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 B/ENG04/002
 Mechanical

ENG 214

1 Real flow rate = $10 \text{ dm}^3/\text{min}$, $T = 125 \text{ mm}$
 $= \frac{10 \times 10^{-3}}{60} = 1.67 \times 10^{-4} \text{ m}^3/\text{s}$

Pressure = 12 bar = $12 \times 10^5 \text{ N/m}^2$

Speed = $1500 \text{ rev/min} = 25 \text{ rev/sec}$

Nominal displacement = $10 \text{ cm}^3/\text{rev} = 1 \times 10^{-5} \text{ m}^3/\text{rev}$

Ideal flow rate = $2.5 \times 10^{-4} \text{ m}^3/\text{sec}$

i) Volumetric efficiency = $\frac{\text{Real flow rate} \times 100}{\text{Ideal flow rate}}$
 $= \frac{1.67 \times 10^{-4} \times 100}{2.5 \times 10^{-4}} = 66.8\%$

ii) Fluid power = $(Q \times \Delta P)$
 $= 1.67 \times 10^{-4} \times 12 \times 10^5 = 200.4 \text{ Watts}$

iii) Shaft power = $T \times \omega$

$\omega = 2\pi N = 2 \times \pi \times 25$
 $= 157.08$

\therefore Shaft power = 12.5×157.08
 $= 1963.51 \text{ Watts}$

iv) Overall efficiency = $\frac{\text{Fluid power} \times 100}{\text{Shaft power}}$
 $= \frac{200.4 \times 100}{1963.5} = 10.206$
 $\approx 10.21\%$

2 Pump Delivery = $35 \text{ dm}^3/\text{min}$
 $= \frac{35 \times 10^{-3}}{60} = 5.83 \times 10^{-4}$

$P = 100 \text{ bar} = 100 \times 10^5 \text{ N/m}^2$

Overall efficiency = 87%

Fluid Power = $(Q \times \Delta P)$

$= 5.83 \times 10^{-4} \times 100 \times 10^5$
 $= 5830 \text{ Watts}$

i) Overall efficiency = $\frac{\text{Fluid power} \times 100}{\text{Shaft power}}$

\therefore Shaft power = $\frac{\text{Fluid power} \times 100}{\text{Overall efficiency}}$

Shaft power = $\frac{5830 \times 100}{87}$

$= 6701.1491 \text{ Watts}$

3) Nominal displacement $50 \text{ cm}^3/\text{rev} = 50 \times 10^{-6} \text{ m}^3/\text{rev}$

Pressure = 100 bar = $100 \times 10^5 \text{ N/m}^2$
 Shaft power = 15 kW = 15000 Watts

* Actual flow rate = $35 \text{ dm}^3/\text{min}$
 $= \frac{35 \times 10^{-3}}{60} \text{ m}^3 = 5.83 \times 10^{-4} \text{ m}^3/\text{s}$

Speed = $850 \text{ rev/min} = \frac{850}{60}$

$= 14.17 \text{ rev/sec}$
 Ideal flow rate = $\text{Nominal displacement} \times \text{speed}$

$= 30 \times 10^{-6} \text{ m}^3/\text{rev} \times 14.17 \text{ rev/sec}$
 $= 7.085 \times 10^{-4} \text{ m}^3/\text{sec}$

i) Volumetric efficiency = $\frac{\text{Real flow rate} \times 100}{\text{Ideal flow rate}}$

$= \frac{5.83 \times 10^{-4} \times 100}{7.085 \times 10^{-4}}$
 $= 82.29\%$

Fluid power = $(Q \times \Delta P)$

$= 5.83 \times 10^{-4} \times 100 \times 10^5$
 $= 5830 \text{ Watts}$

$$\text{Overall Efficiency} = \frac{\text{Fluid power} \times 100}{\text{Shaft power}}$$

$$= \frac{5330}{15000} \times 100 = 38.87\%$$

$$\approx 38.9\%$$

4) $z = 2400 \text{ cm} = 24 \text{ m}$
 Volumetric flowrate; $Q = 13 \text{ litres/sec}$
 $= 0.013 \text{ m}^3/\text{sec}$

