

1. Pipe flow  
 2. Continuity  
 3. Bernoulli



$z_1 = 2m, P_1 = 2.5 \text{ bar}, v_1 = 5 \text{ m/s}, z_2 = 2 \text{ m}$

h<sub>L</sub> = loss of head (Energy loss)  
 $= 0.35 \frac{(v_1 - v_2)^2}{2g}$   
 $= \frac{0.35(5-2)^2}{2 \times 9.81} = 0.1606 \text{ m}$

According to conservation of energy

$P_1 + z_1 + \frac{v_1^2}{2g} = P_2 + z_2 + \frac{v_2^2}{2g} + h_L$

$2.5 \text{ bar} + 2 \text{ m} + \frac{25}{2 \times 9.81} \text{ m} = \frac{P_2}{9.81} + 0 + \frac{4}{2 \times 9.81} + 0.1606 \text{ m}$

$= 5.774 \text{ m} - 0.1606 \text{ m} - 0.2039 \text{ m}$

$\frac{P_2}{9.81} = 5.4095 \text{ m}$   
 Pressure head at base

$d_1 = 20 \text{ cm}$ , throat diameter = 10 cm  
 Pressure at throat = 0.5 bar

$Q = C_d = 0.98$

$= C_d A_1 A_2 \sqrt{\frac{2g h}{A_1^2 - A_2^2}}$

$M_1 = \pi d_1^2 \times \frac{v_1}{4} = \pi (0.05)^2 \times 0.001 \times 1 \text{ m}^3$   
 $M_2 = \pi d_2^2 \times \frac{v_2}{4} = \pi (0.1)^2 \times 7.107 \text{ m}^3$

$h = \frac{P}{\rho g} - \frac{v^2}{2g}$

$P_1 = 30 \text{ m} \times 1000 \times 9.81$   
 $P_2 = 24.8 \text{ m} \times 1000 \times 9.81$

$P = \frac{17.658 \text{ N}}{(100)^2 \times 1000 \times 9.81} \text{ m}$   
 $= 1.8 \times 10^{-7} \text{ m}$

$h = (1.8 \times 10^{-7} - 0.3) \text{ m}$   
 $h = -0.30 \text{ m}$

$Q = 0.98 \times 0.0314 \times 7.107 \times 10^{-3}$   
 $= \sqrt{2 \times 9.81 \times 0.3}$

$0.0314^2 - (7.107 \times 10^{-3})^2$

$Q = 0.0198 \text{ m}^3/\text{s}$

$d_0 = 15 \text{ cm} = 0.15 \text{ m}$

$Q = C_d A_0 \sqrt{2gh}$

$\sqrt{A_1^2 - A_2^2}$   
 $A_1^2$

$$N = \frac{2\pi N}{60} = \frac{2\pi \times 1000}{60} = 0.1047 \text{ rad/s}$$

$$A_1 = \frac{\pi d_1^2}{4} = \frac{\pi \times (0.07)^2}{4} = 0.003847 \text{ m}^2$$

$$h = \frac{2\gamma}{\rho g} \left( \frac{S_{hg}}{S_u} - 1 \right)$$

$$h = \frac{100}{1000} \left( \frac{13.6}{0.9} - 1 \right)$$

$$h = 7.056 \text{ m}$$

$$Q = 0.64 \times 0.0177 \times \sqrt{2 \times 9.81 \times 7.056}$$

$$Q = \frac{\sqrt{(0.0707)^2 - (0.0177)^2}}{(0.0707)}$$

$$Q = 0.1377 \text{ m}^3/\text{s}$$

$$V = \sqrt{2gh}$$

$$\Delta h = y \left( \frac{S_{hg}}{S_L} - 1 \right)$$

$$e_{hg} = 13.600 \therefore S_{hg} = 13.6$$

$$e_L = 1000 \therefore S_L = 1$$

$$\Delta h = \frac{170}{1000} \left( \frac{13.6}{1} - 1 \right)$$

$$\Delta h = 2.142 \text{ m}$$

$$V = \sqrt{2 \times 9.81 \times 2.142}$$

$$V = 6.488 \text{ m/s}$$

$$Q = 0.05 \text{ m}^3/\text{min} \quad P = 15 \text{ bar}$$

$$N = 1700 \text{ rev/min} = 28.3 \text{ rev/sec}$$

$$\text{vol displacement} = 10 \text{ cm}^3/\text{rev}$$

$$T = 15 \text{ Nm}$$

Fluid Power = Force x Speed

Power = Force x Speed

Force = Force exerted on the fluid

Force x Area x Speed

$$= 15 \times 10^3 \times 0.05 \text{ m}^2/\text{s}$$

$$= 1250 \text{ W}$$

① Shaft power

Force x Speed

The shaft rotates

Force x r x  $\omega$

Torque x  $\omega$

Shaft power

$$= 15 \text{ Nm} \times 28.3 \text{ rev/s}$$

$$= 424.5 \text{ W}$$

② Volumetric Efficiency

$$\eta_v = \frac{Q}{Q_{\text{theor}}} = \frac{0.05}{0.05 + (28.3 \times 10^{-6})}$$

$$\eta_v = 28.3 \times 10^{-6} \text{ m}^3/\text{s}$$

$$\eta_v = 0.994$$

③ Overall efficiency

$$\eta_o = \frac{\text{Shaft power}}{\text{Fluid power}} \times 100\%$$

$$= \frac{424.5}{1250} \times 100\%$$

$$= 33.96\%$$