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18/ENG04/1007

ELECT/ELECT

FLUID MECHANICS

$$\begin{aligned} \text{Real flowrate} &= 10 \text{ dm}^3/\text{min} \quad T = 12.5 \text{ Nm} \\ &= \frac{10 \times 10^{-3}}{60} = 1.67 \times 10^{-4} \text{ m}^3/\text{s} \end{aligned}$$

$$\text{Pressure} = 12 \text{ bar} = 12 \times 10^5 \text{ N/m}^2$$

$$\text{Speed} = 1500 \text{ rev/min} = \frac{1500 \text{ rev}}{60} = 25 \text{ rev/sec}$$

$$\text{Nominal displacement} = \frac{10 \text{ cm}^3}{\text{rev}} = 1 \times 10^{-5} \text{ m}^3/\text{rev}$$

$$\begin{aligned} \text{Ideal flowrate} &= \text{Nominal displacement} \times \text{Speed} \\ &= 1 \times 10^{-5} \frac{\text{m}^3}{\text{rev}} \times 25 \frac{\text{rev}}{\text{sec}} \\ &= 2.5 \times 10^{-4} \text{ m}^3/\text{sec} \end{aligned}$$

$$\begin{aligned} \text{i) Volumetric efficiency} &= \frac{\text{Real flowrate}}{\text{Ideal flowrate}} \times 100\% \\ &= \frac{1.67 \times 10^{-4}}{2.5 \times 10^{-4}} \times 100\% \\ &= 66.8\% \end{aligned}$$

$$\begin{aligned} \text{ii) Fluid power} &= Q \cdot dp \\ &= 1.67 \times 10^{-4} \times 12 \times 10^5 \\ &= 200.4 \text{ watts} \end{aligned}$$

$$\begin{aligned} \text{iii) Shaft power} &= T \cdot \omega \\ \omega &= 2\pi N = 2 \times \pi \times 25 \\ &= 2 \times \pi \times 25 = 157.08 \end{aligned}$$

14) Overall Efficiency

$$\frac{\text{fluid power}}{\text{shaft power}} \times 100\%$$

$$\frac{200.4}{19.635} \times 100\% = 10.206 \approx 10.2\%$$

2) Pump delivery = $35 \text{ dm}^3/\text{min}$

$$\frac{35 \times 10^{-3}}{60} = 5.83 \times 10^{-4}$$

$$P = 100 \text{ bar} = 100 \times 10^5 \text{ Nm}^{-2}$$

Overall Efficiency = 87%

$$\begin{aligned} \text{fluid power} &= Q \cdot dp \\ &= 5.83 \times 10^{-4} \times 100 \times 10^5 \\ &= 5830 \text{ watts} \end{aligned}$$

Recall

$$\text{Overall Efficiency} = \frac{\text{fluid power}}{\text{shaft power}} \times 100\%$$

$$\begin{aligned} \text{shaft power} &= \frac{\text{fluid power} \times 100}{\text{Overall Efficiency}} \\ &= \frac{5830 \times 100}{87} \\ &= 6701.149 \text{ watts} \end{aligned}$$

3) Normal displacement of $50 \text{ cm}^3/\text{rev}$
 $\approx 50 \times 10^{-6} \text{ m}^3/\text{rev}$

Pressure = 100 bar = $100 \times 10^5 \text{ N/m}^2$

Shaft power = 15 kW = 15000 watts

Actual flowrate = $35 \text{ dm}^3/\text{min} = \frac{35 \times 10^{-3} \text{ m}^3}{60}$
 $= 5.83 \times 10^{-4} \text{ m}^3/\text{s}$

Speed = $850 \text{ rev/min} = \frac{850}{60}$
 $= 14.166 \approx 14.17 \text{ rev/s}$

Ideal flowrate = Nominal displacement \times Speed
 $= 50 \times 10^{-6} \text{ m}^3/\text{rev} \times 14.17 \text{ rev/s}$
 $= 7.085 \times 10^{-4} \text{ m}^3/\text{s}$

i) Volumetric efficiency = $\frac{\text{Real flowrate}}{\text{Ideal flowrate}} \times 100\%$
 $= \frac{5.83 \times 10^{-4}}{7.085 \times 10^{-4}} \times 100\%$
 $= 82.29\%$

ii) Fluid power = $Q \cdot dp$
 $= 5.83 \times 10^{-4} \times 100 \times 10^5$
 $= 5830 \text{ watts}$

