdot Q V^2}{2} + \rho g Q (0)$$

$$P = \frac{\rho Q \cdot V^2}{2}$$

$$= \frac{1000 \times 13 \times 10^{-3} \times (66)^2}{2}$$

$$P = 5662.8$$

$$P = 2831.4 \text{ kW}$$

$$P = 28.314 \text{ MW}$$

$$P = 2831.4 \text{ W} \quad P = 28314 \text{ W}$$

$$P = 28.314 \text{ kW} \quad P = 28.314 \text{ kW}$$

iii) Power supplied from reservoir.

The reservoir operates at atm pressure,  $P=0$ , and  $v=0$ .

$$P = P_1 Q + \frac{\rho \cdot Q V^2}{2} + \rho g Q z$$

Introducing  $P=0$  and  $v=0$  into the above equation.

$$P = 0 \cdot Q + \frac{\rho \cdot Q (0)^2}{2} + \rho g Q z$$

$$P = \rho g Q z$$

$$= 1000 \times 9.81 \times 13 \times 10^{-3} \times 240$$

$$P = 30607.2 \text{ W}$$

$$P = 30.6072 \text{ kW}$$

iv) Head used to overcome losses.

Power loss = Head loss =  $\frac{\text{Power lost in transmission}}{\rho g Q}$

$$\rho g Q$$

$$\begin{aligned} \text{Power lost in transmission} &= \text{Power of reservoir} - \text{Power of jet} \\ &= 30607.2 - 28314 \\ &= 2293.2 \text{ W} \end{aligned}$$

$$\text{Head loss} = \frac{2293.2}{1000 \times 9.81 \times 13 \times 10^{-3}}$$

$$h = \frac{2293.2}{127.53}$$

$$h = 17.98 \text{ m}$$

iv) efficiency of pipe and nozzle in transmitting operation -

$$\begin{aligned} \text{Efficiency} &= \frac{\text{Power of jet}}{\text{Power of reservoir}} \\ &= \frac{28314}{30607.2} \\ &= 0.925 \times 100 \\ &= 92.5\% \end{aligned}$$

5)  $Z = 30,000 \text{ cm} = 300 \text{ m}$

$Q = 220 \text{ litres/sec} = 220 \times 10^{-3} \text{ m}^3/\text{sec}$

$V = 7 \text{ m/sec}$

$S.G = 0.89$

$\rho = 0.89 \times 1000 = 890 \text{ kg/m}^3$

① Power of jet:

$$P = P_a + \frac{\rho \cdot Q \cdot V^2}{2} + \rho g Q z$$

$P = 0, z = 0$

$$P = 0 + \frac{\rho \cdot Q \cdot V^2}{2} + \rho g Q (0)$$

$$P = \frac{\rho \cdot Q \cdot V^2}{2}$$

$$= \frac{890 \times 220 \times 10^{-3} \times (7)^2}{2}$$

$$P = \frac{9594.2}{2}$$

$P = 4797.1$

$$P = 4797.1 \text{ N}$$

$$P = 4.7971 \text{ kN}$$

ii) Power supplied from reservoir

Reservoir operates at atm pressure;  $P_2 = 0, V_2 = 0$

$$P = \rho Q \left[ \frac{v^2}{2} + g z \right]$$

$$P = \rho Q \left[ \frac{v^2}{2} + g z \right]$$

$$P = \rho Q g z$$

$$P = 890 \times 9.81 \times 220 \times 10^{-3} \times 30$$

$$P = 576239.4 \text{ N}$$

$$P = 576.2 \text{ kN}$$

$$P = 576.2394 \text{ kN}$$

iii) Head used to overcome losses

Head loss =  $\frac{\text{Power lost in transmission}}{\rho g Q}$

$$\rho g Q$$

$$\text{Power lost in transmission} = \text{Power of reservoir} - \text{power of jet} = 576239.4 - 4797.1$$

$$\text{Head loss} = \frac{571442.3}{890 \times 9.81 \times 220 \times 10^{-3}} = \frac{571442.3}{1920.198} = 297.50 \text{ m}$$

iv) Efficiency of the pipe and nozzle in transmitting operation

$$\text{Efficiency} = \frac{\text{Power of jet}}{\text{Power of reservoir}} \times 100$$

$$= \frac{4797.1}{576239.4} \times 100$$

$$= 8.32 \times 10^{-3} \times 100$$

$$= 0.832\%$$

$$\begin{aligned}
 6) \quad h &= 20 \text{ m} \\
 d &= 10 \text{ cm} = 0.1 \text{ m} \\
 r &= 5 \text{ cm} = 0.05 \text{ m} \\
 g &= 9.8 \text{ ms}^{-2}
 \end{aligned}$$

