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Actual flow rate = $10 \text{ dm}^3/\text{min} = 1.667 \times 10^{-4} \text{ m}^3/\text{s}$

Normal displacement = $10 \text{ cm}^3/\text{rev} = 1 \times 10^{-5} \text{ m}^3/\text{rev}$

speed rotation = $1500 \text{ rev}/\text{min} = 25.05 \text{ rev}/\text{sec}$

Ideal flow rate = Normal displacement \times speed rotation

= $1 \times 10^{-5} \times 25.05$

= $2.505 \times 10^{-4} \text{ m}^3/\text{s}$

$\therefore \eta_v = \frac{\text{Actual flow rate}}{\text{Ideal flow rate}} \times 100$

= $\frac{1.667 \times 10^{-4}}{2.505 \times 10^{-4}} \times 100$

= 0.6654691

= 0.665

= 66.5%

Fluid power = Actual flow rate \times pressure change

Pressure change = $12 \text{ bar} = 12 \times 10^5 \text{ N/m}^2$

= $1.667 \times 10^{-4} \times 12 \times 10^5$

= $200.04 \text{ Nm}/\text{sec}$

Shaft power = Torque input \times Angular speed

$T \cdot \omega = 12.5 \text{ Nm}$

Angular speed = $2\pi \times \text{speed of rotation}$

= $2\pi \times 25.05$

= $157.39 \text{ rev}/\text{sec}$

shaft power = 12.5×157.39

= $1967.42 \text{ Nm}/\text{sec}$

Overall efficiency = $\frac{\text{fluid power}}{\text{shaft power}} \times 100$

= $\frac{200.04 \times 100}{1967.42} = 10.16\%$

$$35 \times 1.667 \times 10^{-3}$$

2) flow rate = $35 \text{ dm}^3/\text{min} = 5.8345 \times 10^{-4} \text{ m}^3/\text{sec}$
 pressure change = $100 \text{ bar} = 100 \times 10^5 \text{ N/m}^2$
 fluid power = Actual flow rate \times pressure change
 $35 \times 1.667 \times 10^{-3} \times 100 \times 10^5$
 $= 5834.5 \text{ W}$

Overall efficiency = $\frac{\text{fluid power} \times 100}{\text{shaft power}}$

$$0.8 = 87\%$$

Shaft power = x

$$87 = \frac{5834.5 \times 100}{x}$$

$$87x = 5834.5 \times 100$$

$$x = \frac{583450}{87}$$

$$x = 6706.32 \text{ W}$$

3) Actual flow rate = $35 \text{ dm}^3/\text{min} = 5.8345 \times 10^{-4} \text{ m}^3/\text{sec}$
 Normal displacement = $50 \text{ cm}^3/\text{rev} = 5 \times 10^{-5} \text{ m}^3/\text{rev}$
 Speed of rotation = $880 \text{ rpm} = 14.67 \text{ rev/sec}$
 Fluid power = $A \cdot f \cdot p = C$
 If $p = 100 \text{ bar} = 100 \times 10^5 \text{ N/m}^2$
 $F \cdot p = 5.8345 \times 10^{-4} \times 100 \times 10^5$
 $= 5834.5 \text{ W}$

Shaft power = $15 \text{ kW} = 15000 \text{ W}$

Overall efficiency = $\frac{5834.5 \times 100}{15000}$

shaft power = $38.89 \approx 38.9\%$

Hydraulic efficiency = $\frac{\text{Actual flow rate} \times 100}{\text{Ideal flow rate}}$

$$= \frac{5.8345 \times 10^{-4} \times 100}{7.05175 \times 10^{-4}}$$

$$= 82.72\%$$

No. of ideal flow rate = Normal dia \times speed of rotation
 $= 5 \times 10^{-5} \times 14.67 = 7.05175 \times 10^{-4}$

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Water level (H) = 24,000 cm = 240 m
 Volumetric flow rate = $13 \times 10^{-3} \text{ m}^3/\text{sec}$
 Velocity of jet = 66 m/sec
 $p = 0, v = 0$
 Density for water = 1000 kg/m^3

1) Power of jet

$$P = p\phi + \frac{\rho \cdot \phi v^2}{2} + \rho g \phi x$$

recall $p = 0, v = 0$

$$P = 0(\phi) + \frac{\rho \cdot \phi v^2}{2} + \rho g \phi (0)$$

$$P = \frac{\rho \phi v^2}{2} = \frac{1000 \times 13 \times 10^{-3} \times 66^2}{2}$$

$$P = 28314 \text{ KN}$$

2) Power supplied from reservoir

$p = 0, v = 0$

$$P = p\phi = \frac{\rho \phi v^2}{2} + \rho g \phi z$$

$$0 = 0 \cdot \phi = \frac{\rho \phi (0)^2}{2} + \rho g \phi z \quad P = \rho g \phi z$$

$$P = \rho g \phi z = 1000 \times 9.81 \times 13 \times 10^{-3} \times 240$$

$$P = 30607.2 \text{ KN} = 30607.2 \text{ N}$$

Head used to overcome losses

Head loss = power lost in transmission

$$\text{Power lost in transmission} = \frac{\rho g \phi z}{\text{Power of jet}}$$

$$= 30607.2 - 28314$$

$$= 2293.2 \text{ N}$$

3.