Overall Efficiency = $\frac{5830 \times 100}{15000}$
 $= 38.867\%$

$$= 38.8679$$

$$4 \quad z = 2400 \text{ m} = 24 \text{ m}$$

$$\text{Volumetric flowrate, } Q = 13 \text{ litres/sec} \\ = 0.013 \text{ m}^3/\text{sec}$$

$$\text{Velocity} = 66 \text{ m/sec}$$

The general formula

$$P = \rho g Q \left(\frac{p}{\rho g} + \frac{v^2}{2g} + z \right)$$

$$P = 1000 \times Q p + \rho \frac{Q v^2}{2} + \rho g Q z$$

But introducing here (Power of Jet)
Pressure head = 0

$$z = 0$$

$$\therefore P = \rho \frac{Q v^2}{2}$$

$$P = \frac{1000 \times 0.013 \times (66)^2}{2}$$

$$P = 28314 \text{ watts} = 28.314 \text{ Kilowatt}$$

ii) power supplied from reservoir.

At atmospheric pressure; $p = 0$ and $V = 0$

$$P = \rho g Q z \\ = 1000 \times 9.81 \times 0.013 \times 240$$

$$= 30607.2 \text{ watts}$$

$$= 0.030607 \text{ Kilowatts}$$

$$\begin{aligned}
 \text{(ii) Power loss in ~~transform~~ Transmission} \\
 &= \text{Power of Reservoir} - \text{Power of Jet} \\
 &= (30607.2 - 28314) \\
 &= 2293.2 \text{ Watts} \\
 &= 2.2932 \text{ Kilowatts}
 \end{aligned}$$

$$\text{Head loss in pipeline} = 2.2932 \text{ Kwatts}$$

$$h = \frac{\text{power lost in transmission}}$$

$$\rho g Q$$

$$= \frac{2293.2}{1000 \times 9.81 \times 0.013}$$

$$= \frac{2293.2}{127.53}$$

$$h = 17.98 \text{ m}$$

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$$\text{Efficiency} = \frac{\text{Power of Jet}}{\text{Power of Reservoir}} \times 100\%$$

$$= \frac{28314 \times 100}{30607.2}$$

$$= 92.5\%$$

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$$\rho \text{ of oil} = 0.89$$

$$Z = 30,000 \text{ cm} = 300 \text{ m}$$

$$Q = 220 \text{ l/sec} = 0.22 \text{ m}^3/\text{sec}$$

$$V = 7 \text{ m/sec}$$

Introducing, $Z = 0$, Pressure = 0

$$P = \frac{\rho Q V^2}{2}$$

$$\rho, S_g = 0.89$$

$$S_g = \frac{\lambda}{1000}$$

$$\lambda = 0.89 \times 1000$$

$$\lambda = 890$$

$$\rho = \lambda = 890$$

$$P = \frac{890 \times 0.22 \times (7)^2}{2}$$

$$P = 4797.1 \text{ Watts}$$

Power supplied from Reservoir

$$P = \rho g Q Z$$

$$P = 890 \times 9.81 \times 0.22 \times 300$$

$$P = 576239.4 \text{ Watts}$$

$$\underline{P} = 576.2394 \text{ Kilowatts}$$

$$\text{Efficiency} = \frac{\text{Power of Jet} \times 100}{\text{Power of Reservoir}} = 0.83\%$$

$$6.) P = \rho g Q z$$

$$z = 20\text{m} = h$$

$$\rho = 1000$$

$$g = 9.81$$

$$Q = VA$$

$$d = 10\text{cm} = 10 \times 10^{-2}\text{m}$$

$$A = \frac{\pi d^2}{4} = 7.85 \times 10^{-3}\text{m}^2$$

But we need the velocity at height of initial velocity was
one of the equation of motion

