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DEPT: MECHATRONICS

COURSE CODE: ENG 214

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18/ENG05/003  
MECHATRONICS ENGINEERING  
ASSIGNMENT

(1) length  $l = 2.0\text{m}$   
The velocity flow at smaller end ( $V_1$ ) = 5m/s  
The velocity flow at lower end ( $V_2$ ) = 2m/s  
Let the pressure head at the smaller end ( $P_s$ ) = 2.5m of liquid  
Loss of head ( $H_L$ ) =  $\frac{0.35(V_1 - V_2)^2}{2g} = \frac{0.35(5-2)^2}{2 \times 9.81} = 0.161\text{m}$   
Let the pressure head at lower end ( $P_L$ ) = ?

Applying Bernoulli's equation  
 $\frac{P_1}{\rho g} + \frac{V_1^2}{2g} + z_1 = \frac{P_2}{\rho g} + \frac{V_2^2}{2g} + z_2 + H$   
where  $P_s = \frac{P_1}{\rho g}$  and  $P_L = \frac{P_2}{\rho g}$

$z_1 = 2.0$  and  $z_2 = 0$  (datum line passes through section 2)  
Inputting values into the equation  
 $2.5 + \frac{5^2}{2 \times 9.81} + 2.0 = P_L + \frac{2^2}{2 \times 9.81} + 0 + 0.161$

$2.5 + \frac{25}{19.62} + 2 = P_L + \frac{4}{19.62} + 0.161$

$2.5 + \frac{25}{19.62} + 2 - \left(\frac{4}{19.62} + 0.161\right) = P_L$

$5.774 - 0.365 = P_L$   
 $P_L = 5.409\text{m}$  of fluid

(2) Let inlet diameter ( $D_1$ ) = 20cm  
Let throat diameter ( $D_2$ ) = 10cm  
inlet area ( $A_1$ ) =  $\frac{\pi D_1^2}{4} = \frac{\pi (20)^2}{4} = 314.16\text{cm}^2$

$$\text{throat area } (A_2) = \frac{\pi D_2^2}{4} = \frac{\pi (10)^2}{4} = 78.54 \text{ cm}^2$$

$$\text{Density of water, } \rho = 1000 \text{ kg/m}^3$$

$$\text{Pressure at inlet} = 17.658 \text{ N/cm}^2 = 17.658 \text{ N/m}^2$$

$$\therefore \frac{P_1}{\rho g} = \frac{17.658 \times 10^4}{1000 \times 9.81} = 18 \text{ m}$$

$$\frac{P_2}{\rho g} = -30 \text{ cm of mercury}$$

$$\text{Specific gravity} = 13.6$$

$$\frac{P_2}{\rho g} = -30 \times 10^{-2} \text{ m of mercury} \times 13.6$$
$$= -4.08 \text{ m}$$

$$\text{Let Differential Head} = H = \frac{P_1}{\rho g} - \frac{P_2}{\rho g}$$

$$= 18 - (-4.08)$$

$$= 18 + 4.08 = 22.08 \text{ m} \times 100$$

$$H = 2208 \text{ cm}$$

$$\text{Using } Q = \frac{C_d \sqrt{2gh} \cdot A_1 A_2}{\sqrt{A_1^2 - A_2^2}} = \frac{0.98 \times \sqrt{2 \times 9.81 \times 2208} \times 314.16 \times 78.54}{\sqrt{(314.16)^2 - (78.54)^2}}$$

$$= \frac{0.98 \times 2081.37 \times 24674.1204}{304.184112} = 165455.3 \text{ cm}^3/\text{s}$$