$$\text{Head loss} = \frac{2293.2}{1000 \times 9.81} \times 13 \times 10^{-3} = 17.98 \text{ m}$$

1) Efficiency of the nozzle & pipeline

$$\eta = \frac{\text{power of jet}}{\text{power of reservoir}} \times 100$$

$$= \frac{28314}{306070.2} \times 100 = 92.5\%$$

2) $Z = 30 \text{ m}$
 $Q = 220 \text{ litres/sec} = 220 \times 10^{-3} \text{ m}^3/\text{sec}$
 $v = 7 \text{ m/sec}$
 $\rho = 0.89 \times 1000 = 890 \text{ kg/m}^3$

3) Power of jet

$$P = \rho Q + \frac{\rho Q v^2}{2} + \rho g Q z \quad \text{when } p=0, \text{ } v=0$$

$$P = \rho Q + \frac{\rho Q v^2}{2} + \rho g Q z$$

$$= 890 \times 220 \times 10^{-3} + \frac{890 \times 220 \times 10^{-3} \times (7)^2}{2} + 890 \times 9.81 \times 220 \times 10^{-3} \times 30$$

$$= 4757 \text{ N} \quad \text{or} \quad 4.757 \text{ kN}$$

4) Power supplied from reservoir

$$P = \rho Q + \frac{\rho Q v^2}{2} + \rho g Q z$$

$$P = \rho Q + \frac{\rho Q v^2}{2} + \rho g Q z$$

$$= 890 \times 220 \times 10^{-3} + \frac{890 \times 220 \times 10^{-3} \times (7)^2}{2} + 890 \times 9.81 \times 220 \times 10^{-3} \times 30$$

$$= 576.24 \text{ kN}$$

Head used to overcome losses

Head loss = power lost to transmission

$$\text{Power lost to transmission} =$$

$$\text{Power of reservoir} - \text{power of jet}$$

$$= 571442.3$$

$$H \cdot L = \frac{571442.3}{890 \times 9.81 \times 220 \times 10^{-3}} = 290.50 \text{ m}$$

$$\text{Efficiency of pipeline and nozzle} = \frac{\text{Power of jet}}{\text{Power of reservoir}} \times 100$$

$$= \frac{4797.1}{5717.42} \times 100 = 84.08\%$$

$$h = 20\text{m}$$

$$d_1 = 10\text{cm} = 0.1\text{m}$$

$$d_2 = 5\text{cm} = 0.05\text{m}$$

$$C_d = 0.8 \text{ m/s}^{-2}$$

By conservation of energy $\frac{1}{2} \rho V^2 = \rho g h$

$$V^2 = 2gh \quad V = \sqrt{2gh} \quad V = \sqrt{2 \times 9.81 \times 20}$$

$$V = 19.8 \text{ m/s}$$

Flux rate at base,

$$\pi r^2 V = \pi \times (0.05)^2 \times 19.8 = 0.1555 \text{ m}^3/\text{s}$$

To find the amount of water that emerges

$$m = \rho \pi r^2 V$$

$$\frac{m}{t} = 1000 \times \pi \times (0.05)^2 \times 19.8$$

$$= 155.5088 \text{ kg}$$

$$P = \frac{W}{t} = \frac{mgh}{t} = (\rho \pi r^2 V) g h$$

$$= 155.5088 \times (9.81) \times (20)$$

$$P = 30479.02 \text{ N}, P = 30.479 \text{ kN}$$

$$\rho g = 19.62 \text{ N/m}^2$$

$$C_d = 0.96, d_1 = 0.05\text{m}, d_2 = 0.2\text{m}$$

$$u_1 = \frac{Q}{\text{section}} \quad u_2 = \frac{Q}{\text{section}}$$

$$0.6514$$

for the manometer:

$$P_1 + \rho g z_1 = P_2 + \rho g (z_2 - R) + \rho g R$$

$$P_1 - P_2 = 19.62 (z_2 - z_1) + 587.9 \text{ --- (4)}$$

for the venturimeter

$$\frac{P_1}{\rho g} + \frac{U_1^2}{2g} + Z_1 = \frac{P_2}{\rho g} + \frac{U_2^2}{2g} + Z_2$$

$$P_1 - P_2 = 18062 (Z_2 - Z_1) + 0.803 U_2^2 \quad \text{--- (1)}$$

$$0.803 U_2^2 = 587.423$$

$$U_{ideal} = 27.047 \text{ m/s}$$

$$Q_{ideal} = 27.047 \times \pi (0.2)^2 = 0.85 \text{ m}^3/\text{s}$$

$$Q = C_d Q_{ideal} = 0.96 \times 0.85$$

$$Q = 0.816 \text{ m}^3/\text{sec}$$