Velocity = 66 m/sec

$$P = \rho g Q \left(\frac{P}{\rho g} + \frac{V^2}{2g} + z \right)$$

$$P = QP + \frac{\rho Q V^2}{2} + \rho g Q z$$

Introducing for Jet power
 Pressure head = 0
 $z = 0$
 $\therefore P = \frac{\rho Q V^2}{2}$

$Q = 0.013$, $\rho = 1000$, $V = 66 \text{ m/s}$
 $\therefore P = \frac{1000 \times 0.013 \times 66^2}{2}$
 $P = 28314 \text{ Watts}$

Power supplied from reservoir at
 $P = 0$ & $V = 0$
 $\therefore P = \rho g Q z$
 $P = 1000 \times 9.81 \times 0.013 \times 240$
 $= 30607.2 \text{ Watts}$

Power loss in transmission
 $= \text{Power of reservoir} - \text{Power of Jet}$
 $= (30607.2 - 28314)$
 $= 312293.2 \text{ Watts}$

Head loss in pipeline
 $= 2293.2 \text{ Watts}$

iv) $h = \frac{\text{Power loss in transmission}}{\rho g Q}$
 $h = \frac{2293.2}{1000 \times 9.81 \times 0.013}$
 $h = \frac{2293.2}{127.53} = 17.98 \text{ m}$

v) Efficiency = $\frac{\text{Power of Jet} \times 100}{\text{Power of reservoir}}$
 $= \frac{28314}{30607.2} \times 100 = 92.51\%$

5) Specific gravity of oil = 0.89

$z = 30,000 \text{ cm} = 300 \text{ m}$

$Q = 220 \text{ l/sec} = 0.22 \text{ m}^3/\text{sec}$

$V = 7 \text{ m/sec}$

Introducing, $z = 0$, Pressure = 0

i) $P = \frac{\rho Q V^2}{2}$ (Jet power)

$S_g = 0.89$

$S_g = \frac{\rho}{1000}$

$\therefore \rho = 0.89 \times 1000 = 890$

$\rho = \rho = 890$

$P = \frac{890 \times 0.22 \times 7^2}{2}$

$= 4797.1 \text{ Watts}$

ii) Power supplied from reservoir

$P = \rho g Q z$

$P = 890 \times 9.81 \times 0.22 \times 300$

$P = 576239.4 \text{ Watts}$

iii. Power loss in transmission
 = Reservoir power - Jet power
 = 576239.4 - 4797.1
 = 571442.3 Watts

Head used to overcome losses

= $\frac{\text{Power loss in transmission}}{\rho g Q}$
 = $\frac{571442.3}{890 \times 9.81 \times 0.22} = 297.51 \text{ m}$

iv. Efficiency = $\frac{\text{Jet power}}{\text{Reservoir power}} \times 100$
 = $\frac{4797.1}{576239.4} \times 100$

6. $P = \rho g Q z$ $Q = vA$
 $z = 20 \text{ m} = h$ $d = 10 \text{ cm} = 10 \times 10^{-2} \text{ m}$
 $\rho = 1000$

$g = 9.81$
 $A = \frac{\pi d^2}{4} = \frac{\pi (10 \times 10^{-2})^2}{4} = 7.85 \times 10^{-3} \text{ m}^2$

Applying eqn of motion,
 Velocity at height of initial velocity

$v = 0$
 $v^2 = u^2 - 2gh$
 $u = \sqrt{v^2 + 2gh}$
 $u = \sqrt{0^2 + 2 \times 9.81 \times 20}$
 $u = \sqrt{392.4}$
 $u = 19.809 \approx 19.81 \text{ m/s}$

$Q = vA$
 = $19.81 \times 7.85 \times 10^{-3}$
 = $0.15558 \text{ m}^3/\text{sec}$
 $\approx 0.156 \text{ m}^3/\text{sec}$

$P = \rho g Q z$
 = $1000 \times 9.81 \times 0.156 \times 20$
 $P = 30510.7671 \text{ Watts}$

7) $d_1 = 0.3 \text{ m}$
 $A_1 = \frac{\pi d_1^2}{4} = \frac{\pi (0.3)^2}{4} = 0.0707 \text{ m}^2$

$d_2 = 0.2 \text{ m}$
 $A_2 = \frac{\pi d_2^2}{4} = \frac{\pi (0.2)^2}{4} = 0.0314 \text{ m}^2$

