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FLUID MECH  
COMPUTER ENGINEERING

$$1) Q = 10 \text{ dm}^3/\text{min} = 10/1000 \times 60 \\ = 1.667 \times 10^{-4} \text{ m}^3/\text{s}$$

$$\Delta P = 12 \text{ Bar} = 12 \times 10^5 \text{ N/m}^2$$

$$\text{Speed of Rotation} = 1500 \text{ rev/min} \\ = 1500/60 \\ = 25 \text{ rev/s}$$

$$\text{Nominal displacement} = 10 \text{ cm}^3/\text{rev} \\ = 10/1000000 = 1 \times 10^{-5} \text{ m}^3/\text{rev}$$

$$\text{Torque Input} = 125 \text{ Nm}$$

$$\text{Volumetric Efficiency} = \frac{Q}{\text{Ideal flow rate}}$$

$$\text{Ideal flow rate} = \text{Nominal displacement} \times \text{speed} = 1 \times 10^{-5} \times 25 \\ = 2.5 \times 10^{-4} \text{ m}^3/\text{s}$$

$$\therefore \text{Volumetric Efficiency} = \frac{1.667 \times 10^{-4}}{2.5 \times 10^{-4}} \\ = 0.6668 \times 100\% = 66.68\%$$

$$\text{ii) Fluid Power} = Q \times \Delta P \\ = (1.667 \times 10^{-4}) \times (12 \times 10^5) = 200.04 \text{ W}$$

$$\text{iii) Shaft Power} = 2\pi T \times \text{speed} \\ = 2 \times 3.14 \times 125 \times 25 \\ = 1963.50 \text{ W}$$

$$\text{iv) Overall Efficiency} = \frac{\text{Fluid Power}}{\text{Shaft Power}} = \frac{200.04}{1963.50} = 0.102 \times 100 = 10.2\%$$

$$2) Q = 35 \text{ dm}^3/\text{min} = (35 \times 0.001)/60 \\ = 5.83 \times 10^{-4} \text{ m}^3/\text{s}$$

$$\Delta P = 100 \text{ bar} = 100 \times 10^5 \text{ N/m}^2$$

$$\text{Overall Efficiency} = 87\%$$

$$\text{Shaft Power} = \frac{\text{Fluid Power}}{\text{Overall Efficiency}}$$

$$= \frac{Q \times \Delta P}{87 \div 100} = \frac{5.83 \times 10^{-4} \times 100 \times 10^5}{0.87} = 6701.5 \text{ W}$$

$$3^c) Q = 35 \text{ dm}^3/\text{min} = (35 \times 0.001) / 60$$

$$= 5.83 \times 10^{-4} \text{ m}^3/\text{s}$$

$$\Delta P = 100 \text{ bar} = 100 \times 10^5 \text{ N/m}^2$$

$$\text{Shaft Power} = 15 \text{ kW}$$

$$\text{Speed Rotation} = 880 \text{ rev/min}$$

$$= 880/60 = 14.67 \text{ rev/s}$$

$$i) \text{ Volumetric Efficiency} = \frac{\text{Actual flowrate, } Q}{\text{Ideal flowrate}}$$

$$\text{Ideal flow} \cdot R = \text{Nominal displacement} \times \text{speed}$$

$$= 50 \text{ cm}^3/\text{rev} \times 14.67$$

$$= 5 \times 10^{-3} \times 14.67$$

$$= 7.0835 \times 10^{-4} \text{ m}^3/\text{s}$$

$$\therefore \text{Volumetric } \epsilon = \frac{5.83 \times 10^{-4}}{7.0835 \times 10^{-4}} = 82.3\%$$

$$ii) \text{ Overall Efficiency} = \frac{\text{Fluid P}}{\text{Shaft P}} = \frac{Q \times \Delta P}{\text{Shaft power}}$$

$$= \frac{5.83 \times 10^{-4} \times (100 \times 10^3)}{(15 \times 10^3)} = \frac{5830}{15000} = 0.3887 \times 100$$

$$= 38.87\%$$

Q10)

Difference of Mercury level,  $x = 170 \text{ mm} = 0.17 \text{ m}$

Speed of submarine = ?

