

- 4 Specific gravity of mercury = 13.6
 " " of sea = 1.026

Difference in mercury level = 170 mm = 0.17 m

$$h = \left[\frac{S.G. \text{ of mercury}}{S.G. \text{ of liquid}} - 1 \right] y$$

$$h = 0.17 \left[\frac{13.6}{1.026} - 1 \right]$$

$$h = 2.083$$

$$V = C_d \times \sqrt{2gh}$$

$$V = 1 \times \sqrt{2 \times 9.81 \times 2.083}$$

$$V = \underline{6.39 \text{ m/s}}$$

- 5 Volumetric flow rate = $0.05 \text{ m}^3/\text{min} = 8.3333 \times 10^{-5} \text{ m}^3/\text{s}$
 pressure change = 15 bar = $1.5 \times 10^6 \text{ N/m}^2$
 Speed of rotation = 1700 rev/min = 28.333 rev/s
 torque input = 15 Nm
 Normal displacement = $10 \text{ cm}^3/\text{rev} = 1 \times 10^{-5} \text{ m}^3/\text{rev}$

a) Volumetric efficiency = $\frac{\text{Actual flow rate}}{\text{Theoretical flow rate}} \times 100$

Actual flow rate = 8.33×10^{-5}

Theoretical flow rate = speed of rotation \times displacement
 $= 28.333 \times 1 \times 10^{-5}$
 $= 2.83 \times 10^{-4} \text{ m}^3/\text{s}$

Volumetric efficiency = $\frac{8.33 \times 10^{-5}}{2.83 \times 10^{-4}} \times \frac{100}{1}$
 $= \underline{29.45\%}$

- b. Fluid power = $Q(P_2 - P_1)$
 $(P_2 - P_1) = 1.5 \times 10^6 \text{ N/m}^2$
 $= 8.3333 \times 10^{-5} \times 1.5 \times 10^6$
 $= \underline{124.99 \text{ watt}}$

$$Q = \frac{0.78 \times 0.0314 \times 7.854 \times 10^{-3}}{\sqrt{0.0314^2 - (7.854 \times 10^{-3})^2}} \times \sqrt{2 \times 9.81 \times 17.09}$$

$$Q = \frac{0.94 \times 0.0314 \times 7.854 \times 10^{-3} \times 18.5773}{0.02}$$

$$Q = \underline{0.149 \text{ m}^3/\text{s}}$$

3. Orifice diameter = 15 cm = $15 \times 10^{-2} \text{ m}$
 pipe diameter = 30 cm = $30 \times 10^{-2} \text{ m}$
 $P_1 - P_2 = 80 \text{ cmHg} = 6666.12 \text{ N/m}^2$
 Specific gravity of oil = 0.9, $C_d = 0.64$

$$Q = C_d A_o A_1 \sqrt{\frac{2gh}{A_o^2 - A_1^2}}$$

$$A_o = \frac{\pi (15 \times 10^{-2})^2}{4} = 0.0177 \text{ m}^2$$

$$A_1 = \frac{\pi (30 \times 10^{-2})^2}{4} = 0.0707 \text{ m}^2$$

$$h = \frac{P_1 - P_2}{\rho} = \frac{6666.12}{8829} = 0.755 \text{ m}$$

$$S.G. = \frac{\rho}{1000 \times 9.81}$$

$$\rho = 0.9 \times 1000 \times 9.81$$

$$\rho = 8829$$

$$Q = 0.64 \times 0.0177 \times 0.0707 \times \frac{\sqrt{2 \times 9.81 \times 0.755}}{\sqrt{0.0707^2 - (0.0177)^2}}$$

$$Q = 0.64 \times 0.0177 \times 0.0707 \times \frac{3.847}{\sqrt{0.0707^2 - (0.0177)^2}}$$

$$\therefore Q = \underline{0.075 \text{ m}^3/\text{s}}$$

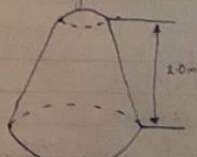
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1.

Assignment



Using Bernoulli's equation

$$\frac{P_1}{\rho} + z_1 + \frac{V_1^2}{2g} = \frac{P_2}{\rho} + z_2 + \frac{V_2^2}{2g}$$

$$z_1 = z_2$$

$$2.5 + 2.0 + \frac{5^2}{2 \times 9.81} = \frac{P_2}{\rho} + 0 + \frac{2^2}{2 \times 9.81}$$

$$2.5 + 2.0 + 1.27 = \frac{P_2}{\rho} + 0 + 0.20$$

$$\frac{P_2}{\rho} = 5.77 - 0.20$$

$$\frac{P_2}{\rho} = 5.57 \text{ m}$$

Inlet diameter = 20 cm = 20×10^{-2} m

Inlet pressure = 17.655 N/cm² = 176550 N/m²

Throat diameter = 10 cm = 10×10^{-2} m

Throat pressure = 30 cm Hg = 3997.67 N/m², $C_d = 0.78$

$$Q = C_d \frac{A_1 A_2}{\sqrt{A_1^2 - A_2^2}} \sqrt{2gh}$$

$$h = \frac{P_1 - P_2}{\rho} = \frac{176550 - 3997.67}{1000 \times 9.81} = 17.97 \text{ m}$$

$$A_1 = \frac{\pi (0.2)^2}{4} = 0.0314 \text{ m}^2$$

c. Shaft power = $\gamma \times \omega$
 $= 2 \times \pi \times \text{speed of rotation}$
 $= 2 \times \pi \times 28.3$
 $= 177.81 \text{ rad/s}$

$$\text{Shaft power} = 15 \times 177.81$$
$$= \underline{\underline{2667.2 \text{ watts}}}$$

d. Overall efficiency = $\frac{\text{Fluid power}}{\text{shaft power}} \times 100$
 $= \frac{124.95}{2667.2} \times 100$
 $= \underline{\underline{4.68\%}}$