$C_d = 0.96$

Specific weight of gas = 19.62 N/m^3

$\int = \frac{mg}{V} = \rho g$

= $\frac{19.62}{9.81} = \frac{\rho \times 9.81}{9.81}$

$\rho g = 19.62$

$\rho = 2 \text{ kg/m}^3$

$Q_1 = A_1 V_1$; $Q_2 = A_2 V_2$
 $V_1 = \frac{Q}{A_1}$; $V_2 = \frac{Q}{A_2}$

$V_1 = \frac{Q}{0.0707}$; $V_2 = \frac{Q}{0.0314}$

For manometer;

$P_1 + \rho g z_1 = P_2 + \rho g (z_2 - R_p) + \rho g R_p$
 $P_1 - P_2 = \rho g (z_2 - R_p) + \rho g R_p - \rho g z_1$
 $\therefore P_1 - P_2 = 19.62 (z_2 - z_1) + 587.423 \text{ @}$

For venturimeter;

$\frac{P_1}{\rho g} + \frac{V_1^2}{2g} + z_1 = \frac{P_2}{\rho g} + \frac{V_2^2}{2g} + z_2$
 $P_1 - P_2 = 19.62 (z_2 - z_1) + 0.803 V_2^2 - \text{@}$
 $z_2 - z_1 = 0.06 \text{ m}$

$$0.803 V_2^2 = 587.423$$

$$V_2^2 = \frac{587.423}{0.803}$$

$$V_2^2 = 731.533$$

$$V_2 = \sqrt{731.533}$$

$$V_2 = 27.0469$$

$$\approx 27.05 \text{ m/s}$$

$$\text{Ideal flow rate} = Q_{\text{ideal}} = A_2 V_2$$

$$= 27.047 \times 0.0314$$

$$= 0.85 \text{ m}^3/\text{s}$$

$$Q_{\text{real}} = C_d \times Q_{\text{ideal}}$$

$$= 0.96 \times 0.85$$

$$= 0.816 \text{ m}^3/\text{s}$$

3 Throat diameter = 0.076 m²

Vahol diameter = 0.152 m²

Relative density = 0.8

Throat berg = 0.914 m

$C_d = 0.91$

Bernoulli's eqn

$$\frac{P_1}{\rho_g} + \frac{V_1^2}{2g} + z_1 = \frac{P_2}{\rho_g} + \frac{V_2^2}{2g} + z_2$$

$$Q = V_1 A_1 = V_2 A_2$$

$$A_2 = \frac{\pi d^2}{4} = \frac{\pi \times 0.076^2}{4}$$

$$= 4.64 \times 10^{-3} \text{ m}^2$$

$$A_1 = \frac{\pi d^2}{4} = \frac{\pi \times 0.152^2}{4}$$

$$= 0.0181 \text{ m}^2$$

$$V_1 A_1 = V_2 A_2$$

$$V_1 = \frac{V_2 A_2}{A_1} = \frac{V_2 \times 4.64 \times 10^{-3}}{0.0181}$$

$$V_1 = 0.25 V_2$$

For $P_1 = P_2$, $f = 800$

$$\frac{P_1}{\rho_g} - \frac{P_2}{\rho_g} + \frac{V_1^2}{2g} + z_1 = \frac{V_2^2}{2g} + z_2$$

$$z_1 - z_2 + \frac{V_1^2}{2g} = \frac{V_2^2}{2g}, z_1 - z_2 = 0.914$$

$$0.914 + \frac{(0.25 V_2)^2}{2 \times 9.81} = \frac{V_2^2}{2 \times 9.81}$$

$$0.914 = \frac{V_2^2 - 0.25 V_2^2}{19.62}$$

$$V_2^2 - 0.063 V_2^2 = 17.93$$

$$0.937 V_2^2 = 17.93$$

$$V_2^2 = \frac{17.93}{0.937}$$

$$V_2^2 = 19.136$$

$$V_2 = \sqrt{19.136}$$

$$= 4.37 \text{ m/s}$$

$$Q_{\text{ideal}} = A_2 V_2 = 4.37 \times 4.64 \times 10^{-3}$$

$$= 0.02027$$

$$Q_{\text{real}} = C_d \times Q_{\text{ideal}}$$

$$= 0.96 \times 0.02027$$

$$= 0.0195 \text{ m}^3/\text{s}$$

ii) $P_1 - P_2 = 15170$

$$\left(\frac{P_1}{\rho_g} + z_1 \right) - \left(\frac{P_2}{\rho_g} + z_2 \right) = \frac{V_1^2}{2g} - \frac{V_2^2}{2g}$$