S. gravity of mercury = 13.6

S. gravity of sea water = 1.026

$$\text{Differential Head, } h = x \left\{ \frac{\rho_1}{\rho_2} - 1 \right\}$$

$$= 0.17 \left( \frac{13.6}{1.026} - 1 \right)$$

$$= 2.0839 \text{ m of water}$$

Velocity/speed of Sub

$$v = \sqrt{2gh}$$

$$= \sqrt{2 \times 9.81 \times 2.0839}$$

$$= 2.22 \text{ m/s}$$

No(7)

Specific weight =  $19.62 \text{ N/m}^3$

$$C_d = 0.96$$

$$d_1 = 0.3 \text{ m}$$

$$d_2 = 0.2 \text{ m}$$

Calculate  $Q$ ,

$$V_1 = \frac{Q}{0.0707}, \quad V_2 = \frac{Q}{0.0314}$$

For the manometer

$$P_1 + \rho g Z = P_2 + \rho g (Z_2 - Z_1) + \rho g R_f$$

$$P_1 - P_2 = 19.62 (Z_2 - Z_1) + 587.423 \quad \text{--- (1)}$$

For the Venturimeter

$$\frac{P_1}{\rho g} + \frac{V_1^2}{2g} + Z_1 = \frac{P_2}{\rho g} + \frac{V_2^2}{2g} + Z_2$$

$$P_1 - P_2 = 19.62 (Z_2 - Z_1) + 0.803 V_2^2 \quad \text{--- (2)}$$

Comb. (1) & (2)  $\Rightarrow$

$$0.803 V_2^2 = 587.423$$

$$V_2 \text{ ideal} = 27.047 \text{ m/s}$$

$$Q_1 \text{ ideal} = 27.047 \times \pi \times \left(\frac{0.2}{2}\right)^2$$

$$= 0.85 \text{ m}^3/\text{s}$$

$$Q = C_d \cdot Q_{\text{ideal}} = 0.96 \times 0.85 = 0.816 \text{ m}^3$$

No(6)

$$\text{Power} = \frac{\text{Work done}}{\text{Time}}$$

$$\text{work done} = mgh / \text{time}$$

$V$  = Velocity of stream

$\rho$  = density of water ( $1000 \text{ kg/m}^3$ )

$$m = \rho \times V$$

$$V = \sqrt{2gh} = \sqrt{2 \times 9.81 \times 20} = 19.7989 \text{ m/s}$$

$$1) P \Rightarrow \rho \pi r^2 \frac{Vgh}{m^2} = 1000 \text{ kg/m}^3 \times \left(\frac{10 \times 10^{-2}}{2}\right)^2 \times 19.7989 \text{ m/s} \times 9.8 \text{ m/s}^2 \times 20$$

$$\text{Power} = 30478.63 \text{ W} \approx 30.5 \text{ kW}$$

Ab. 8

$$d_1 = 0.152 \text{ m} \Rightarrow A_1 = \frac{\pi}{4} (0.152)^2 \\ = 0.01814 \text{ m}^2$$

$$d_2 = 0.076 \text{ m} \Rightarrow A_2 = \frac{\pi}{4} (0.076)^2 = 0.00464 \text{ m}^2$$

$$\rho = 0.8 \times 1000 = 800 \text{ kg/m}^3$$

$$C_d = 0.97$$

$\Rightarrow$  Apply Bernoulli

$$\frac{P_1}{\rho g} + \frac{V_1^2}{2g} + Z_1 = \frac{P_2}{\rho g} + \frac{V_2^2}{2g} + Z_2$$

(a)  $P_1 = P_2$

$$\frac{V_1^2}{2g} + Z_1 = \frac{V_2^2}{2g} + Z_2$$

By continuity =

$$Q = V_1 A_1 = V_2 A_2$$

$$V_2 = V_1 \frac{A_1}{A_2}$$

$$\frac{V_1^2}{2g} = 0.314 = \frac{16(V_1^2)}{2g}$$

$$V_1 = \sqrt{\frac{0.314 \times 2 \times 9.81}{16}} = 1.0934 \text{ m/s}$$

$$Q = C_d A_1 V_1 = 0.97 \times (0.01814) \times (1.0934)$$

b)  $P_1 - P_2 = 18170$

$$\Rightarrow \frac{P_1 - P_2}{\rho g} = \frac{V_2^2 - V_1^2}{2g} - 0.914$$

$$\frac{18170}{800 \times 9.81} = \frac{Q^2 \left[ (0.2043)^2 - (55.11)^2 \right]}{2 \times 9.81} - 0.914$$

$$\Rightarrow Q = 0.035 \text{ m}^3/\text{s}$$

No. (3-1)