Using conservation of energy,

$$\frac{1}{2} mv^2 = mgh$$

$$v^2 = 2mgh = 2gh$$

$$v^2 = 2 \times 9.81 \times 20$$

$$v^2 = 392.4 \text{ m/s}^2$$

$$v = 19.8 \text{ m/s}$$

Flow rate at the base

$$\pi r^2 v = \pi \times (0.05)^2 \times 19.8$$

$$= 0.1555 \text{ m}^3/\text{s}$$

To find the amount of water that emerges from the fountain each

$$\frac{m}{t} = \rho \pi r^2 v$$

$$\frac{m}{1} = 1000 \times \pi \times (0.05)^2 \times 19.8$$

$$m = 155.5088 \text{ kg}$$

$$P = \frac{W}{t} = mg \frac{h}{t}$$

$$= (\rho \pi r^2 v) g \frac{h}{t}$$

$$= 155.5088 \times (9.8) \times \left( \frac{20}{1} \right)$$

$$P = 30797.72 \text{ W}$$

$$P = 30.79772 \text{ kW}$$

$$7) \quad \rho g = 19.62 \text{ N/m}^2$$

$$cd = 0.96$$

$$d_1 = 0.3 \text{ m}$$

$$d_2 = 0.2 \text{ m}$$

$$u_1 = \frac{Q}{0.0707}$$

$$u_2 = \frac{Q}{0.6314}$$

For the manometer;

$$p_1 + \rho_f g z = p_2 + \rho_f g (z_2 - R_p) + \rho_w g R_p$$

$$p_1 - p_2 = 19.62 (z_2 - z_1) + 587.423 \quad \text{--- (i)}$$

For the venturimeter;

$$\frac{p_1}{\rho_f g} + \frac{u_1^2}{2g} + z_1 = \frac{p_2}{\rho_f g} + \frac{u_2^2}{2g} + z_2$$

$$p_1 - p_2 = 19.62 (z_2 - z_1) + 0.803 u_2^2 \quad \text{--- (ii)}$$

Combining equation (i) and (ii)

$$0.803 u_2^2 = 587.423$$

$$u_{2, \text{ideal}} = 27.047 \text{ m/s}$$

$$Q_{\text{ideal}} = 27.047 \times \pi \left( \frac{0.2}{2} \right)^2 = 0.85 \text{ m}^3/\text{s}$$

$$Q = C_d Q_{\text{ideal}} = 0.96 \times 0.85$$

$$Q = 0.816 \text{ m}^3/\text{s}$$

$$d_1 = 0.152 \text{ m}$$

$$d_2 = 0.076 \text{ m}$$

$$\rho = 800 \text{ kg/m}^3$$

$$C_d = 0.97$$

$$A_1 = \frac{\pi d_1^2}{4} = \frac{\pi (0.152)^2}{4} = 0.0181 \text{ m}^2$$

$$A_2 = \frac{\pi d_2^2}{4} = \frac{\pi (0.076)^2}{4} = 4.5 \times 10^{-3} \text{ m}^2$$

Apply Bernoulli's equation;

$$\frac{p_1}{\rho g} + \frac{u_1^2}{2g} + z_1 = \frac{p_2}{\rho g} + \frac{u_2^2}{2g} + z_2$$

$$8) \textcircled{a} p_1 = p_2$$

$$\frac{u_1^2}{2g} + z_1 = \frac{u_2^2}{2g} + z_2$$

By continuity;  $Q = u_1 A_1 = u_2 A_2$

$$u_2 = u_1 \frac{A_1}{A_2} = u_1 \frac{0.0181}{4 \times 10^{-3}} = u_1 \cdot 4.025$$

$$\frac{u_1^2}{2g} + 0.914 = \frac{16.178 u_1^2}{2g}$$

$$0.914 = \frac{15.178 u_1^2}{2g}$$

$$2g \times 0.914 = 15.178 u_1^2$$

$$u_1^2 = \frac{2 \times 9.81 \times 0.914}{15.178}$$

$$u_1 = \sqrt{\frac{2 \times 9.81 \times 0.914}{15.178}}$$

$$u_1 = 1.08696 \text{ m/s}$$

$$Q = C_d A_1 u_1$$

$$Q = 0.96 \times 0.0181 \times 1.08696$$

$$= 0.018887 \text{ m}^3/\text{s}$$

$$8) \textcircled{b} p_1 - p_2 = 15170$$

$$\frac{p_1 - p_2}{\rho g} = \frac{u_2^2}{2g} - \frac{u_1^2}{2g} \quad \frac{p_1}{\rho g} + \frac{u_1^2}{2g} + z_1 = \frac{p_2}{\rho g} + \frac{u_2^2}{2g} + z_2$$

$$\frac{p_1 - p_2}{\rho g} = \frac{u_2^2 - u_1^2}{2g} = 0.914$$

$$8) \textcircled{a} p_1 = p_2$$

$$\frac{u_1^2}{2g} + z_1 = \frac{u_2^2}{2g} + z_2$$

By continuity;  $Q = u_1 A_1 = u_2 A_2$

$$u_2 = u_1 \frac{A_1}{A_2} = u_1 \frac{0.0181}{4 \times 10^{-3}} = u_1 \cdot 4.02$$

$$\frac{u_1^2}{2g} + 0.914 = \frac{16.178 u_1^2}{2g}$$

$$0.914 = \frac{15.178 u_1^2}{2g}$$

$$2g \times 0.914 = 15.178 u_1^2$$

$$u_1^2 = \frac{2 \times 9.81 \times 0.914}{15.178}$$

$$u_1 = \sqrt{\frac{2 \times 9.81 \times 0.914}{15.178}}$$

$$u_1 = 1.08696 \text{ m/s}$$

$$Q = Cd \cdot u_1$$

$$Q = 0.96 \times 0.0181 \times 1.08696$$

$$= 0.018887 \text{ m}^3/\text{s}$$

$$p_1 = p_2 = 15170$$

$$\frac{p_1}{\rho g} + \frac{u_1^2}{2g} + z_1 = \frac{p_2}{\rho g} + \frac{u_2^2}{2g} + z_2$$