$$\frac{P_1 - P_2}{\rho_g} + (z_1 - z_2) = \frac{V_2^2}{2g} - \frac{V_1^2}{2g}$$

Recall, $z_1 - z_2 = 0.914$

$$\frac{P_1 - P_2}{\rho_g} = \frac{V_2^2}{2g} - \frac{V_1^2}{2g} - 0.914$$

Recall; $Q = VA$; $\frac{V}{A} = \frac{Q}{A}$

$$P = 800, g = 9.81$$

$$\frac{15170}{800 \times 9.81} = \left(\frac{Q}{A_2}\right)^2 - \left(\frac{Q}{A_1}\right)^2 - 0.914$$

$$\frac{15170}{7848} = Q^2 \left[\left(\frac{1}{A_2}\right)^2 - \left(\frac{1}{A_1}\right)^2 \right] - 0.914$$

$$1.932 = Q^2 \left(\frac{48516.36 - 3052.41}{2g} \right) - 0.914$$

$$(1.932 + 0.914)2g = Q^2 (48516.36 - 3052.41)$$

$$56.3678 = Q^2 45463.95$$

Divide through by 45463.95

$$Q^2 = 1.24 \times 10^{-3}$$

$$Q = \sqrt{1.24 \times 10^{-3}} = 0.0352 \text{ m}^3/\text{s}$$

9 $d_1 = 300 \text{ mm} = 0.3 \text{ m}$

$d_2 = 150 \text{ mm} = 0.15 \text{ m}$

$$\therefore A_1 = 0.07069 \text{ m}^2 = \frac{\pi \times 0.3^2}{4}$$

$$A_2 = 0.0177 \text{ m}^2 = \frac{\pi \times 0.15^2}{4}$$

$Q = 40 \text{ litres/sec} = 0.04 \text{ m}^3/\text{sec}$

$z_1 = 10 \text{ m}; z_2 = 6 \text{ m}$

$P_1 = 480 \text{ kN/m}^2, P_2 = ?$

$$\frac{P_1}{\rho g} + z_1 + \frac{V_1^2}{2g} = \frac{P_2}{\rho g} + z_2 + \frac{V_2^2}{2g}$$

But, $Q = A_1 V_1$

$$V_1 = \frac{Q}{A_1} = \frac{0.04}{0.07069} = 0.5658 \text{ m/s}$$

$$A_1 = 0.07069$$

$$\approx 0.57 \text{ m/s}$$

$$V_2 = \frac{Q}{A_2} = \frac{0.04}{0.0177} = 2.26 \text{ m/s}$$

$$A_2 = 0.0177$$

$$\frac{P_1}{\rho g} + (z_1 - z_2) + \left(\frac{V_1^2}{2g} - \frac{V_2^2}{2g} \right) = \frac{P_2}{\rho g}$$

$$\frac{480 \text{ kN}}{9.81 \text{ kN}} + (10 - 6) + \left(\frac{0.57^2}{2 \times 9.81} - \frac{2.26^2}{2 \times 9.81} \right) = \frac{P_2}{9.81 \text{ kN}}$$

$$= \frac{P_2}{9.81 \text{ kN}}$$

$$= 40.77 + 4 + (-0.2438) = \frac{P_2}{9.81 \text{ kN}}$$

$$44.52 \times 9.81 = P_2$$

$$\therefore P_2 = 436.74 \text{ kN}$$

10) Reading of manometer = 170 mm = 0.17 m

S_g of Hg = 13.6

S_g of sea water = 1.026

$$h = 0.17 \left(\frac{13.6}{1.026} - 1 \right)$$

$$h = 2.083 \text{ m}$$

$$V = \sqrt{2gh}$$

$$V = \sqrt{2 \times 9.81 \times 2.083} = 6.39 \text{ m/s}$$