⇒ At section 1

$$r_1 = 0.3 \text{ m, Area} = \pi/4 \times (0.3)^2 = 0.07068 \text{ m}^2, \text{ Pressure, } P_1 = 400 \text{ kPa}$$

Height of upper end above the datum,  $(Z_1) = 10 \text{ m}$

⇒ At section 2,

$$r_2 = 180 \text{ mm} = 0.18 \text{ m, Area} = \pi/4 (0.18)^2 = 0.01767 \text{ m}^2$$

Height of lower end of datum = 6

⇒ Rate of flow,  $Q = 0.04 \text{ m}^3/\text{sec}$

⇒ As the flow is continuous,

$$Q = A_1 V_1 = A_2 V_2 \text{ (Continuity Eqn)}$$

$$V_1 = Q/A_1 = \frac{0.04}{0.07068} = 0.5658 \text{ m/s}$$

$$V_2 = Q/A_2 = \frac{0.04}{0.01767} = 2.2625 \text{ m/s}$$

⇒ Apply Bernoulli equation at section 1 & 2

$$\frac{P_1}{\rho g} + \frac{V_1^2}{2g} + Z_1 = \frac{P_2}{\rho g} + \frac{V_2^2}{2g} + Z_2$$

$$\frac{P_2}{\rho g} = \frac{400 \times 10^3}{1000 \times 9.81} + \frac{(0.5658^2 - 2.2625^2)}{2 \times 9.81} + (10 - 6)$$

$$\frac{P_2}{\rho g} = 414.53$$

$$P_2 = 486.838 \text{ kN/m}^2$$

No. (4)

$$Z = 240 \text{ m}$$

Volumetric flow rate = 13 L/sec

$$= \frac{13}{1000} \text{ m}^3/\text{sec} = 13 \times 10^{-3} \text{ m}^3/\text{sec}$$

Jet Velocity = 60 m/s

Water Density = 1000 kg/m<sup>3</sup>

Since  $P=0$  and  $Z=0$

$$P = (0 \cdot Q) + \frac{\rho \cdot Q \cdot V^2}{2} + \rho g Q(b)$$

$$\Rightarrow P = \frac{\rho Q \cdot V^2}{2}$$

$$= \frac{1000 \times 13 \times 10^{-3}}{2} \times 66^2$$

$P = 28314$  watts; Power of Jet

$\Rightarrow$  Power Supplied from reservoir

Since  $P = 0$  &  $V = 0$ ;

$$P = (0 \times P) + \frac{\rho(0)^2 Q}{2} + \rho g Q z$$

$$\Rightarrow P = \rho g Q z$$

$$= 1000 \times 9.81 \times 13 \times 10^{-3} \times 240$$

$$= 30607.2 \text{ Watts}$$

$\Rightarrow$  Power lost in transmission = Power of reservoir - Jet Power  
 $= 30607.2 - 28314 = 2293.2$

Head loss in pipeline  $\Rightarrow \frac{2293.2}{1000 \times 9.81 \times 13 \times 10^{-3}} = 17.782 \text{ m}$

$$\text{Efficiency} = \frac{\text{Jet } P}{\text{Reservoir } P} \times 100\%$$

$$= \frac{28314}{30607.2} \times 100\% = 92.5\%$$

No. (5)

S.G. of oil = 0.89

$L = 30000 \text{ cm} = 300 \text{ m}$

$Q = 200 \text{ L/sec} = 0.22 \text{ m}^3/\text{sec}$

$V = 7 \text{ m/sec}$

Introductory  $Z = 0$ , and  $P = 0$ ,

$$\Rightarrow P = \frac{\rho Q V^2}{2} \text{ - Jet power}$$

Recall,  $S_g = 0.89$

$$S_g = \frac{\rho}{1000} \therefore \rho = 890$$

$$P = \frac{890 \times 0.22 \times 7^2}{2} = 4797.1 \text{ Watts}$$

$\Rightarrow$  Power Supplied from reservoir;

$$P = \rho g Q x$$
$$= 890 \times 9.81 \times 0.22 \times 300 = 576239.4 \text{ watts} \approx 576.24 \text{ Kwatts.}$$

$$\Rightarrow \text{Power loss}$$
$$= (576.24 - 4.7921) \text{ Kwatts}$$
$$= 571.4423 \text{ Kwatts} = 571442.3 \text{ Watts}$$

$$\Rightarrow \text{Head used to overcome losses}$$
$$= \frac{571442.3}{890 \times 9.81 \times 0.22} = 297.51 \text{ m}$$