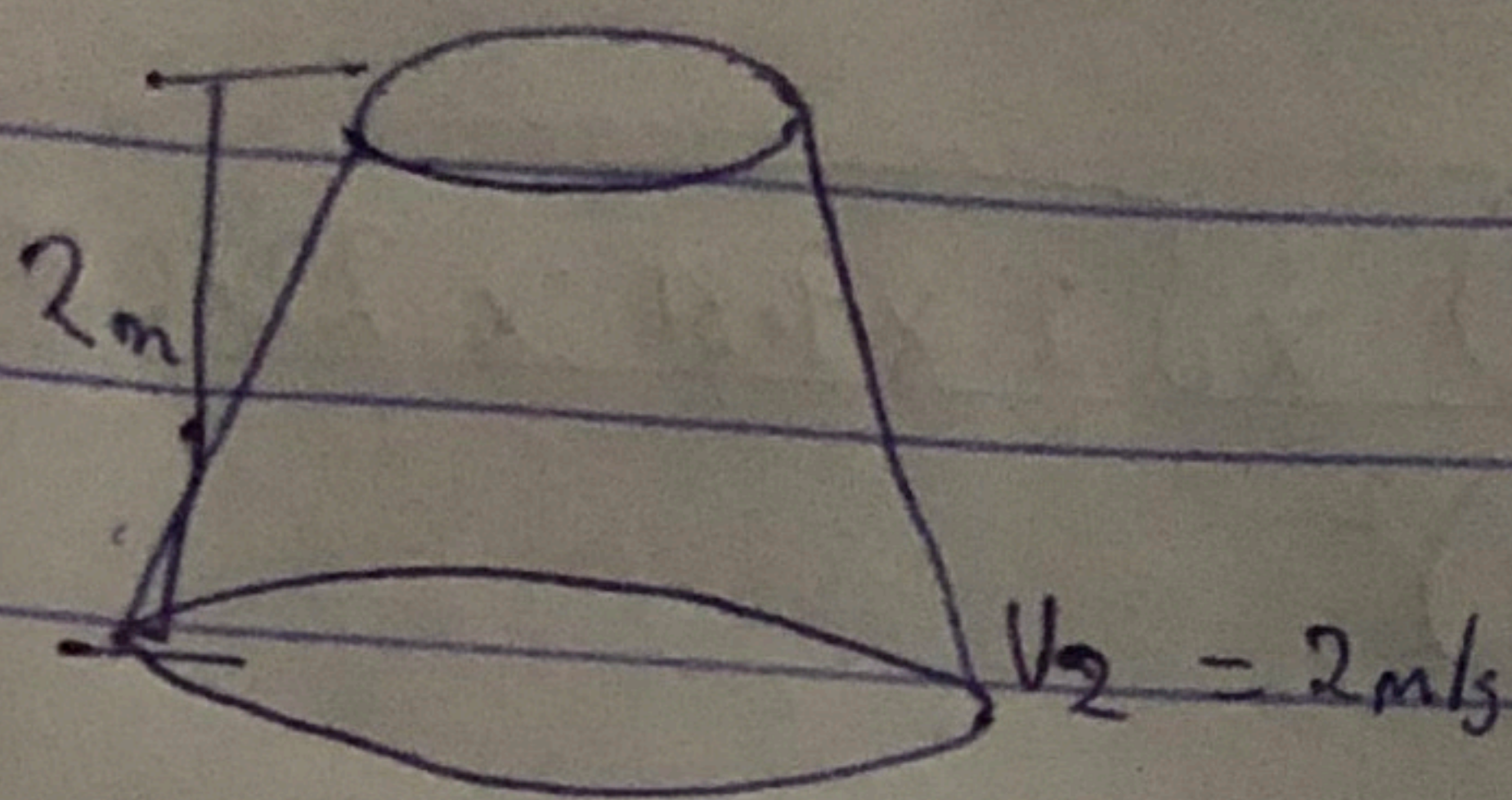


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1.



