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1) Pressure head at smaller end = 2.5m

Length of tube = 200

Velocity of flow at low end = 5ms⁻¹ v₁

" " " " higher " = 2ms⁻¹ v₂

Loss of head = $0.55 \frac{(v_1 - v_2)^2}{2g}$ h_f

$$= \frac{0.55 (5-2)^2}{2 \times 9.81} = 0.16m$$

Pressure head at higher end, $\frac{p_2}{\rho g}$

$$\frac{p_1}{\rho g} + \frac{v_1^2}{2g} + Z_1 + h_f = \frac{p_2}{\rho g} + \frac{v_2^2}{2g} + Z_2 + h_c \quad [Z_2 = 0, Z_1 = 2.0m]$$

$$2.5 + \frac{5^2}{2 \times 9.8} + 2 = \frac{p_2}{\rho g} + \frac{2^2}{2 \times 9.8} + 0 + 0.16$$

$$5.775 = \frac{p_2}{\rho g} + 0.364$$

$$\frac{p_2}{\rho g} = 5.775 - 0.364 = 5.411m \text{ of liquid}$$

Pressure head at higher end = 5.411m

2) Inlet diameter = 20cm = 0.2m

throat diameter = 10cm = 0.1m

Pressure at inlet = 17.88N/cm² = 17.88kN/m²

Sea of mercury

Coefficient of discharge = 0.98

Solve

$$\text{Area of inlet } A_1 = \frac{\pi}{4} \times 0.2^2 = 0.0314 \text{ m}^2$$

$$\text{Area of throat } = \frac{\pi}{4} \times 0.1^2 = 0.00785 \text{ m}^2$$

$$\frac{p_1}{\rho g} = \frac{17.88}{9.8} = 18.01m$$

Velocity pressure at the throat,

$$\frac{P_1}{\rho} = -3000 = -0.3 \times 13.6 = -4.08 \text{ m of water}$$

Differential head, $h = \frac{P_1}{\rho} - \frac{P_2}{\rho} = 18.01 - (-4.08) = 22.09 \text{ m}$

Rate of flow, Q

Using the relation, $Q = C_1 \times A_1 A_2 \times \sqrt{2gh}$
 $\sqrt{A_1^2 - A_2^2}$

$$= 0.18 \times 0.0314 \times 0.00785 \times \sqrt{2 \times 9.81 \times 22.09}$$
$$= \frac{0.000241 \times 20.82}{0.0304}$$

$$Q = 0.165 \text{ m}^3/\text{s}$$

3) Area

Area of orifice diameter $P_2 = 1500 = 0.15 \text{ m}^2$

Pipe diameter = ~~3000~~ = ~~0.3 m~~

Manometer

Area of orifice, $\frac{\pi}{4} \times 0.15^2 = 0.0177 \text{ m}^2 = A_0$

Area of pipe, $\frac{\pi}{4} \times 0.3^2 = 0.707 \text{ m}^2 = A_1$

Differential head, $h = y \left[\frac{S_{HL}}{S_0} - 1 \right]$

$$= 0.5 \left[\frac{13.6}{0.9} - 1 \right] = 7.06 \text{ m of oil}$$

Discharge Q : Using the relation; $Q = C_1 \times A_0 \times A_1 \times \sqrt{2gh}$

$$Q = 0.164 \times 0.707 \times 0.0177 \times \sqrt{2 \times 9.8 \times 7.06} = \frac{0.0142}{0.177} = \frac{\sqrt{(0.707)^2 - (0.0177)^2}}{0.177}$$

4) Recovery of Using the relation; $h = y \left[\frac{S_1 - S_2}{S_1} \right]$

$$h = 0.17 \left[\frac{13.6 - 1}{1.076} \right] = 2.08$$

∴ Speed of the submarine,

$$V = \sqrt{2gh} = \sqrt{2 \times 9.81 \times 2.08} = 6.38 \text{ m/s}$$

5) Actual flow rate = $0.05 \text{ m}^3/\text{min} = \frac{0.05}{60} = 8.3 \times 10^{-4} \text{ m}^3/\text{sec}$

Pressure charge = $15 \text{ bar} = 15 \times 10^5 \text{ N/m}^2$

Speed of rotation = $1700 \text{ rev/min} = \frac{1700}{60} = 28.3 \text{ rps}$

Normal displacement = $10 \text{ cm}^3/\text{rev} = 1 \times 10^{-5} \text{ m}^3/\text{rev}$

Torque input = 15 Nm

Ideal flow rate = Normal \times Speed displacement

$$= 28.3 \times 1 \times 10^{-5}$$

$$= 2.83 \times 10^{-4} \text{ m}^3/\text{sec}$$

i) Volumetric efficiency = $\frac{\text{Actual flow rate}}{\text{Ideal flow rate}} \times 100\%$

$$= \frac{8.3 \times 10^{-4}}{2.83 \times 10^{-4}} \times 100$$

$$= 296\%$$

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ii) Fract. power = $Q \cdot \Delta P$

$$= 8 \times 10^{-4} \times 15 \times 10^5$$

$$= 124.5 \text{ W} \text{ (HS or Nm/sec)}$$

iii) Fract. power Shaft power = $\frac{T \cdot \omega}{T \cdot \omega}$

$$T = 15 \text{ Nm}$$

$$\omega = 2\pi n \text{ for rps}$$

$$\omega = \frac{2\pi n}{60} \text{ for rpm}$$

$$V = \frac{2 \times 52 \times 28.3}{T} = \frac{177.8}{T} \text{ (m/sec)}$$

$$\text{Shaft power} = 15 \times 177.89$$

$$= 2668.35 \text{ W} \text{ (HS)}$$

$$\left[T = \text{Torque input, } \omega = \text{Angular speed} = \frac{2\pi \times 1700}{60} \right]$$

$$\text{iv) Overall efficiency} = \frac{\text{Final power}}{\text{Shaft power}} \times 100$$

$$= \frac{1245}{2668.35} \times 100$$

$$= 46.66\%$$

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