$$= \frac{165455.3}{1000} = 165.455 \text{ lit/sec}$$

3) Diameter of pipe  $d_1 = 30 \text{ cm}$

$$A_1 = \frac{\pi d_1^2}{4} = \frac{\pi (30)^2}{4} = 706.86 \text{ cm}^2$$

Diameter of orifice  $d_2 = 15 \text{ cm}$

$$A_2 = \frac{\pi d_2^2}{4} = \frac{\pi (15)^2}{4} = 176.72 \text{ cm}^2$$

Specific gravity of oil,  $S_o = 0.9$

» » » mercury,  $S_{hg} = 13.6$

Differential manometer reading,  $x = 50 \text{ cm}$  of mercury

Coefficient of discharge,  $C_d = 0.64$

$$\text{Differential head, } h = x \left( \frac{\rho_{\text{Hg}}}{\rho_0} - 1 \right) = 50 \left( \frac{13.6}{0.9} - 1 \right)$$

$$h = 705.56 \text{ cm of oil}$$

∴ The rate of flow of oil is

$$Q = C_d \frac{\sqrt{2gh} \cdot A_1 A_2}{\sqrt{A_1^2 - A_2^2}}$$

$$Q = 0.64 \times \frac{\sqrt{2 \times 9.81 \times 705.56} \times 706.86 \times 176.72}{\sqrt{(706.86)^2 - (176.72)^2}}$$

$$Q = 137443.29 \text{ cm}^3/\text{s}$$

$$Q = \frac{137443.29}{1000} = 137.44 \text{ lit/s}$$

4) Diff of mercury level ( $x$ ) = 170 mm = 0.17 m

Specific gravity of mercury ( $\rho_{\text{Hg}}$ ) = 13.6

„ „ „ sea water ( $\rho_0$ ) = 1.026

Speed  $V = ?$

$$V = \sqrt{2gh} \quad , h = ?$$

$$h = x \left[ \frac{\rho_{\text{Hg}}}{\rho_0} - 1 \right] = 0.17 \left[ \frac{13.6}{1.026} - 1 \right] = 2.0834 \text{ m}$$

$$\therefore V = \sqrt{2 \times 9.81 \times 2.0834} = 6.393 \text{ m/s}$$

In km/hr

$$V = \frac{6.393 \times 60^2}{1000} = 23.01 \text{ km/hr}$$

5)  $Q = 0.05 \text{ m}^3/\text{min} = 50 \text{ dm}^3/\text{min}$

$$P_0 = 15 \text{ bar} = 15 \times 100000 = 15 \times 10^5 \text{ N/m}^2$$

Speed = 1700 rev/min

$$T = 15 \text{ Nm}, \quad \text{MD} = 10 \text{ cm}^3/\text{rev}$$

i) Volumetric efficiency =  $\frac{\text{Actual flow rate}}{\text{Ideal flow rate}}$



$$\begin{aligned} \text{Ideal flow rate} &= \text{Nominal flow rate} \times \text{Speed} \\ &= \cancel{100} \text{ cm}^3/\text{rev} \times 1700 \text{ rev}/\text{min} \\ &= 170000 \text{ cm}^3/\text{min} \end{aligned}$$

$$\text{Ideal flow rate} = \frac{170000}{1000000} = 0.17 \text{ m}^3/\text{min}$$

$$\text{Actual flow rate} = 0.05 \text{ m}^3/\text{min}$$

$$\therefore \text{Volumetric efficiency} = \frac{0.05}{0.17} = 2.94\%$$

ii) Fluid power =  $P \times Q$

$$P = 15 \times 10^5 \text{ N/m}^2$$

$$Q = 0.05 \text{ m}^3/\text{min} = \frac{0.05}{60} = 8.33 \times 10^{-4} \text{ m}^3/\text{s}$$

$$\begin{aligned} \text{Fluid power} &= 15 \times 10^5 \times 8.33 \times 10^{-4} \\ &= 15 \times 10^5 \times 83.3 \times 10^{-5} \\ &= 1249.5 \times 10^0 = 1249.5 \text{ Watts} \end{aligned}$$

iii

$$\text{iii) Shaft power} = \frac{2\pi NP}{60} = \frac{2\pi \times 1700 \times 15}{60} = 2670.35 \text{ watts}$$