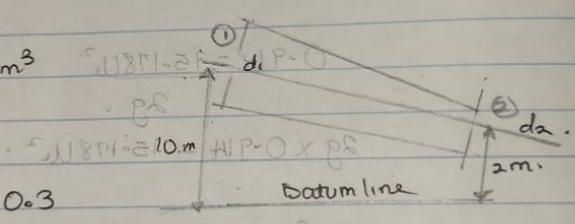
$$\frac{p_1}{\rho g} - \frac{p_2}{\rho g} = \frac{u_2^2}{2g} - \frac{u_1^2}{2g} = 0.914$$

$$\frac{15170}{\rho g} = \frac{Q^2}{2g} \left( \frac{220.43^2}{d^5} - \frac{55.11^2}{d^5} \right) - 0.914$$

$$\frac{15170}{\rho g} = \frac{Q^2}{2g} (220.43^2 - 55.11^2) - 0.914$$

$$Q = 0.035 \text{ m}^3/\text{s}$$

1000 litre = 1 m<sup>3</sup>  
At section 1



$d_1 = 300 \text{ mm} = 0.3 \text{ m}$

$$A_1 = \frac{\pi d_1^2}{4} = \frac{\pi (0.3)^2}{4} = 0.0707 \text{ m}^2$$

$z_1 = 10 \text{ m}$

$v_1 = ?$

$\rho = 1000 \times 10^3 \text{ N/m}^2 \cdot \text{m}^2 \cdot \text{s}^2 = 10^6 \text{ N/m}^2$

At Section 2

$$d_2 = 150 \text{ mm} = 0.15 \text{ m}$$

$$A_2 = \frac{\pi d_2^2}{4} = \frac{\pi (0.15)^2}{4} = 0.01767 \text{ m}^2$$

$z_2 = 2 \text{ m}$

$v_2 = ?$

$\rho_2 = ?$

$A_1 v_1 = A_2 v_2$

$A_1 v_1 = 10 \text{ l/sec} = 10 \times 10^{-3} \text{ m}^3/\text{sec}$

$$\therefore v_1 = \frac{10 \times 10^{-3}}{0.0707}$$

$$V_1 = 0.566 \text{ m/s}$$

$$V_2 = \frac{40 \times 10^{-3}}{0.01767} = 2.264 \text{ m/s}$$

Applying Bernoulli's equation;

$$\frac{P_1}{\rho} + \frac{V_1^2}{2g} + z_1 = \frac{P_2}{\rho} + \frac{V_2^2}{2g} + z_2$$

$$\frac{400 \times 10^3}{9800} + \frac{(0.566)^2}{2 \times 9.8} + 10 = \frac{P_2}{\rho} + \frac{(2.264)^2}{2 \times 9.8} + 6$$

$$40.816 + 0.016 + 10 = \frac{P_2}{\rho} + 0.26 + 6$$

$$50.832 = \frac{P_2}{\rho} + 6.26$$

$$\frac{P_2}{\rho} = 44.572$$

$$P_2 = 44.572 \times 9800$$

$$P_2 = 436805.6 \text{ N/m}^2$$

$$P_2 = 436.8056 \text{ kN/m}^2$$

$$108 \cdot r = 170 \text{ mm} = 0.17 \text{ m}$$

$$S_m = 13.6$$

$$S = 1.025$$

$$C = 1$$

$$V = ?$$

$$V = C \sqrt{2g r \left( \frac{S_m}{S} - 1 \right)}$$

$$V = 1 \sqrt{2 \times 9.81 \times 0.17 \left( \frac{13.6}{1.025} - 1 \right)}$$

$$V = 3.354 (13.268 - 1)$$

$$V = \sqrt{3.3354 \times 12.268}$$

$$V = \sqrt{40.91966} \text{ m/s} =$$

$$V = 6.4 \text{ m/s}$$

$$v^2 + \frac{p}{\rho} + z =$$

$$(0.999)^2 + \frac{p}{\rho} + z = 0 + \frac{p}{\rho} + z$$

$$0.998 + \frac{p}{\rho} + z = 0 + \frac{p}{\rho} + z$$

$$0.998 + \frac{p}{\rho} = 0 + \frac{p}{\rho}$$

Н.В.Д.

0.999 x 0.999 = 0.998

$\rho = 1000 \text{ kg/m}^3$

$\rho = 1000 \text{ kg/m}^3$

0.12m

$$\left( \frac{1}{2} \rho v^2 \right) + \rho g z$$