$$P_{T_1} = \frac{P_1}{\omega} = 2.5 \text{ m}$$

$$H_L = \frac{0.35(V_1 - V_2)^2}{2g}$$

Using Bernell's equation $\frac{P_1}{\omega} = ?$

$$\frac{P_1}{\omega} + \frac{V_1^2}{2g} + z_1 = \frac{P_2}{\omega} + \frac{V_2^2}{2g} + z_2 + H_L$$

$$\frac{P_2}{\omega} = \frac{P_1}{\omega} + \left[\frac{V_1^2 - V_2^2}{2g} \right] + [z_1 - z_2] - H_L$$

$$\frac{P_2}{\omega} = 2.5 + \left[\frac{5^2 - 2^2}{2 \times 9.81} \right] + 2 - \frac{0.35(5-2)^2}{2 \times 9.81}$$

$$\frac{P_2}{\omega} = 2.5 + 1.07 + 2 - 0.161$$

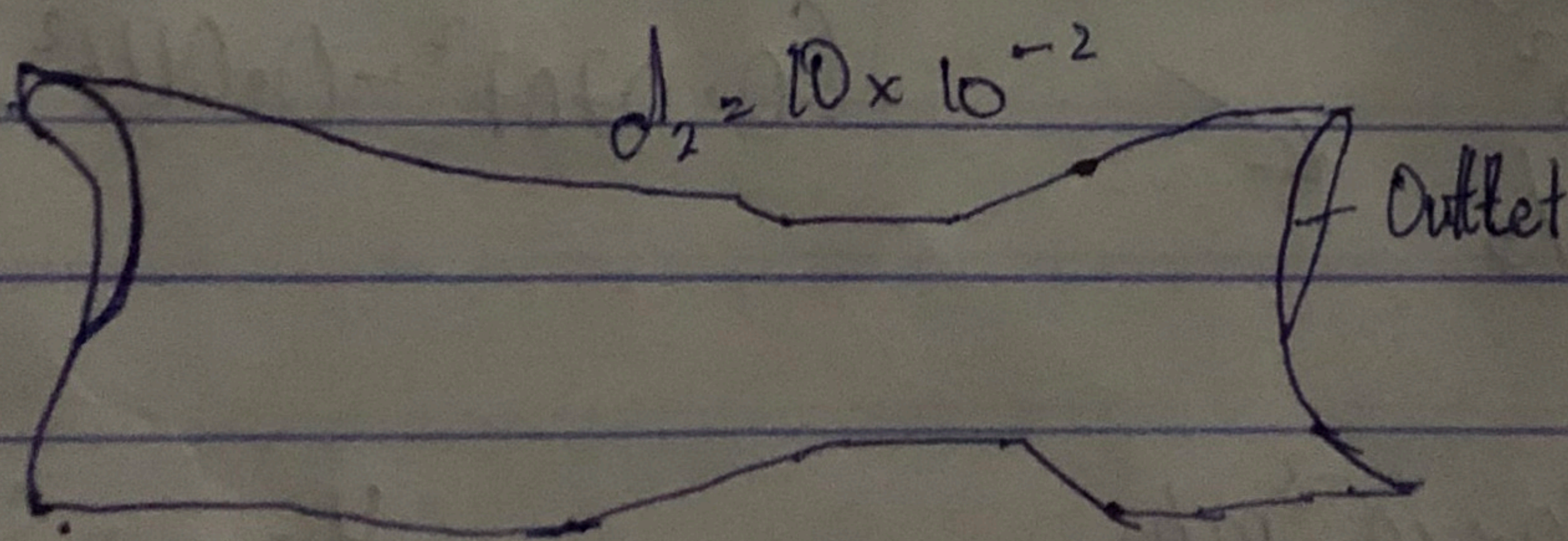
$$\frac{P_2}{\omega} = 5.409 \text{ m}$$

\therefore The Pressure head at the lower end is

$$\pm 5.409 \text{ m}$$

2.) Inlet

$$d_1 = 20 \times 10^{-2} \text{ m}$$



$$P_1 = 17.658 \text{ N/cm}^3 = 17.658 \times 10^4 \text{ N/m}^2 \quad C_d = 0.98$$

$$P_2 = 300 \text{ mm Hg} = 30 \times 10^{-2} \text{ m Hg}$$

$$Q = ?$$

$$A_1 = \frac{\pi \times (20 \times 10^{-2})^2}{4} = 0.03 \text{ m}^2$$

$$A_2 = \frac{\pi \times (10 \times 10^{-2})^2}{4}$$

$$\frac{P_2}{\omega} = 0.3 \times 13.6 = 4.08 \text{ m Hg}$$

$$= 7.85 \times 10^{-3} \text{ m}^2$$

$$\frac{P_2}{\omega} = -4.08 \text{ (since Vacuum pressure)}$$

$$h = \frac{P_1}{\omega} - \frac{P_2}{\omega} = 18 - 4.08 = 22.08$$

$$\frac{P_1}{\rho} = \frac{12.058 \times 10^4}{9.81 \times 10^3} = 1.9$$

$$Q = C_d \frac{A_1 A_2 \sqrt{2gh}}{\sqrt{A_1^2 - A_2^2}}$$

$$Q = 0.98 \times 0.03 \times (7.85 \times 10^{-3}) \times \sqrt{2 \times 9.81 \times 22.08} \\ \sqrt{(0.03^2 - (7.85 \times 10^{-3})^2)}$$