$$v = 0$$

$$v^2 = 0^2 - 2gh$$

$$U = \sqrt{v^2 + 2gh}$$

$$U = \sqrt{0^2 + 2 \times 9.81 \times 20}$$

$$U = \sqrt{392.4}$$

$$U = 19.809 = 19.81\text{ m/s}$$

The velocity = 19.81

$$Q = VA$$

$$= 19.81 \times 7.85 \times 10^{-3}$$

$$= 0.15558\text{m}^3/\text{s}$$

$$= 0.15\text{m}^3/\text{s}$$

$$\Rightarrow d_1 = 0.3 \text{ m}$$

$$A_1 = \frac{\pi d^2}{4} = \frac{\pi \times 0.3^2}{4}$$

$$= 0.07068 \text{ m}^2 = 0.0707 \text{ m}^2$$

$$d_2 = 0.2 \text{ m}$$

$$A_2 = \frac{\pi d^2}{4} = \frac{\pi \times 0.2^2}{4}$$

$$= 0.031415 \text{ m}^2 = 0.0314 \text{ m}^2$$

$$Cd = 0.096$$

Specific weight of gas = 19.62 N/m^3

$$\rho = \frac{mg}{V} = \rho g$$

$$= \frac{19.62}{9.81} = \frac{\rho \times 9.81}{9.81} \quad \text{So, } \rho = 19.62$$

$$\therefore \rho = 2 \text{ kg/m}^3$$

Calculating $Q_1 = A_1 V_1$. $Q_2 = A_2 V_2$, $Q_1 = Q_2$

$$\therefore V_1 = \frac{Q_1}{A_1}$$

$$V_2 = \frac{Q_2}{A_2}$$

$$V_1 = \frac{Q_1}{0.0707}$$

$$V_2 = \frac{Q_2}{0.0314}$$

for the Manometer

$$P_1 - P_2 = 19.62 (z_1 - z_2) + 587.423$$

for the Venturimeter

$$\frac{P_1}{\rho_2 g} + \frac{V_1^2}{2g} + z_1 = \frac{P_2}{\rho_2 g} + \frac{V_2^2}{2g} + z_2$$

$$\therefore z_2 - z_1 = 0.06 \text{ m}$$

$$Q_{\text{ideal}} = A_2 V_2$$

$$\therefore 27.047 \times 0.0314$$

$$Q_{\text{ideal}} = 0.8492$$

$$= 0.85 \text{ m}^3/\text{s}$$

$$Q_{\text{real}} = C_d \times Q_{\text{ideal}}$$

$$= 0.96 \times 0.85$$

$$= 0.816 \text{ m}^3/\text{s}$$

$$\textcircled{8} \text{ Throat diameter} = 0.676 \text{ m } (d_2)$$

$$\text{Vertical diameter} = 0.152 \text{ m}$$

$$\text{Relative density} = 0.8$$

$$\text{Throat being} = 0.914 \text{ m}$$

$$C_d = 0.91$$

Bernoulli's Eqn

$$A_1 = \frac{\pi d^2}{4} = \frac{\pi \times 0.015^2}{4}$$

$$= 0.000177 \text{ m}^2$$

ii) Then $P_1 - P_2 = 15170$

$$Q^2 = 1.24 \times 10^{-3}$$

$$Q = \sqrt{1.24 \times 10^{-3}}$$

$$Q = 0.0352 \text{ m}^3/\text{s}$$

9.) $d_1 = 300 \text{ mm} = 0.3 \text{ m}$

$$d_2 = 150 \text{ mm} = 0.15 \text{ m}$$

$$A_1 = 0.07069 \text{ m}^2$$

$$A_2 = 0.0177 \text{ m}^2$$

$$Q = 40 \text{ lit/sec} = 0.04 \text{ m}^3/\text{sec}$$

$$Z_1 = 10 \text{ m}, \quad Z_2 = 6 \text{ m}$$

$$P_1 = 400 \text{ kN/m}^2, \quad P_2 = 7$$

$$10. \text{ Reading of Manometer} = 170 \text{ mm} \\ = 0.17 \text{ m}$$

$$\text{Specific gravity of mercury} = 13.6$$

$$\text{Specific gravity of seawater} = 1.026$$

$$y = 0.17 \text{ m}$$

$$\text{for } h = y \left(\frac{S_h}{S_l} - 1 \right)$$

$$= 0.17 \left(\frac{13.6}{1.026} - 1 \right)$$

$$= 0.17 \times 12.55$$

$$= 2.0834 \text{ m}$$

$$\text{Recall } v = \sqrt{2gh}$$

$$v = \sqrt{2 \times 9.81 \times 2.0834}$$

$$v = \sqrt{40.87}$$

$$v = 6.393 \text{ m/s}$$