$$Q = 0.166 \text{ m}^3/\text{s}$$

3.) $A_0 = 15 \times 10^{-2} \text{ m}$
 $A_0 = \frac{\pi \times (15 \times 10^{-2})^2}{4}$

$$0.01767 \text{ m}^2$$

$$A_1 = \frac{\pi \times (30 \times 10^{-2})^2}{4} = 0.0707 \text{ m}^2$$

$$H = 30 \times 10^{-2} \left(\frac{13.6}{0.9} - 1 \right)$$

$$H = 7.055 \text{ m}$$

$$Q = C_d \frac{A_0 A_1 \sqrt{2gh}}{\sqrt{A_1^2 - A_0^2}} = \frac{0.64 \times 0.0176 \times 0.0707 \sqrt{2 \times 9.81 \times 7.055}}{\sqrt{(0.0707^2 - 0.0176^2)}}$$

$$Q = 0.137 \text{ m}^3/\text{s}$$

$$d_1 = 30 \times 10^{-2} \text{ m}$$

$$y = 50 \times 10^{-2} \text{ m Hg}$$

$$\text{S.G. of oil} = 0.9$$

$$H = y \left[\frac{S_m}{S_o} - 1 \right]$$

$$C_d = 0.64$$

$$Q = ?$$

$$S_m = 13.6$$

$$S_o = 0.9$$

4.) $y = 170 \text{ mm Hg} = 170 \times 10^{-3} \text{ m Hg}$

$$\text{S.G. of mercury} = 13.0 \text{ hg}$$

$$\text{S.G. of Sea water} = 1.026$$

$$V = \sqrt{2gH}$$

$$V = \sqrt{2 \times 9.81 \times 2.08}$$

$$V = 6.39 \text{ m/s}$$

$$H = y \times \frac{S_m}{S_o} - 1$$

$$H = 170 \times 10^{-3} \times \left(\frac{13.6}{1.026} - 1 \right)$$

$$H = 2.08 \text{ m}$$

5.) Actual flow rate $Q = 0.03 \text{ m}^3$ $3 \text{ dm}^3/\text{min}$

$$= 8.33 \times 10^{-5} \text{ m}^3/\text{sec}$$

$$P = 15 \text{ bar} = 15 \times 10^5 \text{ N/m}^2$$

$$N = 1700 \text{ rev/min} = 28.33 \text{ rev/sec}$$

$$V = 15 \text{ ml} \quad \text{Normal displacement} = 10 \text{ cm}^3/\text{rev} = 1 \times 10^{-5} \text{ m}^3/\text{rev}$$

9.) Volumetric Efficiency

$$\frac{\text{Actual flow rate}}{\text{Total flow rate}} \times 100\%$$

$$\text{Total flow rate} = \text{displacement} \times N$$

$$Q = 1 \times 10^{-5} \times 28.33$$

$$= 2.833 \times 10^{-4} \text{ m}^3/\text{sec}$$

$$\text{Volumetric Efficiency} = \frac{8.33 \times 10^{-3}}{2.833 \times 10^{-4}} \times 100$$

$$= 29.4\%$$

ii) fluid power ($Q \times \Delta P$)

$$= 8.33 \times 10^{-3} \times 15 \times 10^5 = 124.95 \text{ watts}$$

iii) Shaft power = $T \times \omega$

$$\omega = 2\pi \times N$$

$$\omega = 2 \times \pi \times 28.33 = 178 \text{ Watt/sec.}$$

$$\text{Shaft power} = T \times \omega$$

$$= 15 \times 178$$

$$= 2670 \text{ watts}$$

iv) Overall Efficiency

$$\frac{\text{fluid power}}{\text{Shaft power}} \times 100\%$$

$$= \frac{124.95}{2670} \times 100$$

$$= 4.68\%$$

$$= 4.68\%$$